

Staged, Pressurized Oxy-Combustion (SPOC)

McIlvaine Company Hot Topic Hour
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Richard Axelbaum
Jens Professor of Environmental Engineering Science
Department of Energy, Environmental and Chemical Engineering
Director, Consortium for Clean Coal Utilization (CCCU)
Washington University in St. Louis

Consortium for Clean Coal Utilization

Founded in January of 2009, the Consortium is dedicated to addressing the scientific and technological challenges of ensuring that coal can be used in a clean and sustainable manner.



Approach

- Research projects are being supported at Washington University in collaboration with Partner Universities around the world.
- State-of-the-art clean coal facilities have been established.
- A motivated work force is being educated to address the challenges associated with clean utilization of coal in the 21st century.

Sponsors

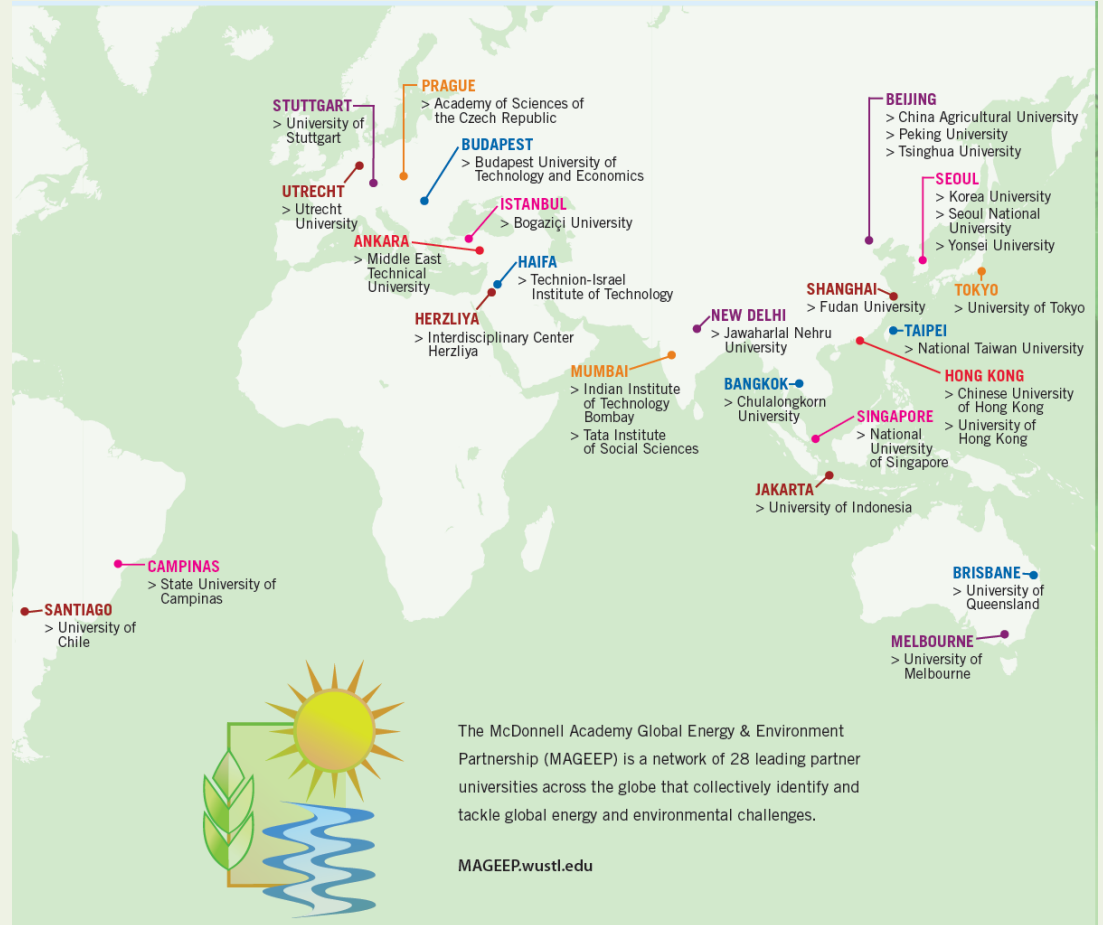
Peabody Energy

Arch Coal

Ameren

CCCU Research Portfolio

- Carbon Dioxide Capture
 - Oxy-combustion
 - Post combustion capture
- Carbon Dioxide Utilization
 - Chemical conversion
 - Algae
- Geological Sequestration
 - Injection/storage modeling
 - Chemical interactions
 - CO₂ Imaging
- Mercury and HAPS control
- Fly Ash Utilization



International Partner Institutions

Advanced Coal & Energy Research Facility



ACERF:

- 1 MWth capacity
- Configured for oxy-combustion
- Full suite of emissions monitoring

Additional Facilities:

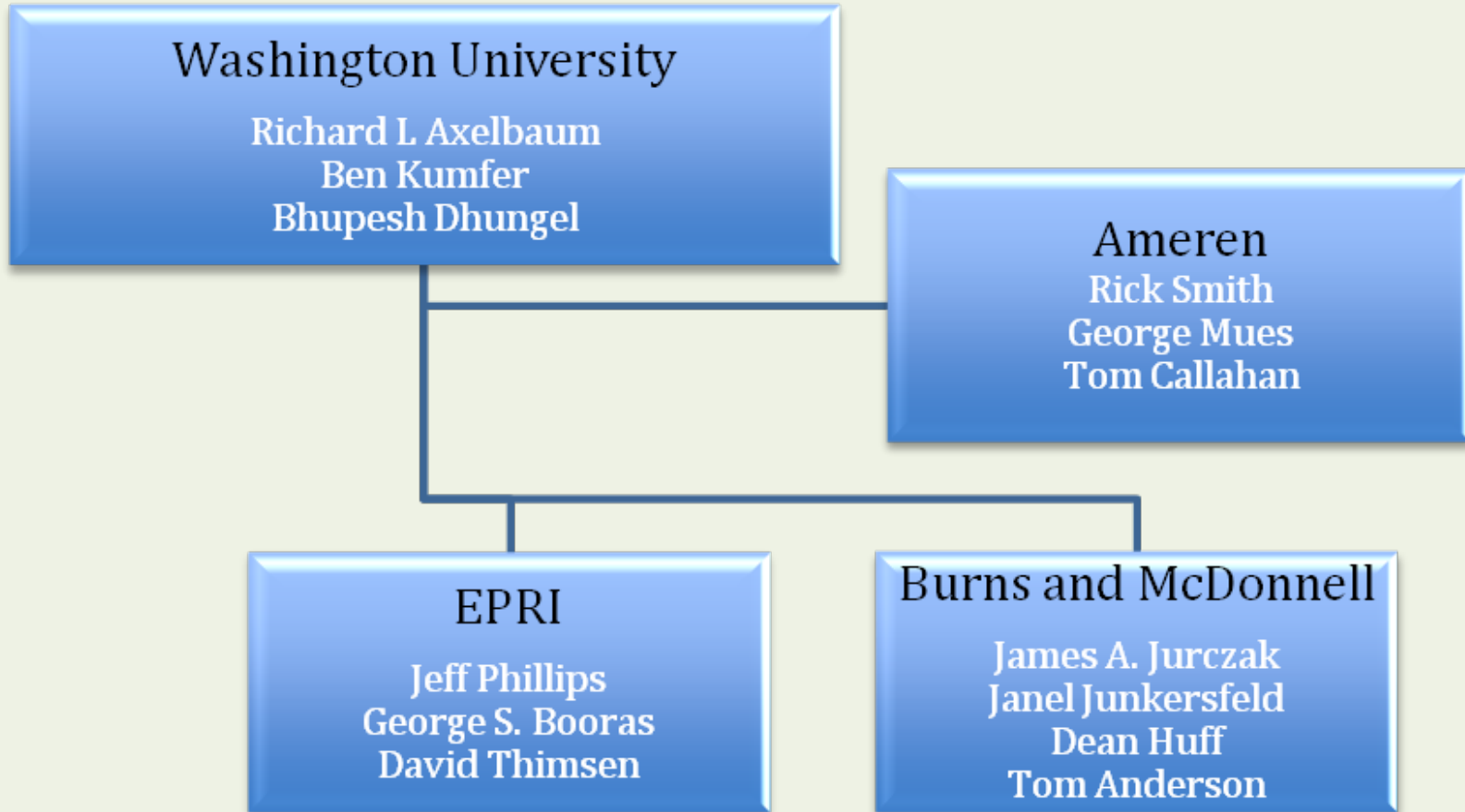
- 30kW lab-scale test furnace
- Drop tube furnace
- Fuel/ash characterization

DOE Project Goals

- Develop a novel pressurized oxy-combustion process capable of achieving 90% carbon dioxide capture at no more than a 35% increase in cost of electricity (COE) (<\$25/ton CO₂ captured)¹
- Optimize the design through process modeling to minimize COE
- Identify and analyze potential technical barriers and determine possible solutions

1. Research and Development Goals for CO₂ Capture Technology DOE/NETL-2009/1366

Project Team



Pressurized Oxy-Combustion

- The requirement of high pressure CO₂ for sequestration enables pressurized combustion as a tool to increase efficiency and reduce costs
- Combustion occurs at 10-40 bar
- Benefits:
 - Latent heat of flue gas moisture can be utilized
 - Reduces flue gas volume, potentially translating into lower capital costs
 - Avoids air ingress
 - Increases convective heat transfer (for a given velocity)
 - Increases char burning rates

Advanced Oxy-Combustion Rankine Cycle

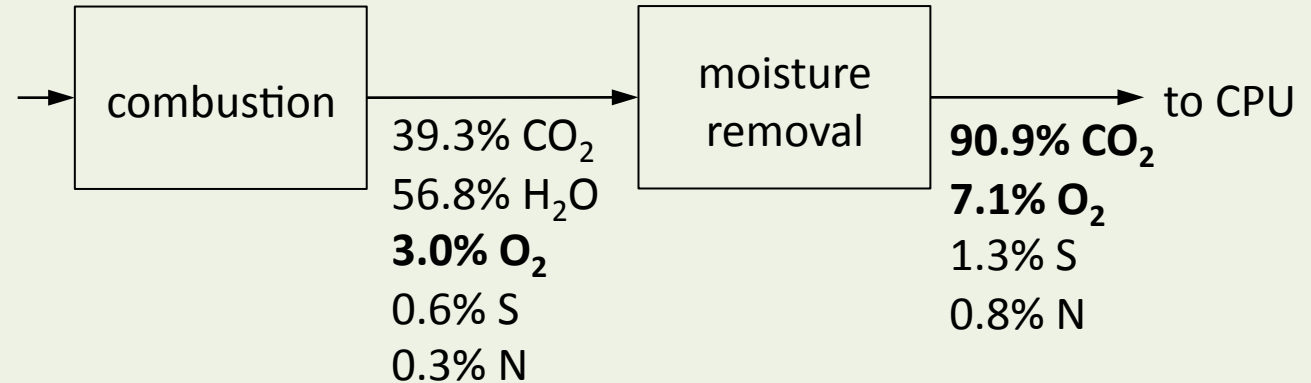
To achieve project goals, capital and operating costs must be reduced over those of 1st generation oxy-combustion or other approaches to pressurized oxy-combustion

- Capital Costs
 - Minimize heat transfer surface area
 - Minimize auxiliary equipment size (CPU, filters, fans)
- Operating Costs
 - Maximize efficiency
 - Recover latent heat in flue gas
 - Use a high temperature & pressure steam cycle
 - Minimize parasitic loads
 - Minimize excess oxygen requirements

Coal Slurry vs. Dry Feed

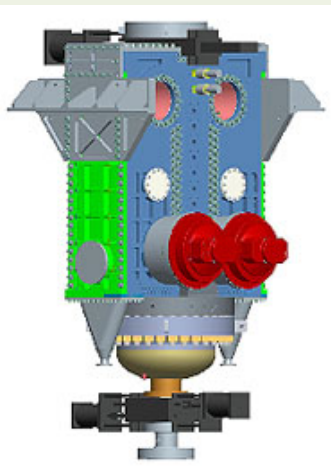
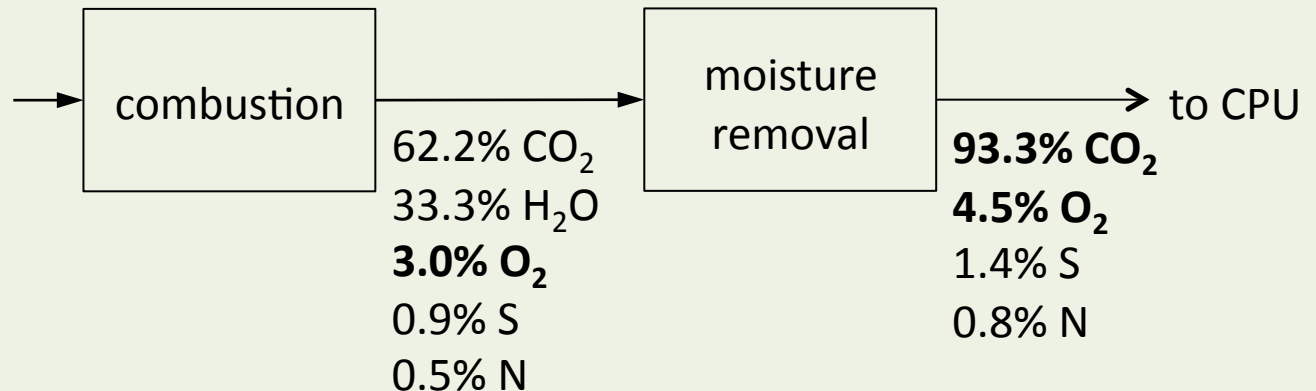
Case A: coal slurry

(50wt% dry coal, 50% H₂O)
+ O₂, $\lambda = 1.065$



Case B: pulverized coal

(as received, 11wt% H₂O)
+ O₂, $\lambda = 1.041$

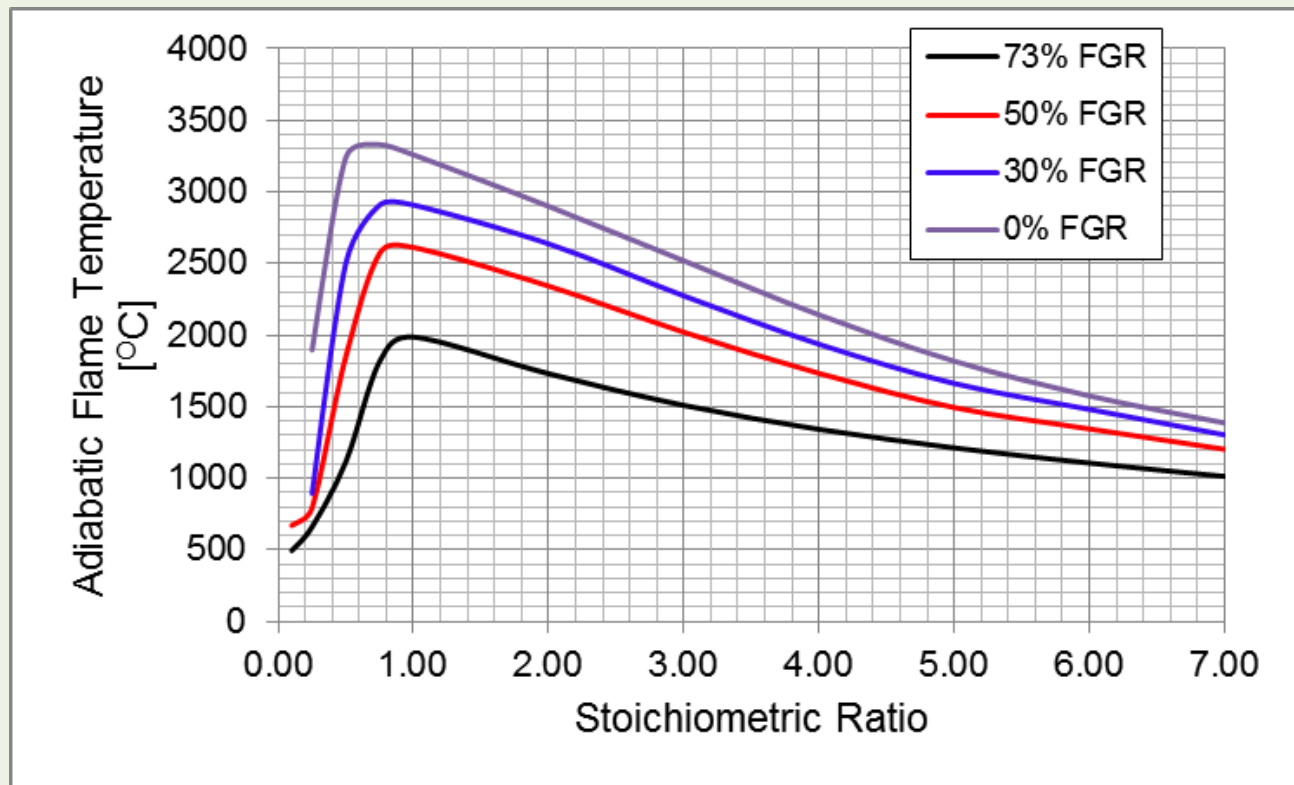


- Less O₂ required from ASU
- Less O₂ removal in CPU

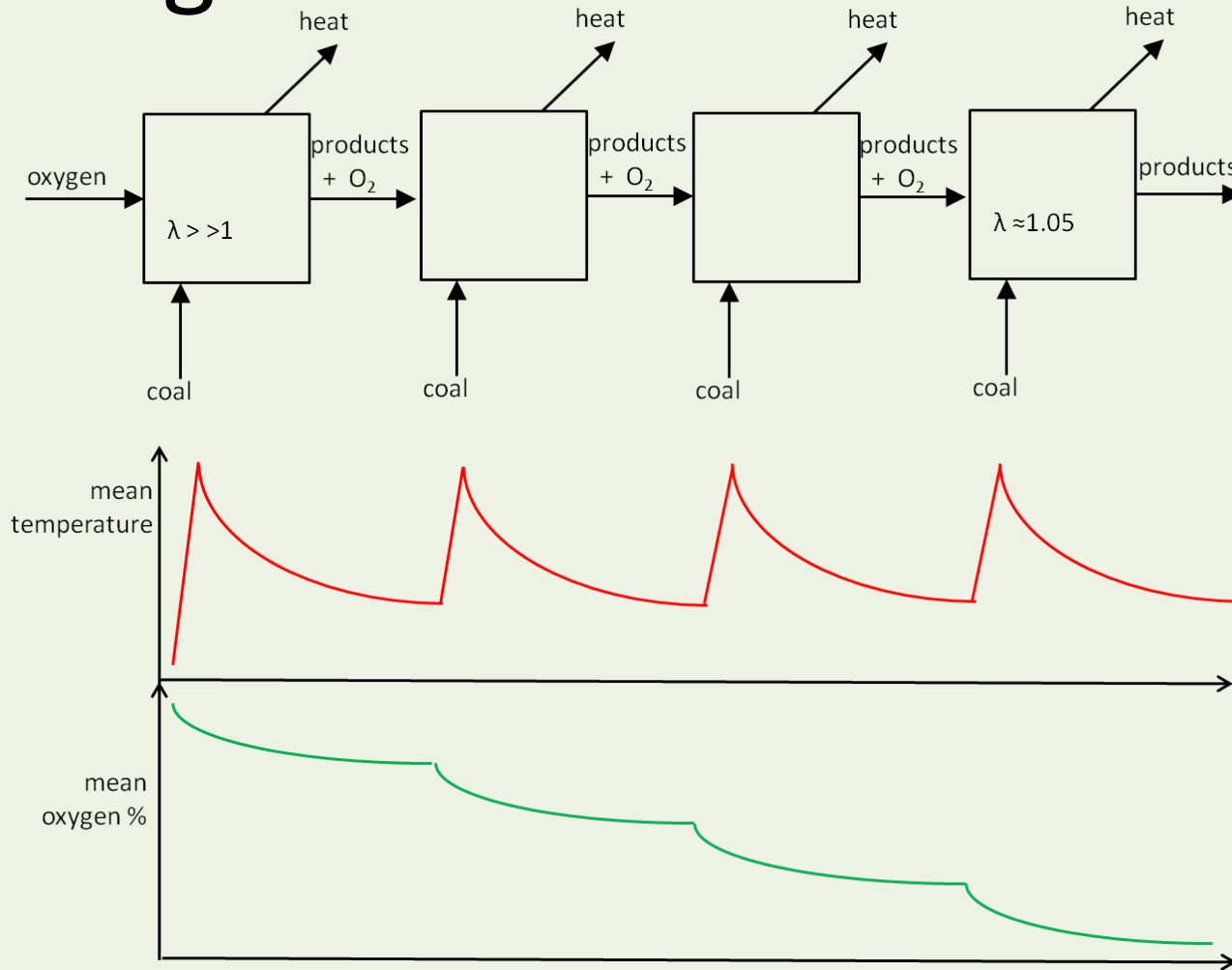
Pratt & Whitney Rocketdyne dry solids feed pump

First Thoughts on Temperature Control

- Temperature in oxy-combustion is typically controlled by addition of RFG or water (CWS or steam)
- But, global combustion temperature is also a function of stoichiometric ratio

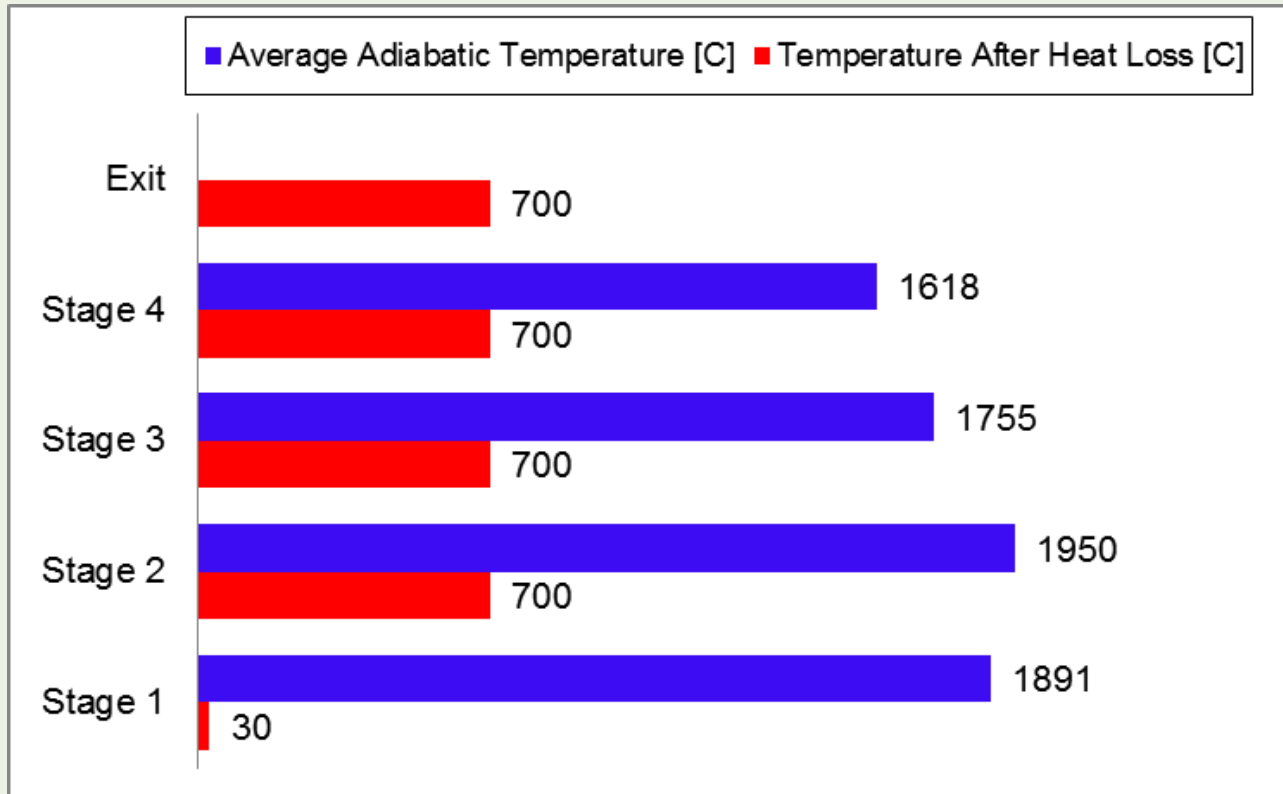


Staged Combustion Concept



- Employ high stoichiometric ratio in early stages to control mean temperature
- Cooled products from early stages (CO₂, H₂O) assist in controlling temp downstream

Progression of T and Gas Composition



End of Stage	Vol. % wet	Vol. % wet	Vol. % wet	Vol. % wet	Vol. % wet
	CO2	H2O	SO2	N2	O2
Stage 1	23.4	8.8	0.2	5.1	62.5
Stage 2	41.4	15.6	0.4	4.6	38.0
Stage 3	55.6	20.9	0.6	4.2	18.7
Stage 4	67.1	25.2	0.7	3.9	3.0

Benefits of Staged Combustion

- Near-zero flue gas recycle
 - Minimizes flue gas volume
 - Minimizes equipment size
 - Minimizes parasitic loads and pumping costs associated with RFG
 - Minimizes oxygen requirements
- Higher peak temperature
 - Increased radiation heat transfer
 - With proper design, can ensure maximum and uniform heat flux to the boiler tubes