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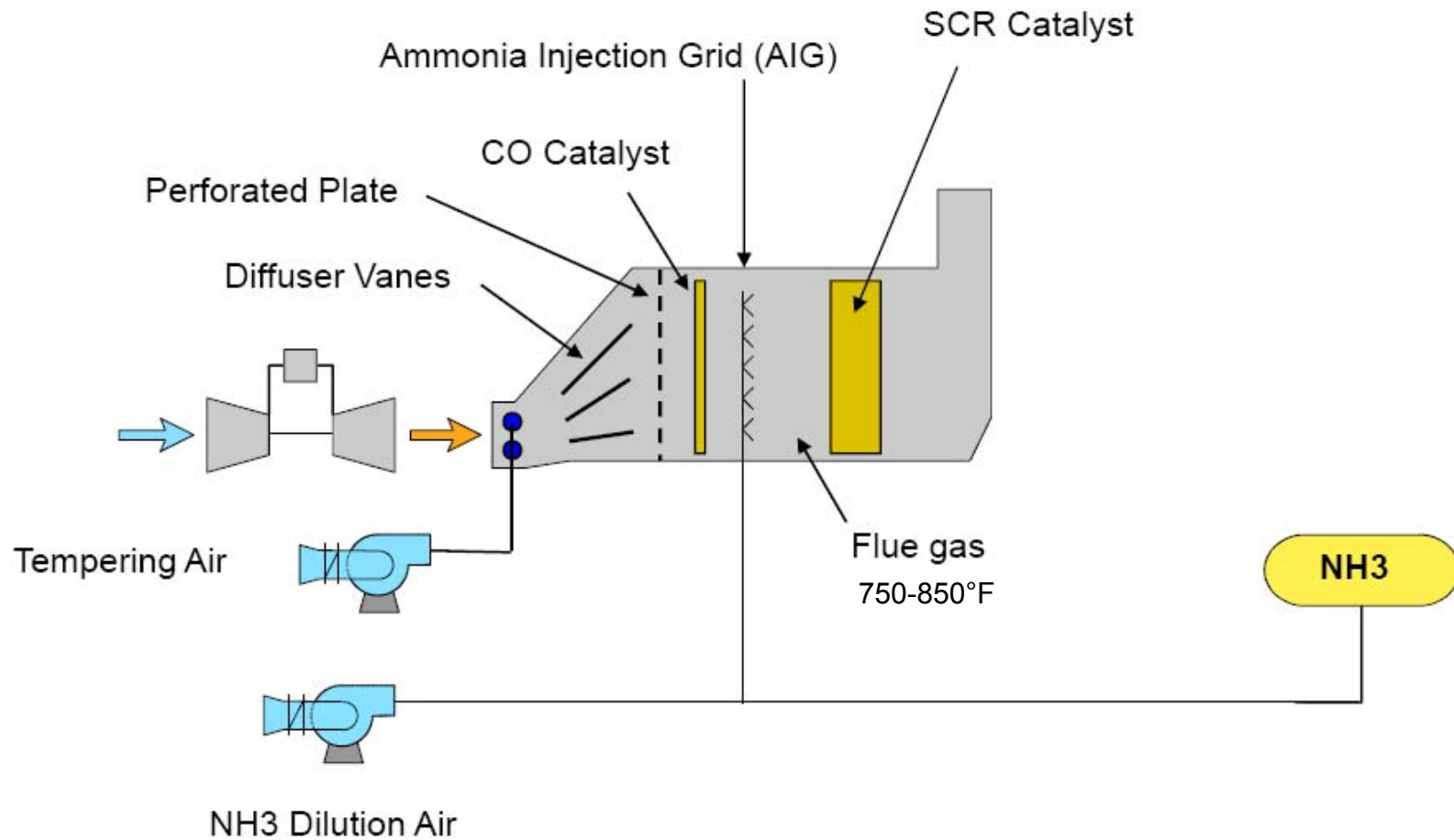
# **Gas Turbine SCR Performance Optimization and Management**

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Laguna Hills, CA

**McIlvaine Hot Topic Hour**  
February 14, 2013

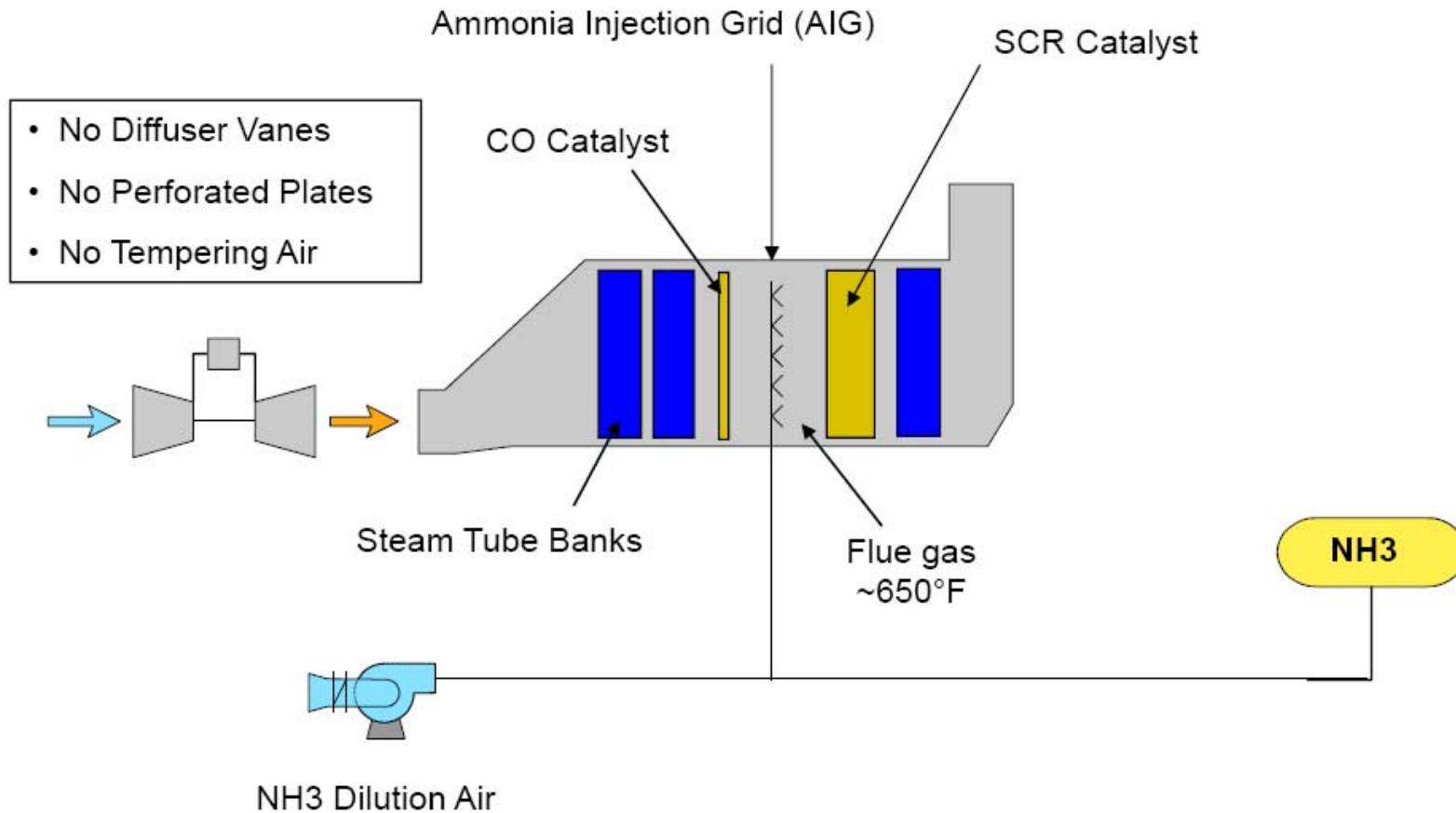
# Gas Turbine SCR Systems

## Simple Cycle GT SCR



# Gas Turbine SCR Systems

## Combined Cycle GT SCR

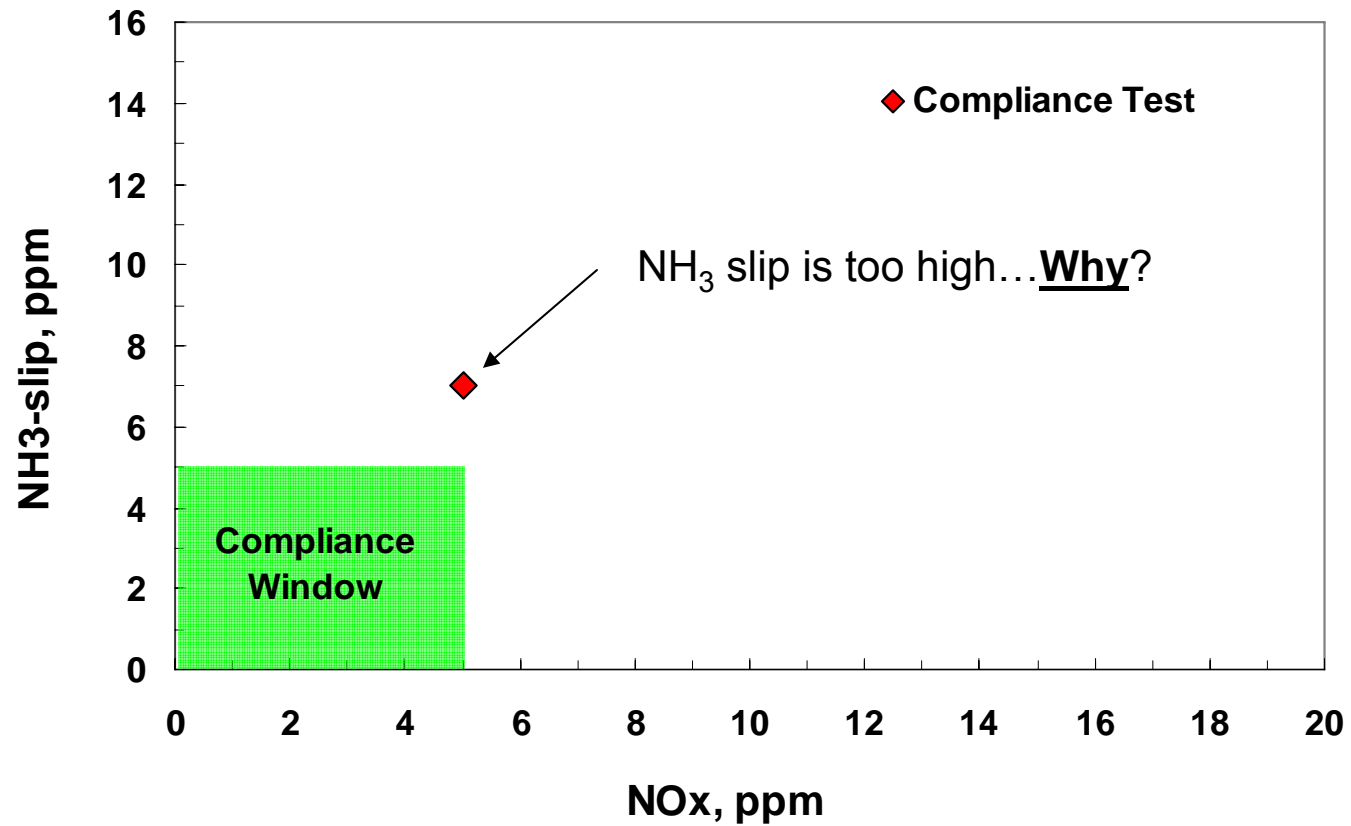


# Today's Gas Turbine SCR Topics

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- **Troubleshooting**
  - FERCo is a trusted 3<sup>rd</sup> party engineering services company
  - Extensive background with SCR (design, modeling, full scale testing)
  - Developed a process model for SCR design and troubleshooting
- **Catalyst Inlet NH<sub>3</sub>/NO<sub>x</sub> Distribution and AIG Tuning**
  - Why NH<sub>3</sub>/NO<sub>x</sub> distribution is important
  - How AIG tuning can extend catalyst life
  - FERCo's approach to AIG tuning
- **SCR Catalyst Management**
  - What is it?
  - How is it done?
  - Why is it done?

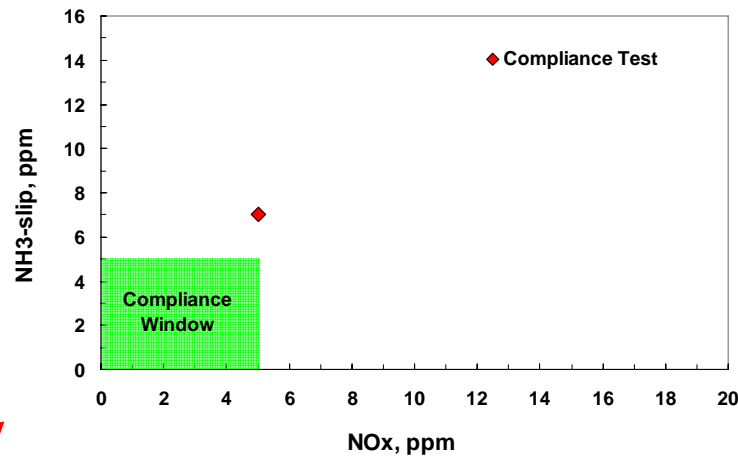
# Troubleshooting



# Why?

## Catalyst Activity (K)?

- F(material, geometry)
- Condition of active sites



## Reactor Potential?

- Ability of the catalyst bed to reduce NO<sub>x</sub>
- $RP = K * A_{sp} * V_{cat} / Q_{fg}$

## Poor NH3/NOx Distribution?

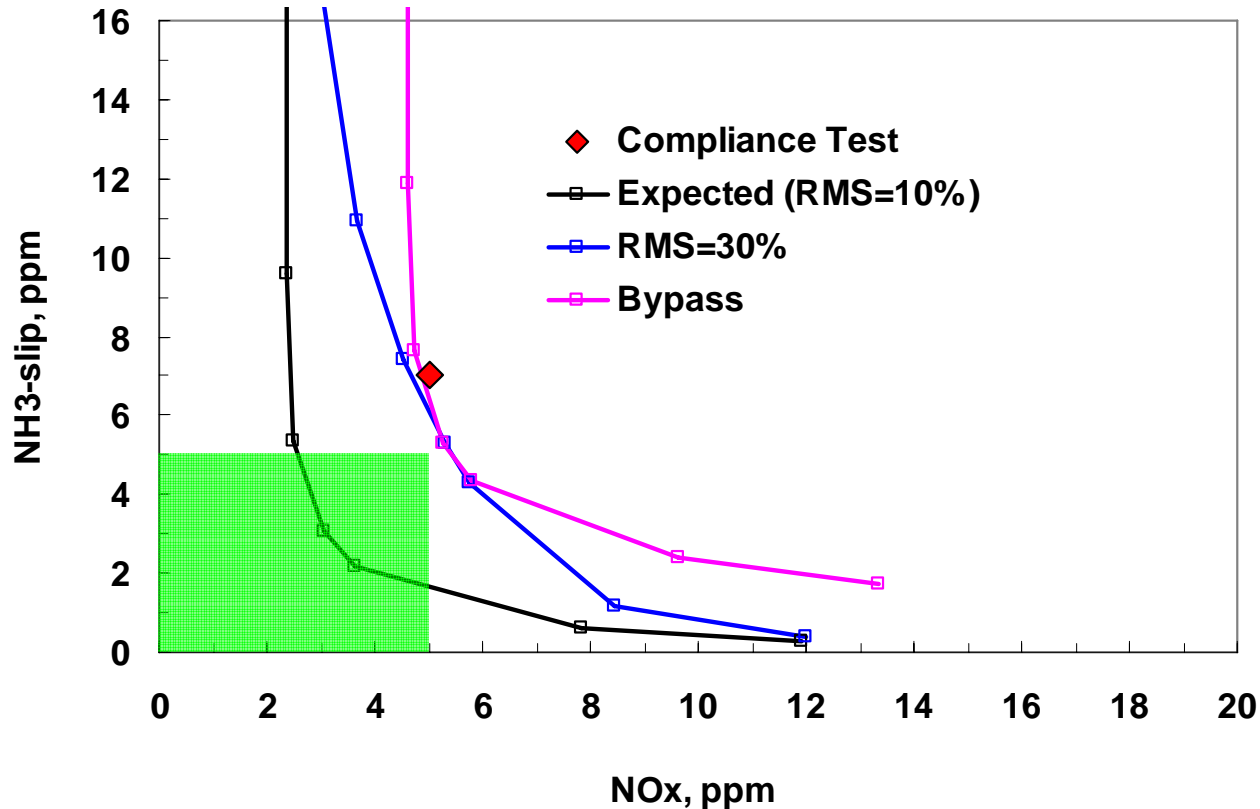
- Uniform NH<sub>3</sub>/NO<sub>x</sub> profile is critical
- Local NH<sub>3</sub>/NO<sub>x</sub> > 1 creates NH<sub>3</sub> slip

## Flue Gas Bypass?

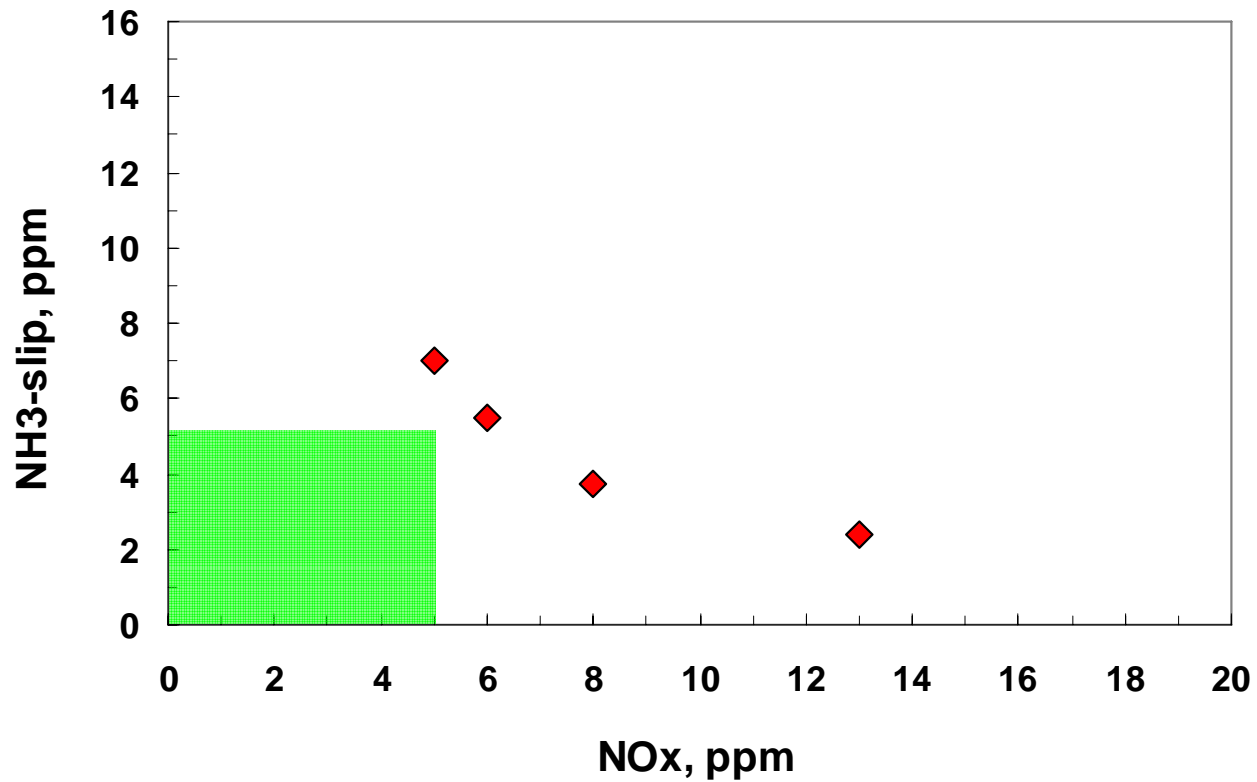
- Any leakage around the catalyst increases stack NO<sub>x</sub> & NH<sub>3</sub>

# Activity, NH3 Distribution, or Bypass?

- FERCo utilizes a process model to compare expected SCR performance to actual performance (see curves below)
- A single data point is not sufficient for identifying the problem

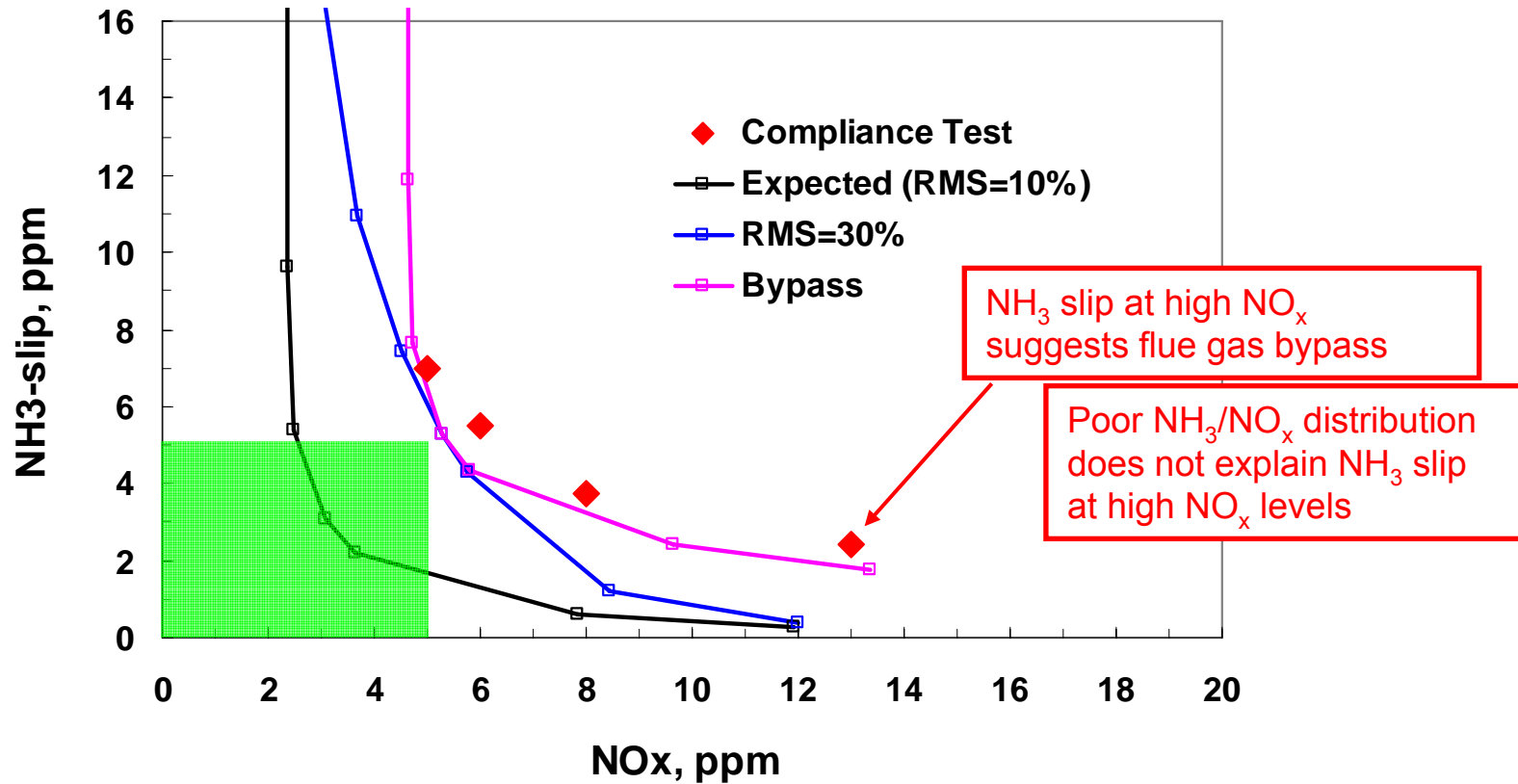


# Perform Additional Tests





# Flue Gas Bypass?

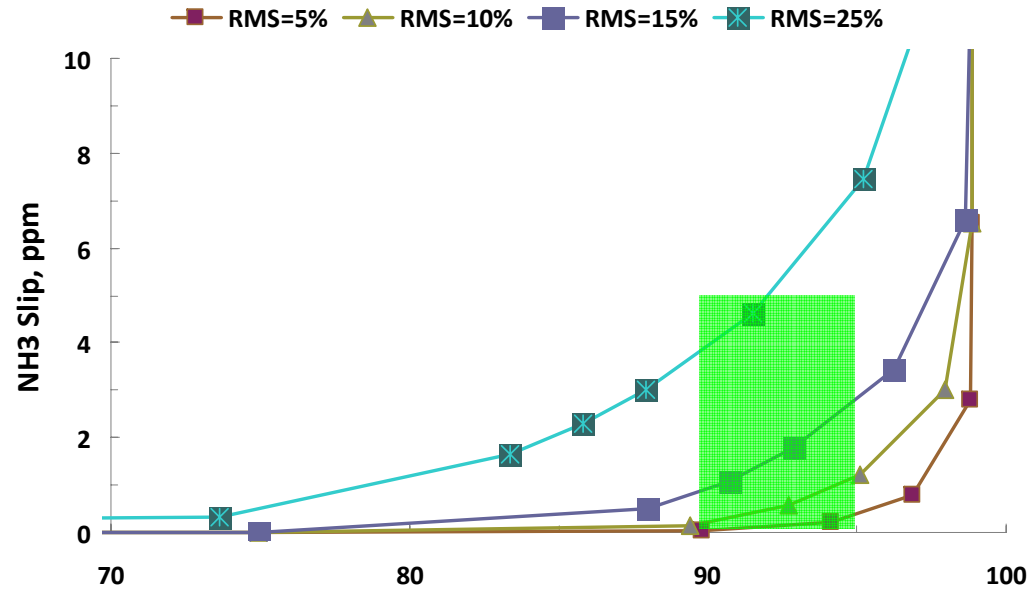


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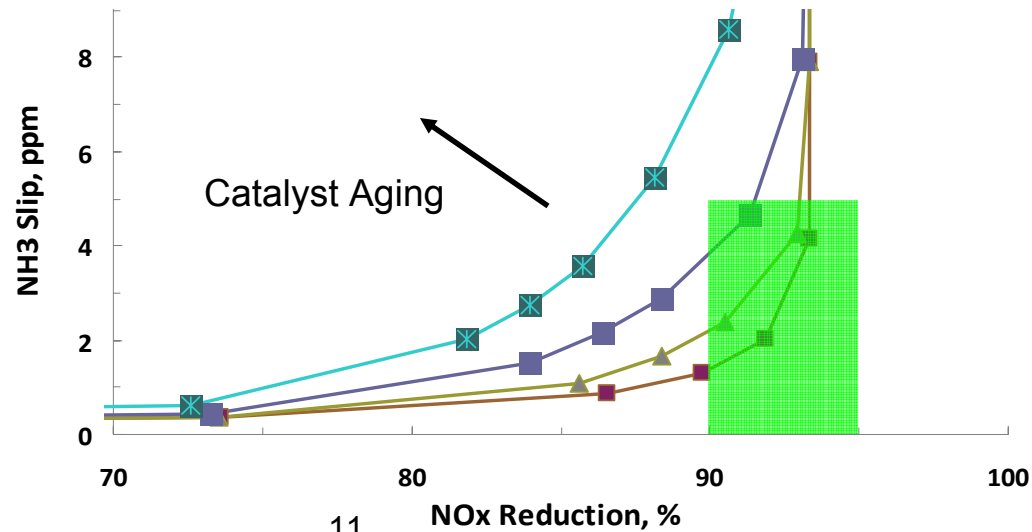
# Catalyst Inlet NH<sub>3</sub>/NO<sub>x</sub> Distribution and AIG Tuning

# NH<sub>3</sub>/NO<sub>x</sub> Distribution and AIG Tuning

New Catalyst



Near Catalyst End-of-Life



# Sample Probe Grid Expedites Tuning



- AIG tuning is difficult without a probe grid at the catalyst exit
  - The costs for installing a probe grid will be recovered in the long run:
    - No scaffolding or manlift required for testing (\$, safety issues)
    - Reduced test times (no manual probe)
    - Reduced testing contractor costs
    - More data
- 50MW simple cycle SCR  
With a grid of 50 sample probes  
(5 x 10)**

# Sample Probe Grid Expedites Tuning



# Sample Probe Grid Expedites Tuning

A sample grid is especially important for larger units (e.g., more than 30' wide)



**325MW combined cycle SCR  
with a 36-point sample grid  
(6 x 6)**

# FERCo's Multipoint Instrumentation

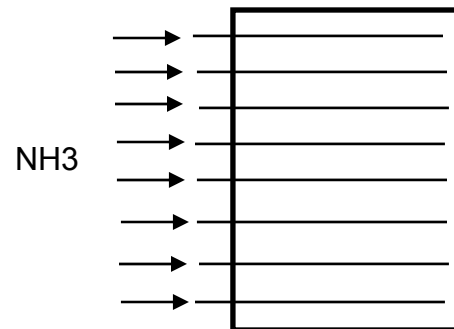


- Samples 48 points in 15 minutes
- NOx and O2



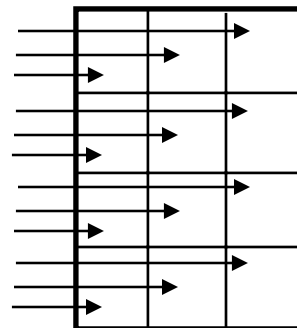
# AIG Design Influences Tuning

- Some systems have no AIG adjustment valves – *bad idea!* No flexibility to account for 1) duct velocity gradients, 2) duct NOx gradients, or 3) lance-to-lance ammonia flow gradients
- Most systems have one-dimensional adjustability



Vertical adjustability can handle only vertical velocity or inlet NOx gradients

- Ideal design: multiple zone adjustability

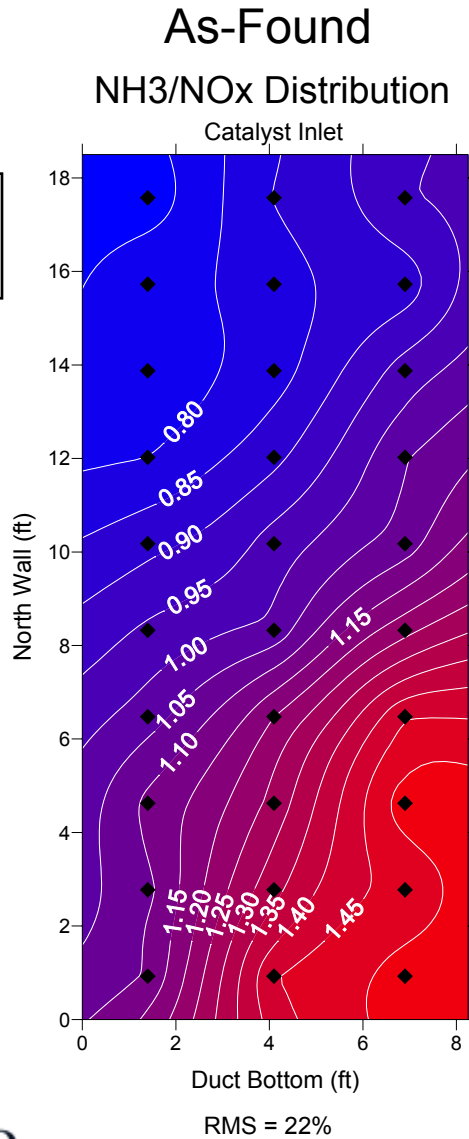
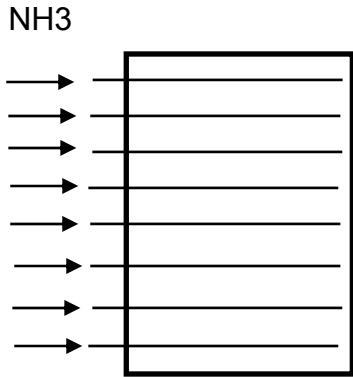


Multiple zones allow treatment of localized gradients

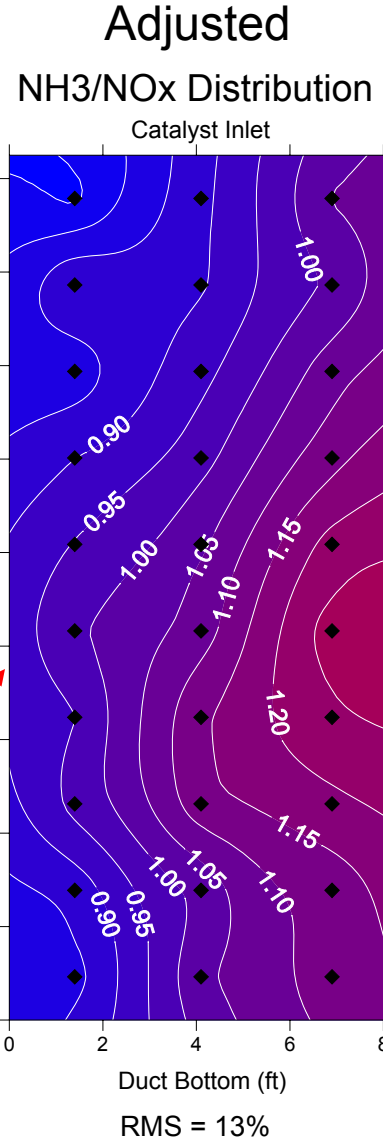


# AIG Tuning, 10 MW Gas Turbine SCR

One-Dimensional,  
Vertical AIG

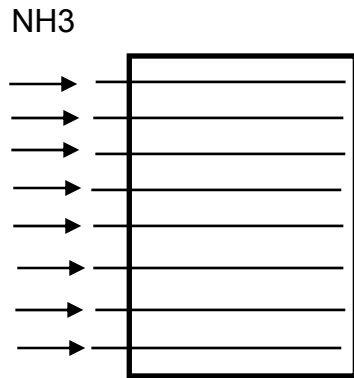


Adjustments  
across the width  
not possible

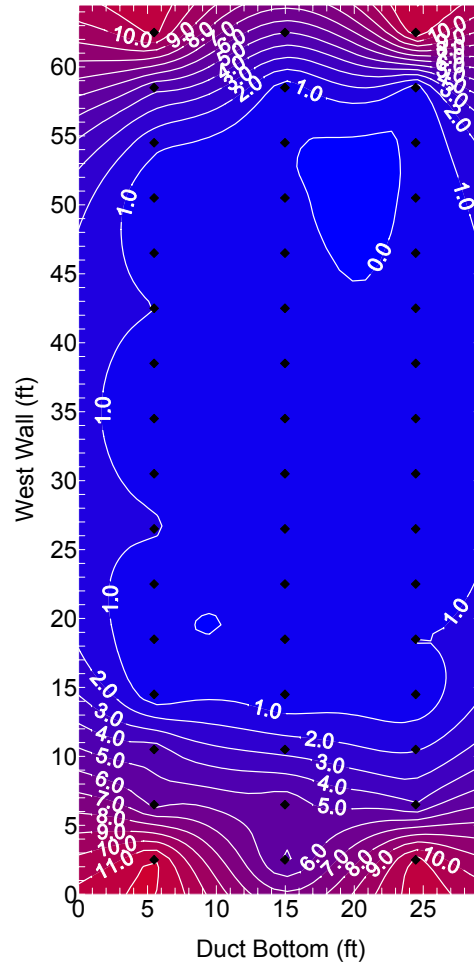


# AIG Tuning, 350MW Combined Cycle SCR

One-Dimensional,  
Vertical AIG



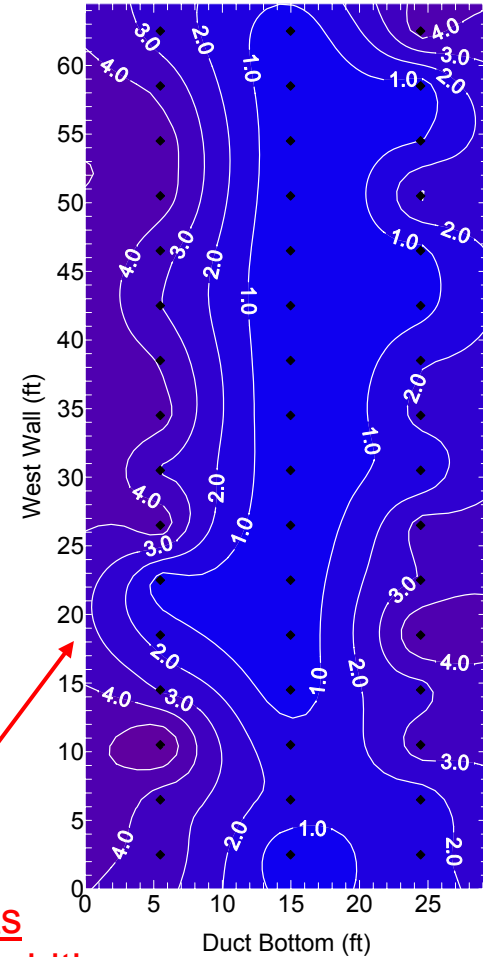
**As-Found Outlet  
NOx (ppm)**



**NH<sub>3</sub> consumption  
reduced by 5%**



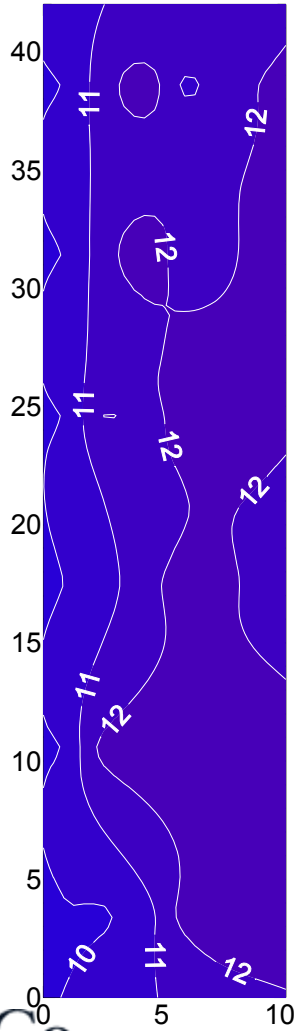
**Optimized Outlet  
NOx (ppm)**



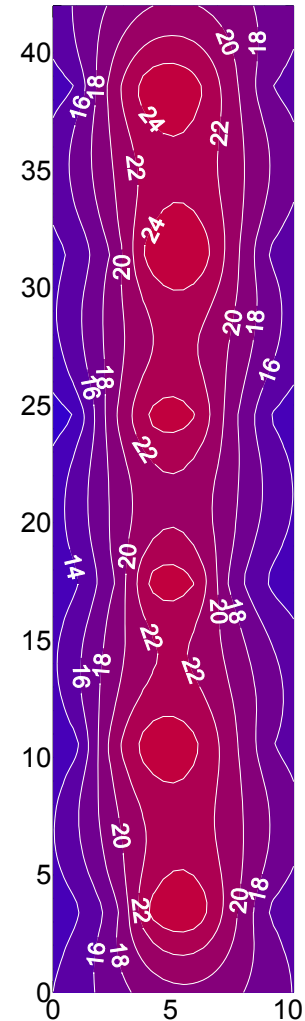
**Adjustments  
across the width  
not possible**

# Duct Burners Impact AIG Tuning

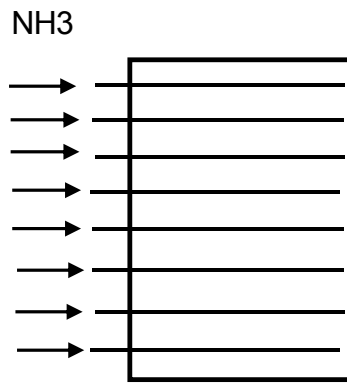
Duct Burners Off  
(Inlet NO<sub>x</sub> ppm)



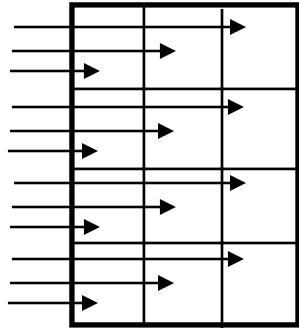
Duct Burners On  
(Inlet NO<sub>x</sub> ppm)



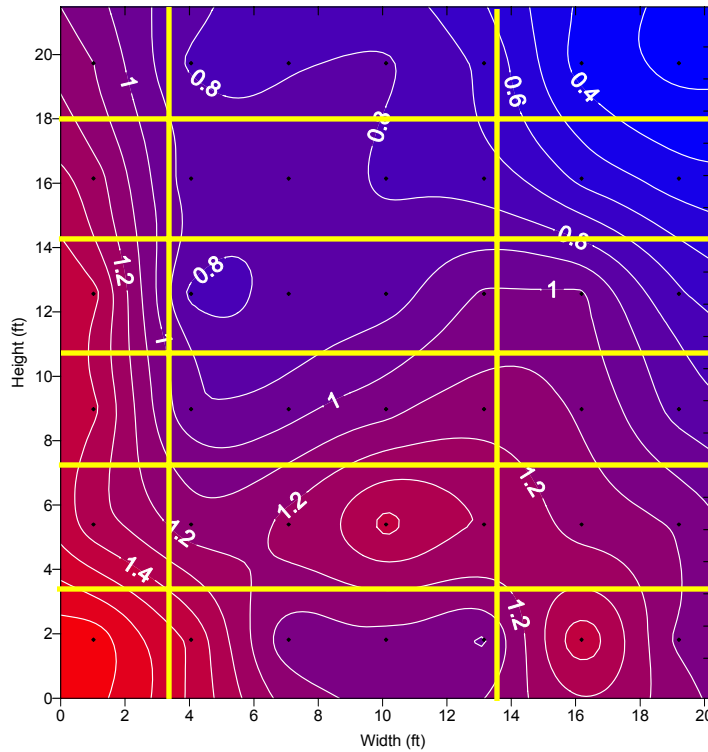
→  
**AIG Tough to Tune**



# AIG Tuning, 10 MW Gas Turbine SCR, 90° Turn

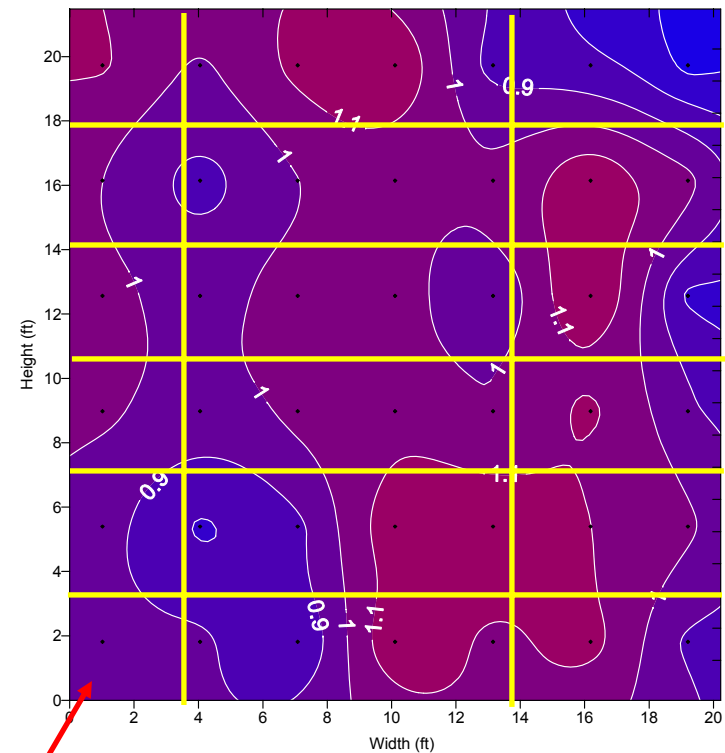


As-Found  
Normalized NH<sub>3</sub>/NO<sub>x</sub> Distribution



RMS = 32%

Adjusted  
Normalized NH<sub>3</sub>/NO<sub>x</sub> Distribution



Corners adjusted

RMS = 13%

Multiple zones,  
skewed based  
on flow modeling

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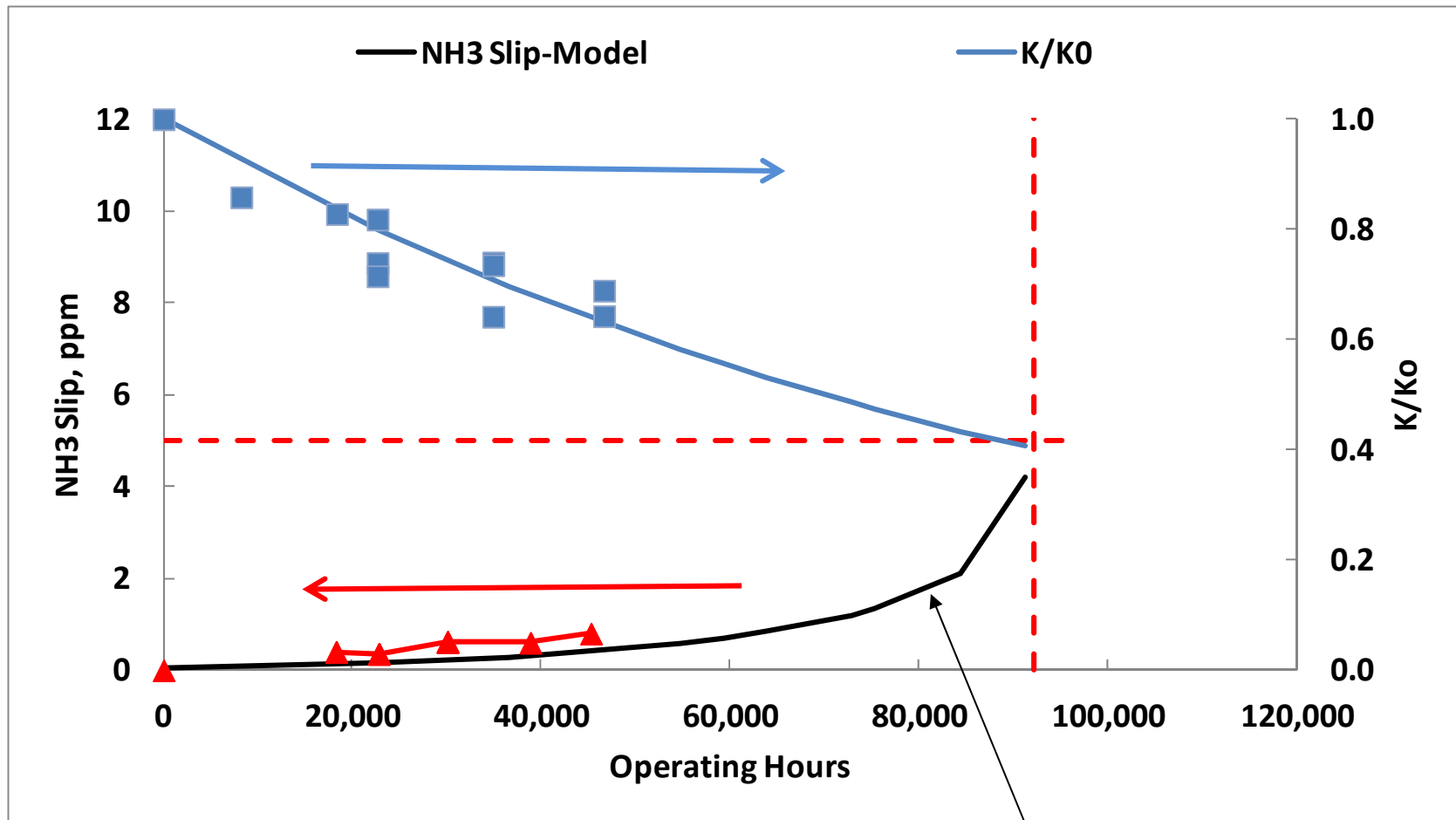
# SCR Catalyst Management

# SCR Catalyst Management

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- **What is catalyst management?**
  - **Keeping track of catalyst activity to ensure continued compliance**
- **How is catalyst management done?**
  - **Periodically determining the activity of the catalyst in the reactor**
  - **Laboratory analysis (if a sample can be obtained)**
  - **In situ analysis (later discussion topic)**
  - **Utilize catalyst management software for planning**
- **Why is it done?**
  - **Forecast when catalyst additions or replacements are necessary**
  - **Provide sufficient lead time to procure catalyst (6-9 months)**

# Catalyst Activity Degrades With Time



Monitoring ammonia slip is also critical

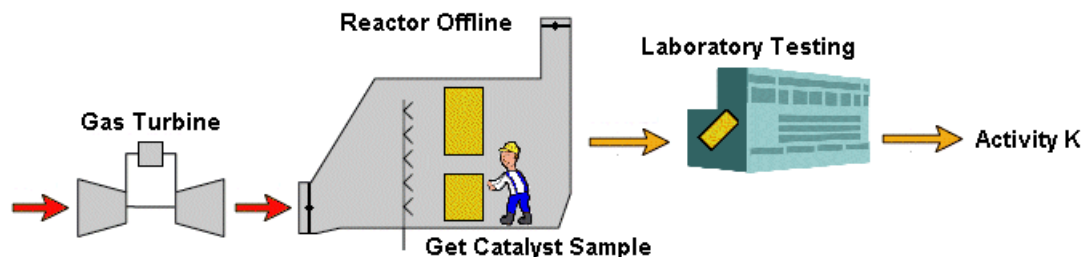
# *In Situ* Catalyst Activity Measurement\*

## Traditional Lab Measurement

- Typically one per year
- Currently no test protocol

$$K_{\text{Lab}} = -A_{\text{Vdesign}} \ln(1 - \Delta\text{NO}_x)_{\text{Lab}}$$

@NH<sub>3</sub>/NO<sub>x</sub>=1-1.5

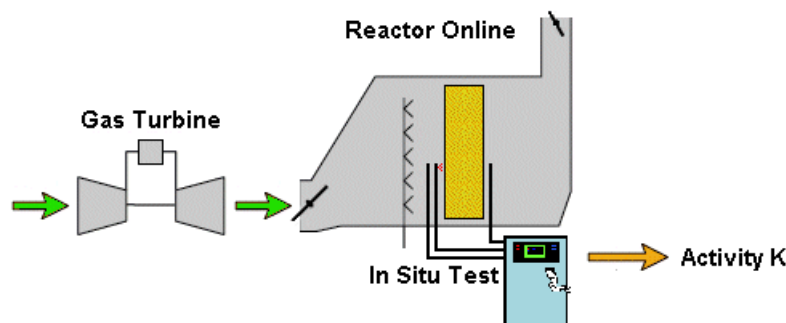


## FERCo's CatalysTrak®\*

- *in situ* measurement
- No outage required

$$K_{\text{In-situ}} = -A_{\text{Vactual}} \ln(1 - \Delta\text{NO}_x)_{\text{full scale}}$$

@NH<sub>3</sub>/NO<sub>x</sub>>1 locally



\* Patented Process



Questions?

[www.ferco.com](http://www.ferco.com)

