Re-Engineering Coal-Fired Generating Plants for Low Pollutant Emissions and Extended Competitive Life



By CastleLight Energy Corp April, 2012

CastleLight Energy Corp.

- CastleLight Energy Corp. comprises the technical team from Rockwell International - from 1980's rocket engine modeling programs.
- Developed the Clean Combustion System[™] (CCS)
 Control of SO₂ & NO_x with improved efficiency
- Coal Beneficiation Processes
 - Remove water, ash, & mercury from coal
 - Recover oil values from coal
- Commercial Field Demonstrated Technology
- Provide Technology Management & Licensing

Observation

EPA 's Strict New Environmental Regulations

- Cross State Air Transport Rules (CSAPR)
 - Focus on SO₂ & NO_x (particularly in summer months)
- Mercury and Air Toxic Standards (MATS)
 - Focus on Particulates, SO₂ Mercury, HAPS
- Green House Gas Performance (GHG) No CO₂ increase allowed
- Impact:
 - The older, smaller (<400MW) coal-fired generating plants may be abandoned due to cost of emissions compliance.

Solution / Approach:

- Re-Engineer plant with Clean Combustion System (CCS) for:
 - ✤ SO₂, NO_x, and mercury emissions compliance
 - ✤ Higher Efficiency (No CO₂ increase)
 - Construction Permit with waiver of PSD No NSR
 - Lower Retrofit & Operating Cost = Competitive Dispatch

Conventional Emission Controls

 $SO_2 = FGD + Limestone; NO_x = SCR + Ammonia;$ $SO_3 = Trona, Hg = Activated Carbon$



CCS Hybrid Coal-Gasification SO₂ & NO_x Control Right in the Combustion Step



Hybrid Coal Gasification Schematic

The Clean Combustion System (CCS)



LNS-CAP Facility

ESSO Site, Cold Lake, Alberta Canada 50 mmBtu/hr – 3T/hr PRB Coal



Demonstrated Emissions

SO₂ - 0.2 lb./mmBtu & NO_x - 0.15 lb./mmBtu

ESSO LNS-CAP Facility, Cold Lake, Alberta, Canada



CCS-Stoker[®] Project Description

Objective:

- Reduce operating cost by half
- (switch to low-cost high-sulfur Illinois coal 2.5 lb. SO₂/mmBtu) Construction Permit w/ waiver NSPS, PSD; no NSR
- Emissions Warrantee: <0.9 lb. SO₂/mmBtu, <0.25 lb. NO_x /mmBtu
- **Project Initiated**: Oct 2005, **Commissioning**: Jan 2007
- - **<u>CEC Scope</u>** : Process Design & Engineering; Supply all equipment, hardware, electrical, instrumentation / controls
 - Provide Commercial Warrantee & License
- **<u>Client Scope</u>**: Site Construction Management; Equipment Installation, as directed by CLPRC

 - Commissioning & Start-up
- **Project Support:** In part, by the Illinois Department of Commerce and Economic Opportunity through the Illinois Clean Coal Institute and the Office of Coal Development.

Coal-Fired Stoker Boiler (typical)



CCS Retrofit Modifications

Remove:

Stoker Feeders, Ash Hopper, Brick over stoker grate Control Panel

New Equipment:

CCS Burner, Gasification Chamber, Combustion Air Heater Boiler Instruments, Coal Mill, Bag house, FD fan, BM & Combustion Sys, HMI & PLC Controls New MCC

Operators (one/shift):

Was all manual operation; Now with HMI - from cold start to automatic full load operation in 5 hrs.

CCS-Stoker® Retrofit 30 MW (Thermal) - 125 mmBtu/hr – 5 T/hr Coal



Gasification Chamber Installation



Gasification Chamber Installation

- McBurney Corp designed and supplied the GC
- Connected to the boiler drums for natural circulation water cooling
- Shop fabricated membrane wall studded and refractory lined.





CCS-Stoker[®] Equipment and Operation Pulverizer

- Refurbished 453 CE/ Raymond mill
- "Indirect Firing" Scheme
- Uses hot combustion flue gas (<10% O₂)
- Fixed sweep gas flow, variable coal flow
- Gas temperature adjusted to give 150F at exit
- Dry powdered coal to bag house



CCS-Stoker® Equipment and Operation Coal-Air Separator

- Separates coal from sweep gas
- No air (O₂) added for bag cleaning
- Hopper w/ level switches maintains ~30min. coal supply
- Gate & spouts to rotary feeders - meters PC to CCS burners





CCS-Stoker® Operation Observations Operation @ MCR – Steam Overboard



CCS-Stoker[®] Retrofit Performance Preliminary Results – Full Load Operation

ltem	Stoker Base Line Test	Preliminary CCS Performance	% Change from Base Line
SO ₂ Stack Emissions (Ib/MMBtu)	1.80	0.72	- 67.0 %
NOx Stack Emissions (Ib/MMBtu)	0.50	0.14 (88 ppm)	- 72.0 %
Boiler Efficiency	77.0	86.9	+ 12.8 %
CO ₂ Emissions - Ton/yr GW credits (% Reduction)	94,019	73,720	20,300T/y (- 21.6 %)
Project Cost Recovery (from firing lower cost coal)		~ 3 years	

CCS-Tangential[™] Boiler Retrofit



600 MW B&W PC Fired Boiler



CCS Re-Engineered PC Boiler 600 MW – 6 GC's, 24 Burners



Capital & O&M Cost Assessment

FGD + SCR + Baghouse vs. CCS + Baghouse

600 MW Power Plant - PRB Coal (Estimated)

600 MW Power Plant - PRB Coal (Estimated)											
Control Technology Retro		Retrofit Cost (\$/kW)) Fuel Cost (\$/Yr)		Fixed + Variable O&M Cost (\$/Yr)		Operating Cost (\$/kW-hr)				
FGD + SCR + E	Bag house	\$ 1,165	\$	80,000,000	\$	24,000,000	\$	0.0200			
CCS + Bag	house	\$ 425	\$	70,000,000	\$	11,000,000	\$	0.0154			
Delta Sav	ings	-64%		-14%		-54%		-23%			
	60	0MW Boiler	GI	VEN / ASSU	MED	Parameter					
Stack Temperature		perature	325			F					
Heat Rate - Net		Net	9600			Btu/kWh					
Plant efficiency		ncy	35.5			%					
Main Steam Pressure		n Pressure	2440			psig					
Main Steam Temperature			980		F						
Main Steam Flow			4250		KLB/h						
Boiler Feed Water Temperature			425		F						
	Boiler Feed Water Flow			4250		KLB/h					
	Low NOx Burners - LOI			7		%					
Coal Cost - PRB, Black											
Thunder			40		\$/ton						
Capacity Factor			80			%					
	FGD - SCI	R Systems		NONE							

Re-Engineered Power Plant with CCS & Coal Beneficiation Processes

Stack Emissions Estimate* firing PRB coals (1.2 lb. SO₂/mm Btu Coal)

- SO₂ = < 0.2 lb./mmBtu (< 105 ppm) ~80% reduction
- NO_x = < 0.10 lb./mmBtu (< 75 ppm)
- CO = < 100 ppm</p>
- LOI = < 1% (very low carbon in ash)</p>
- $SO_3 = < 0.1 \text{ ppm}$ (condensable particulate)
- Mercury = < 40 ppb</p>
- Particulate = < 0.03 lb./mmBtu (bag house)</p>
- Boiler Efficiency = 2 10% increase

Preliminary estimates of performance, includes bag house – no guarantees

CCS Features

Improved Operability, Availability & Reliability

- All equipment off-the-shelf & familiar to the Operators
 - Safe, stable operation,
 - Same startup, shutdown and turndown as a PC burner
- Bottom Ash (slag) removed before furnace
 - low particulate/ash load; clean furnace, less soot blowing
- Sulfur removed from furnace gases near-zero SO₃:
 - Allows for lower furnace exit temperatures
 - Minimize water-wall wastage & corrosion,
 - Can use hot boiler exhaust for pulverizer sweep air:
 - Dry the coal reject moisture
 - Improves coal pulverizer safety from fire & puffs (low O_2)
- Improved Boiler Efficiency (2 to +10%)

 - Reduce CO₂ emissions
 High combustion efficiency (LOI < 1%)
- Limestone is only "chemical" required
- No waste water for disposal

CCS Summary (Key Strategic Issues)

- From Fundamental Combustion Theory to Commercial Operation
- Fire lower cost coals reduce plant operating cost
- Meets EPA's new stringent CAIR initiatives for SO₂ & NO_x
- Allow power plant upgrade with waiver of NSPS & PSD No NSR
- May generate $CO_2 SO_2 NO_x$ emission credits
- Low Retrofit Cost; maintain older, smaller power boilers competitive - improve capacity factor & dispatch
- Fits within Plant & Boiler Site Footprint
- No waste water discharge
- Coal waste is inert and may be land filled
- Ash products have value (sell bottom ash & fly ash)
- No Hazardous or Toxic Chemicals Required

It's ADVANCED COAL GASIFICATION TECHNOLOGY!

CastleLight Energy Corp Re-Engineering Programs

- CastleLight Energy Corp. provides advanced environmental engineering consulting services.
- Re-engineer / upgrade gas, oil and coal-fired plants:
 - To burn coal with reduced operating cost
 - Extend competitive life for 20 or more years
 - And meet stringent new EPA emission regulations.

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