

**McIlvaine “Hot Topic Hour”  
April 14, 2011**

**Mercury Oxidation Test Program Results**

Presenter:

John Cochran

CERAM Environmental, Inc.

+1 913 239 9896

[john.cochran@ceram-usa.com](mailto:john.cochran@ceram-usa.com)

Co-Author:

Andreas Klatt

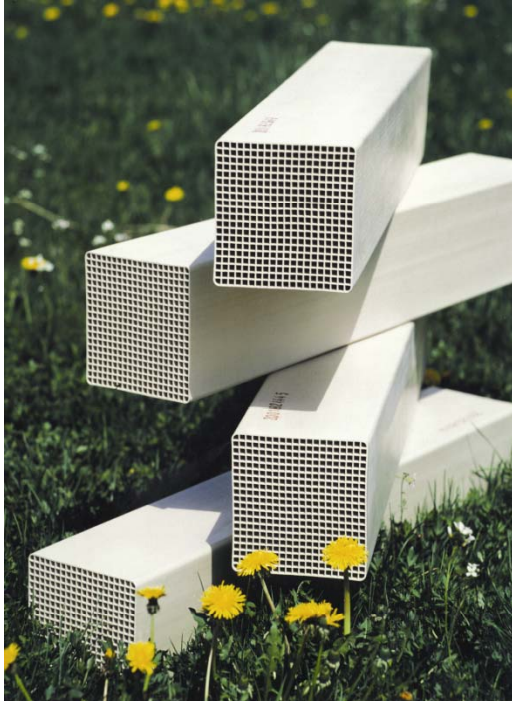
Porzellanfabrik Frauenthal (CERAM)

+49 9574 651277

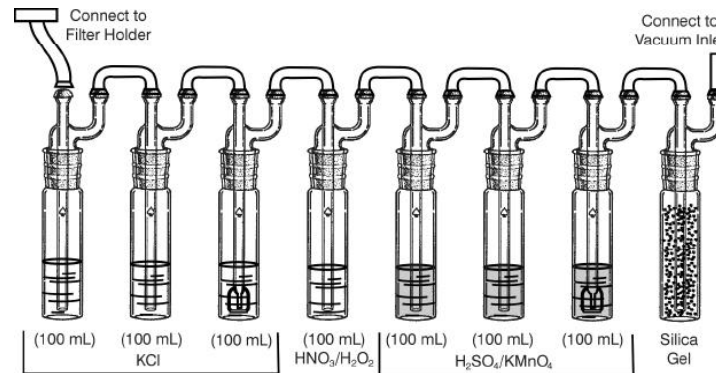
[andreas.klatt@frauenthal.net](mailto:andreas.klatt@frauenthal.net)



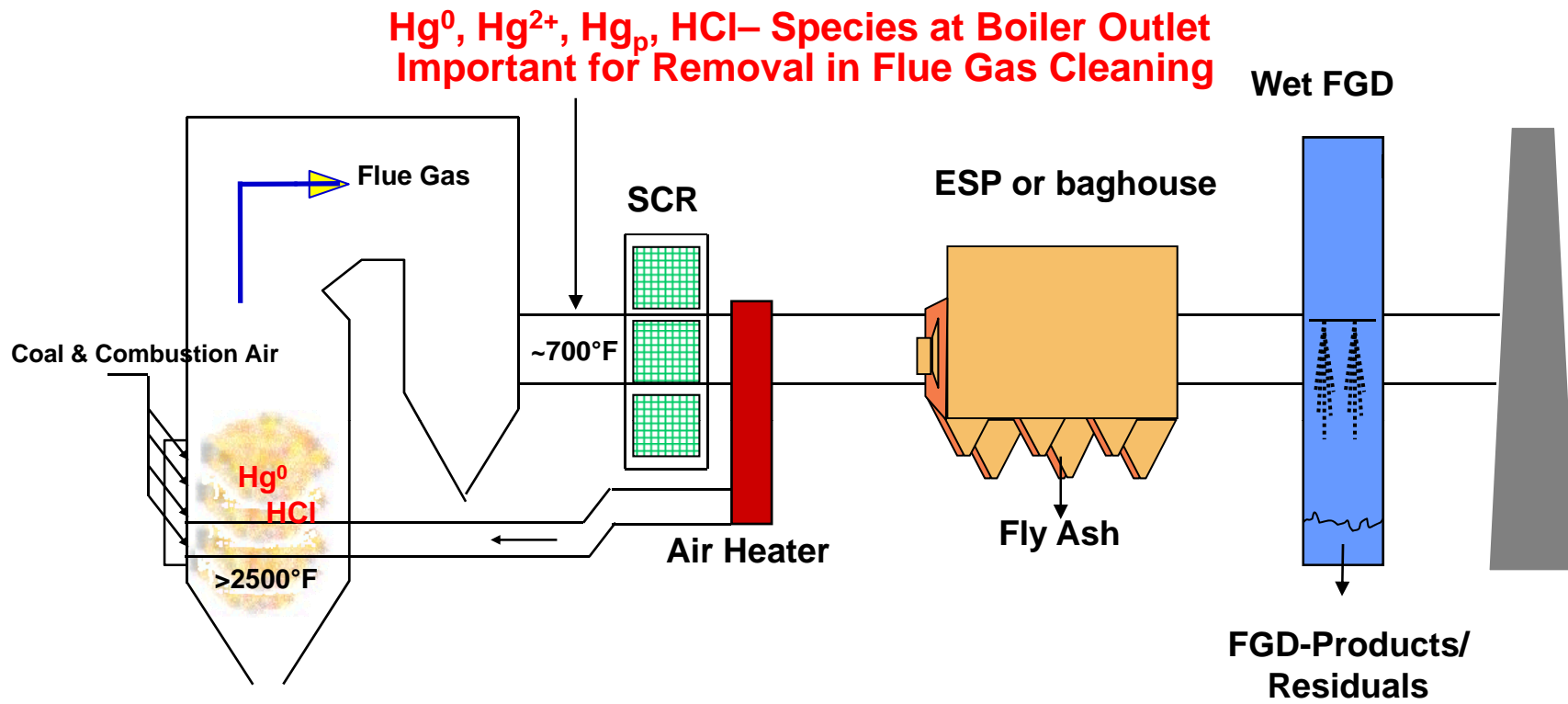
# Presentation Topics



- Main Reactions on SCR Catalyst
- Mercury Oxidation Characterization and Optimization Test Program
  - Test Plan and Objectives
  - Pilot, Bench, Full Scale Results
  - Simulation Modeling Results
- Representative Full Scale Results
- Low Temperature Mercury Oxidation



# Example of Flue Gas Cleaning System in Power Plants

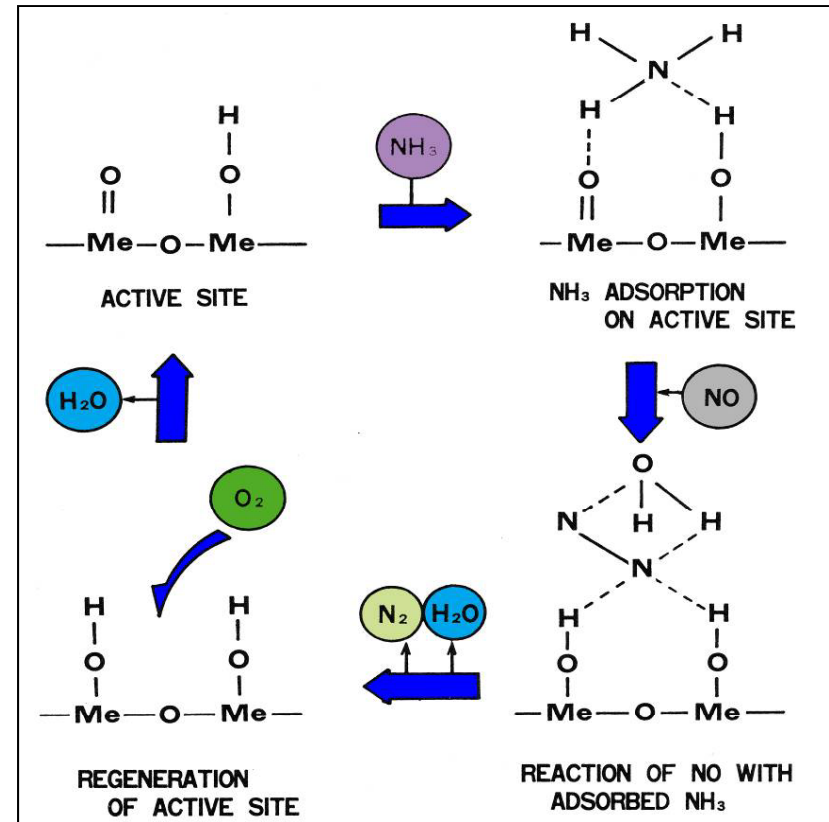


- Use Existing Flue Gas Cleaning Systems for Mercury Removal
  - Hg Oxidation on SCR Catalyst
  - Removal of Particulate Hg (ESP, baghouse)
  - Separation and Removal of Oxidized Hg in FGD
- Clean Air Mercury Rule (CAMR) – Reduce Hg Emissions (≈48 tons/yr Uncontrolled in U.S.)
- Combination of high-dust SCR/ESP/FGD may result in Hg removal up to 95%

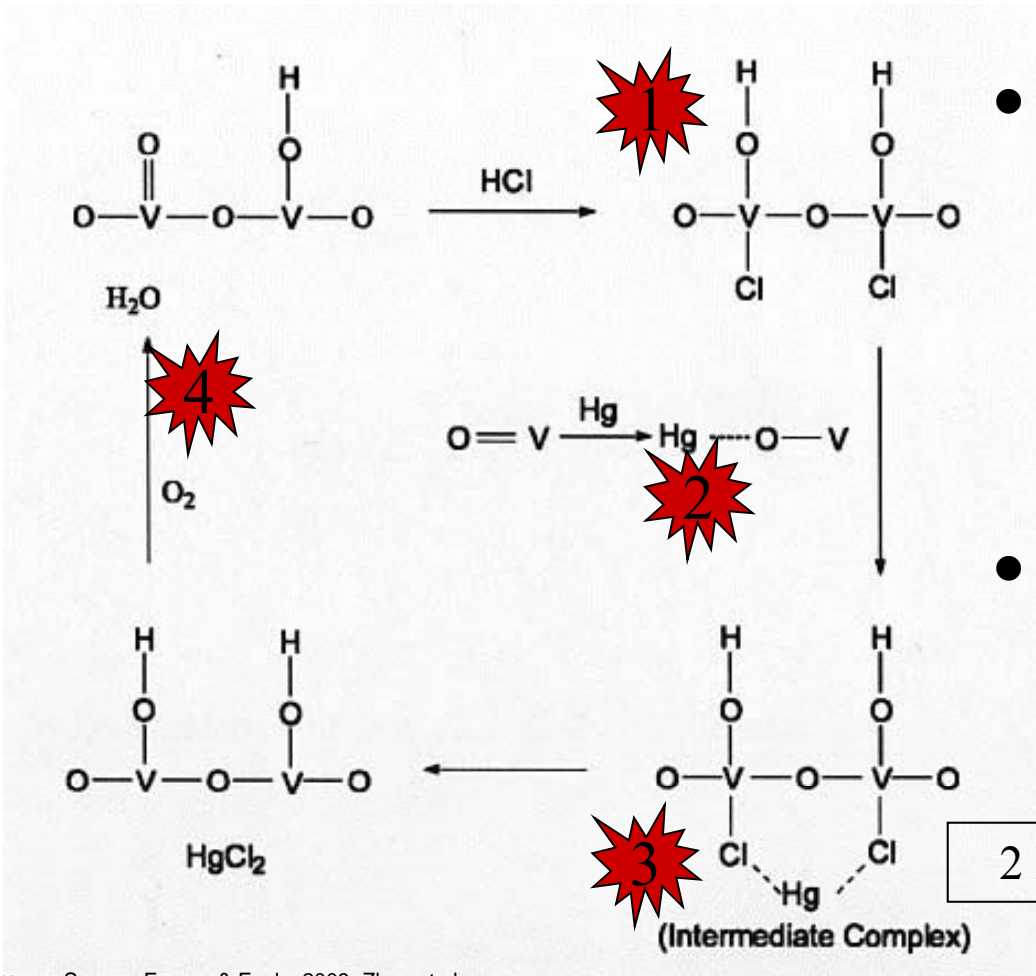
**Important Step: Hg<sup>0</sup>-Oxidation on SCR Catalyst**

# SCR DeNOx Reaction – Process Basics

- Catalyst Active Sites Constantly Being Regenerated in a Cycle
  1. Active Site Available
  2. Adsorb Ammonia
  3. Reaction of NOx With NH<sub>3</sub>
  4. Regenerate Site With O<sub>2</sub>
- Active Sites **Not Busy** With NOx Reduction (Ammonia) **Available** For Oxidation of SO<sub>2</sub>, Hg<sup>0</sup>, Unburned Hydrocarbons, VOC, Dioxins, etc.



# Hg Oxidation With Titanium/Vanadium SCR-Catalysts

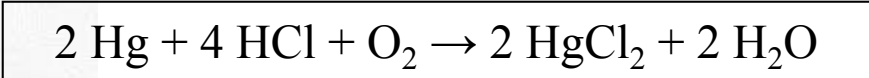


- **Langmuir-Hinshelwood-Mechanism at adjacent active sites**

1. HCl adsorb onto V sites
2. Reactive Cl generated
3. Weakly adsorbed Hg<sup>0</sup>
4. O<sub>2</sub> re-oxidizes active sites

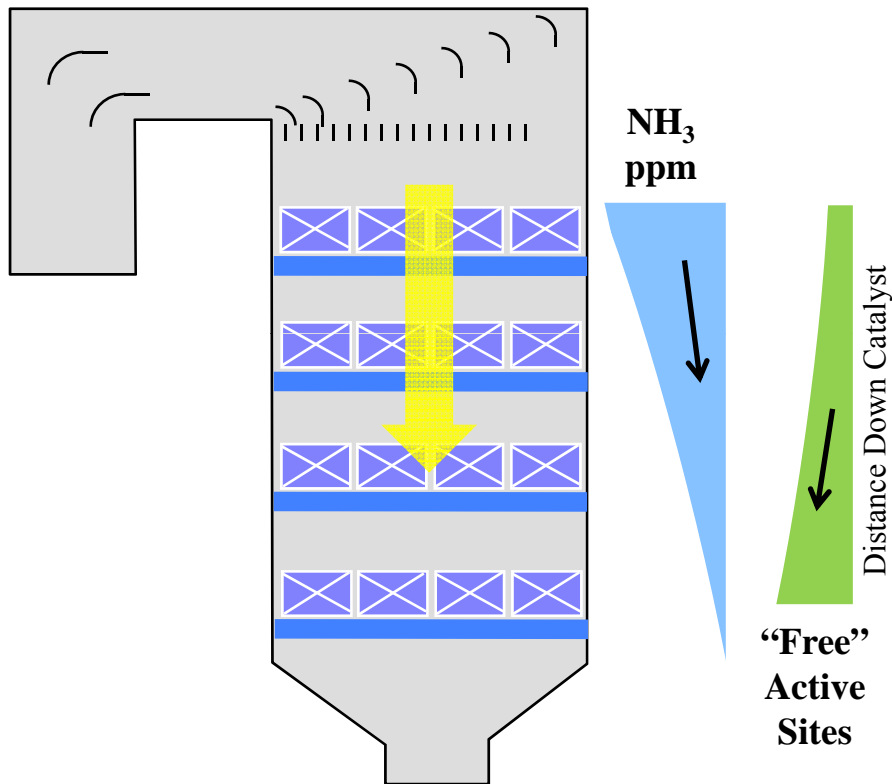
- **Deacon Reaction**

1. V<sub>2</sub>O<sub>5</sub> and HCl React to Produce Cl<sub>2</sub> Which Reacts With Hg<sup>0</sup>

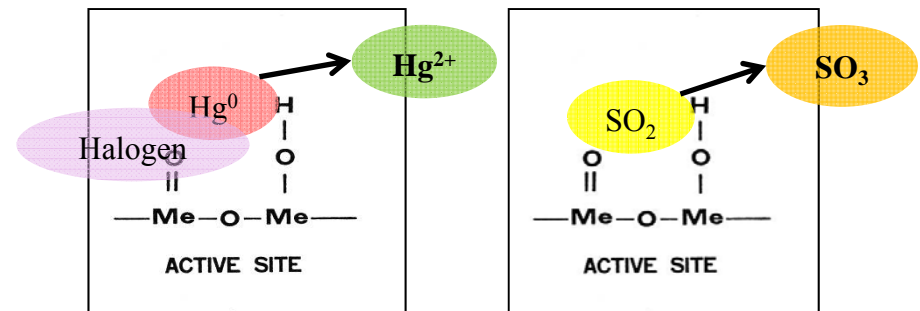


Source: Energy & Fuels, 2009, Zhou et al..

# Oxidation Rates Vary Based on Location in the Reactor



- Ammonia Concentration Decreases as Flue Gas Flows Down Through Catalyst Layers
  - Surplus or “Free” Active Sites Increase Down Through Reactor
- Surplus Active Sites Result in Increasing Rate of...
  - SO<sub>2</sub> to SO<sub>3</sub> Oxidation
  - Mercury Oxidation
  - Dependent on Catalyst Aging



# CERAM Participating in Comprehensive Mercury Oxidation Test Programs

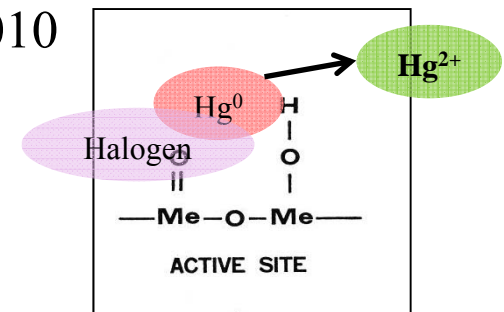
- CERAM Working to Optimize Mercury Oxidation Potential in Extensive Pilot/Demonstration Programs
- European Research Project **DENOPT**  
Research Fund for Coal and Steel RFCR-CT-2007-00008
- Participants - ENEL, E.ON, EnBW, CERAM, Reaction Engineering, University of Stuttgart, and RECOM Service
- Test Approach:
  - Evaluating Different Catalyst Compositions
  - Evaluating New, Deactivated, and Regenerated Catalyst
  - Bench and Pilot Scale Tests
  - Full Scale Tests (600 MW PC) When Firing Coal and Co-Firing Coal and Biomass
  - CERAM is the Only Catalyst Supplier Participating





# CERAM Participating in Comprehensive Mercury Oxidation Test Programs

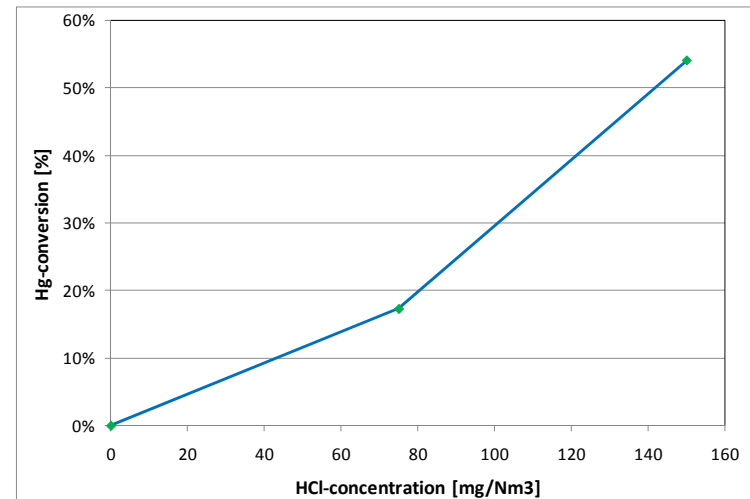
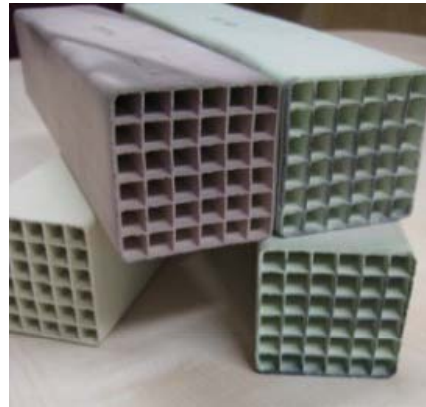
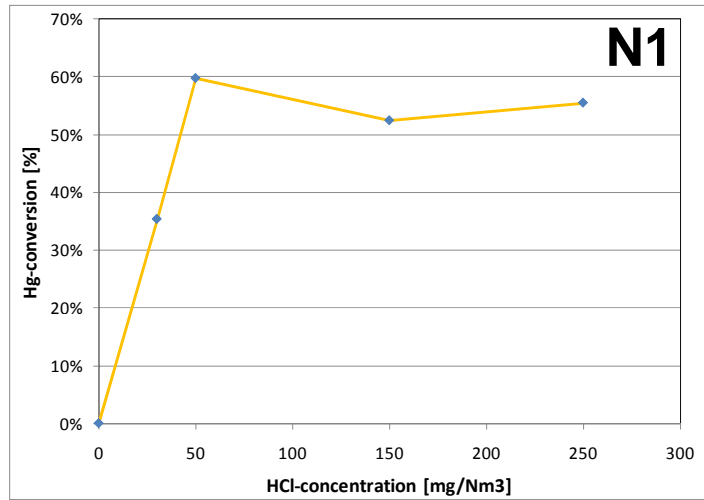
- Program Objectives:
  - Fully Characterize Oxidation Reactions – Develop Mathematical Model
  - Evaluate Commercial and Innovative Low and High Temperature Catalyst Compositions Directed at Promoting Mercury Oxidation
  - Assess Catalyst Effects on Mercury Speciation for Different Coals
  - Investigate Effects of Operating Conditions (Area Velocity, Catalyst Age, and Deactivation Levels) on Oxidation Rate
  - Optimization of SCR Catalyst Performance Related to Mercury Oxidation and Limiting Deactivation
- Program **DENOPT** completed June 2010
  - Research has Expanded CERAM's Knowledge Base Regarding Hg Oxidation Reaction Mechanisms and Kinetics
- Second Program **DEV**CAT (**DE**velopment of High Performance SCR **CAT**alyst Related to Different Fuel Types) started July 2010 (ongoing for three years)





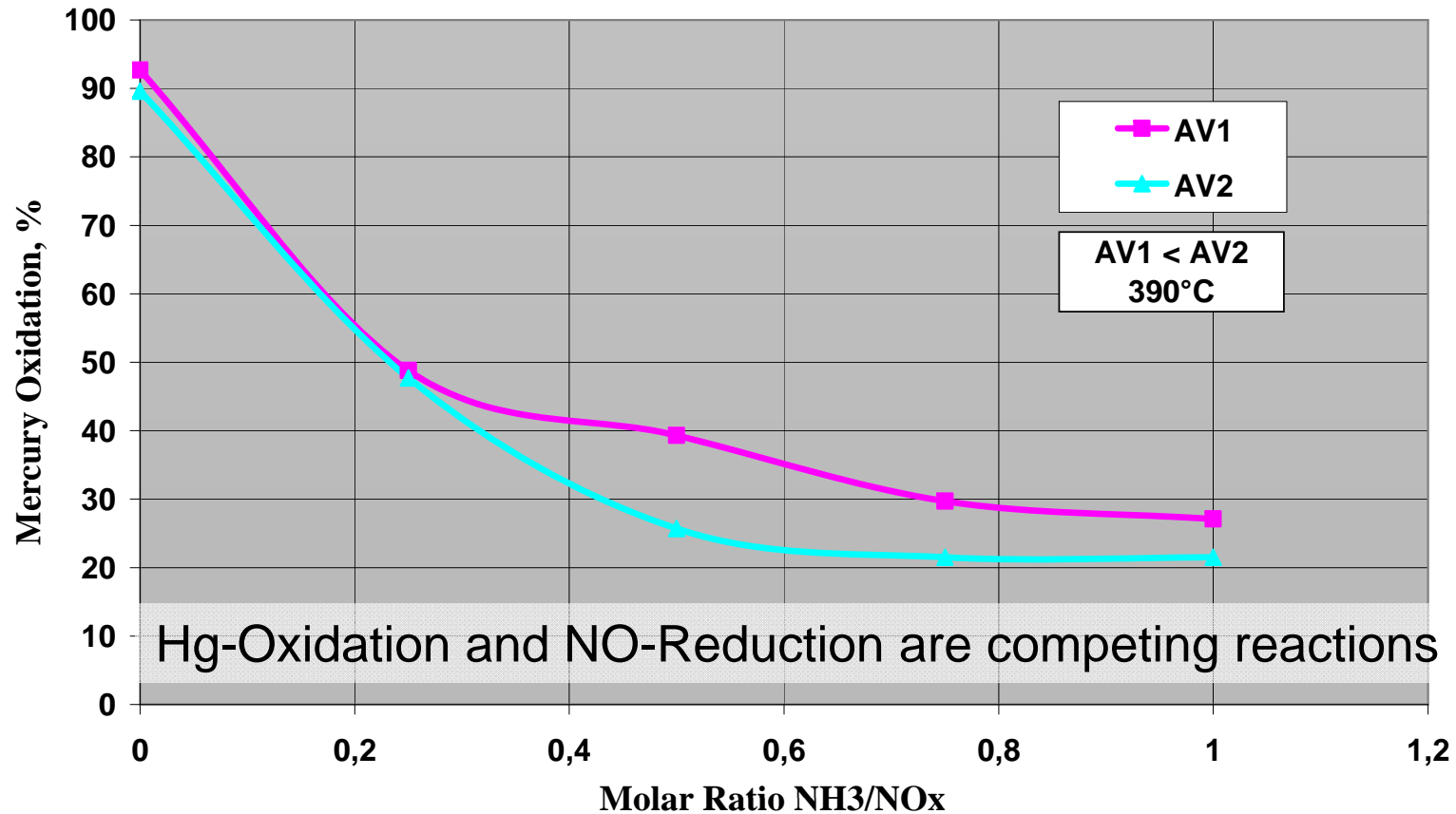
# Micro-scale Reactor Tests on Different Catalysts

## Influence of HCl-concentration



# Influence of Molar Ratio $\text{NH}_3/\text{NO}_x$

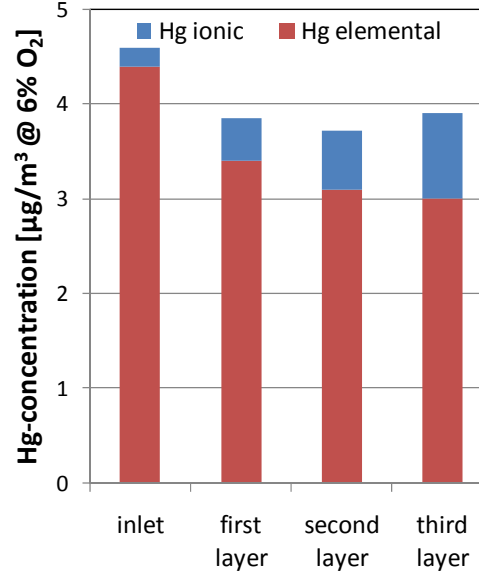
## Hg-Oxidation an CERAM-Wabenkatalysatoren



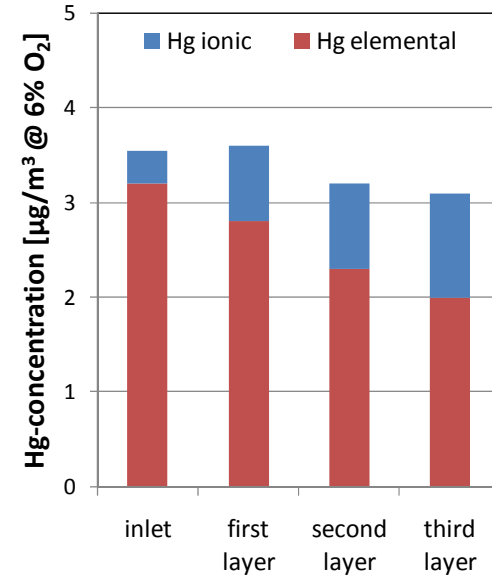
# Tests Results for 500kW Test Rig



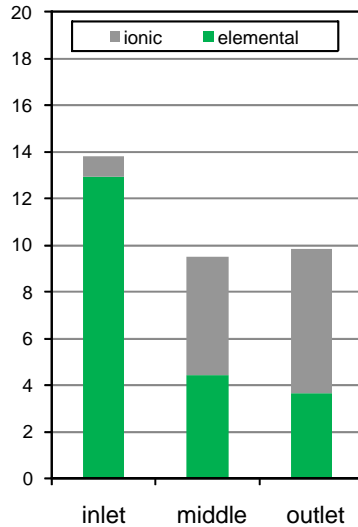
Coal – Catalyst 1



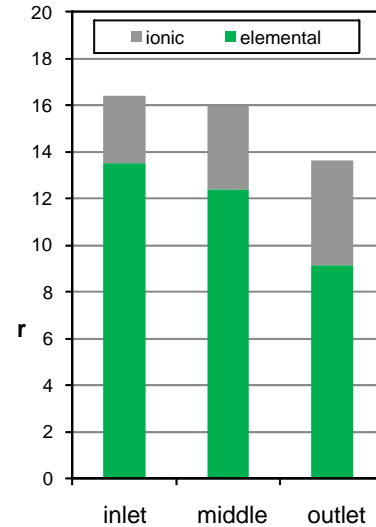
Coal – Catalyst 2



coal + sludge



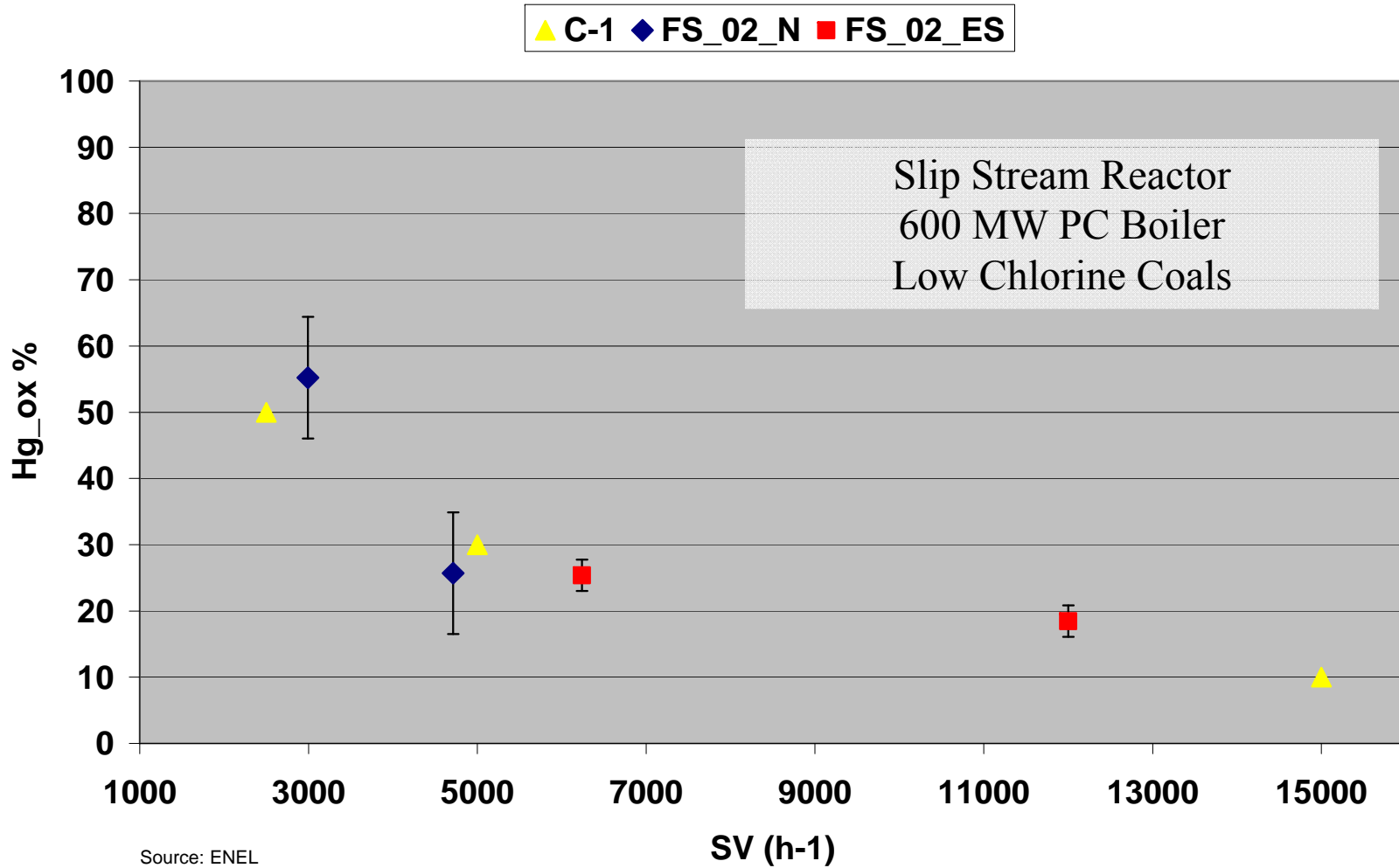
coal + sludge + NH3



Universität Stuttgart

ifk

# Influence of Space Velocity (SV) on Hg<sub>ox</sub> %



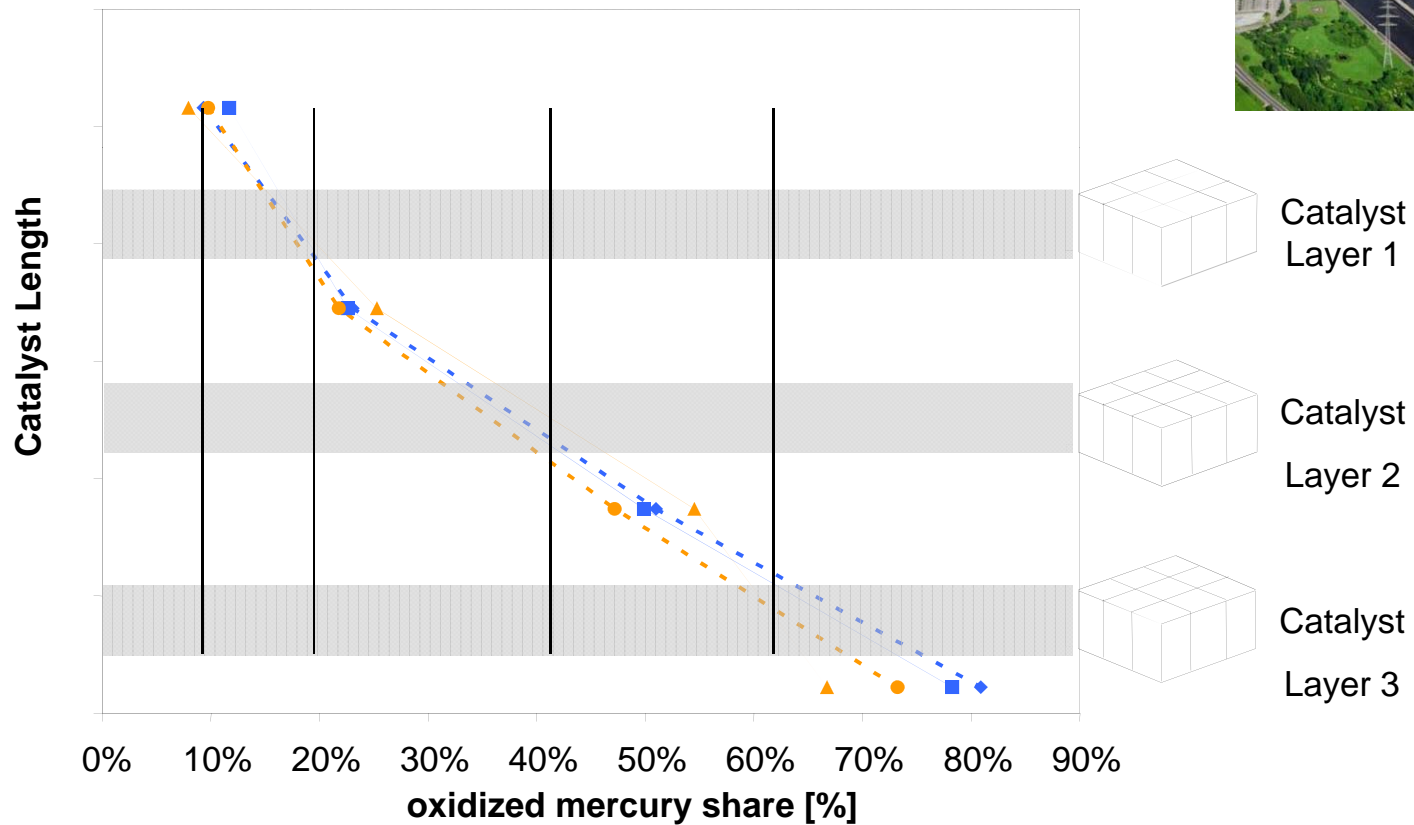
# Power Plant Measurements

600 MW PC Boiler

High-Dust SCR

3 Honeycomb Catalyst Layers

High Chlorides (~900 ppm in coal)

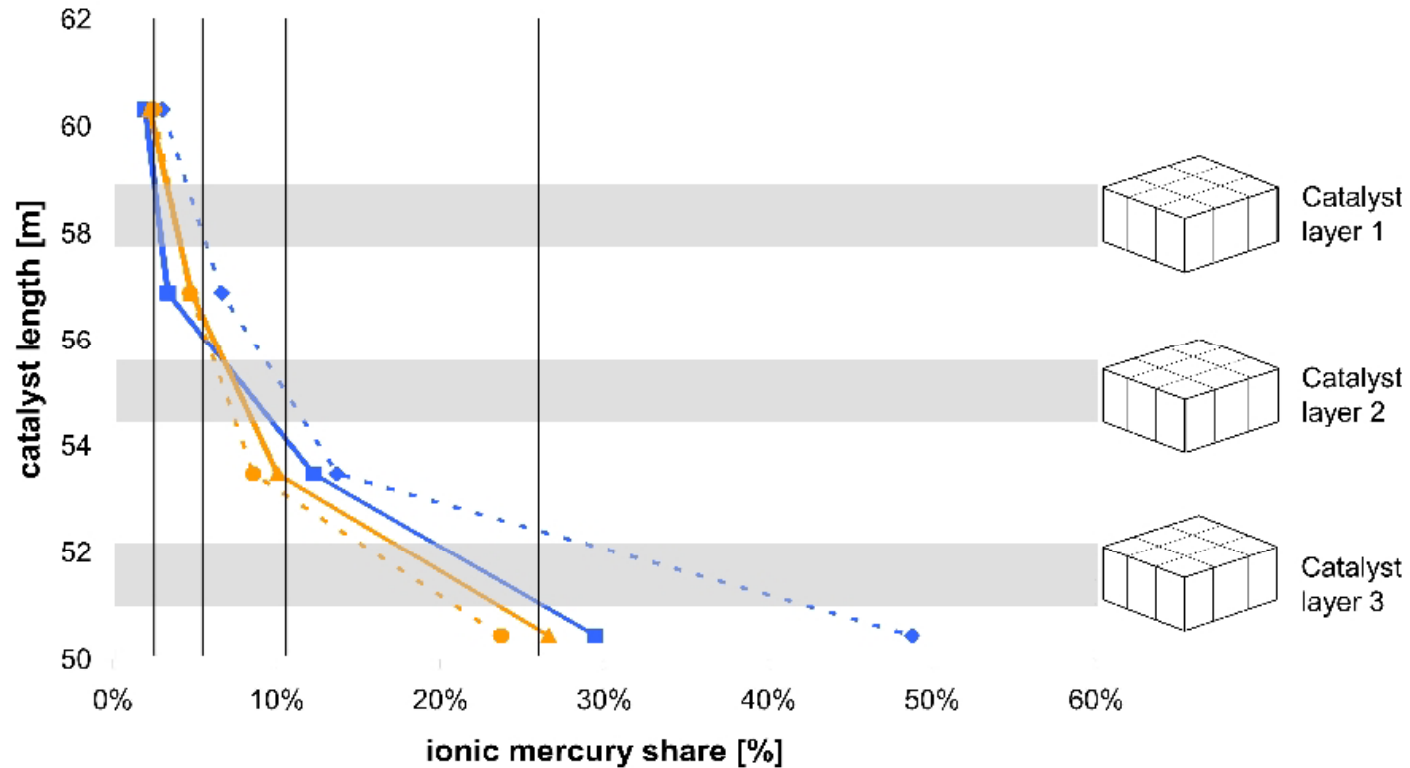


# Power Plant Measurements

## 2nd Measuring Campaign

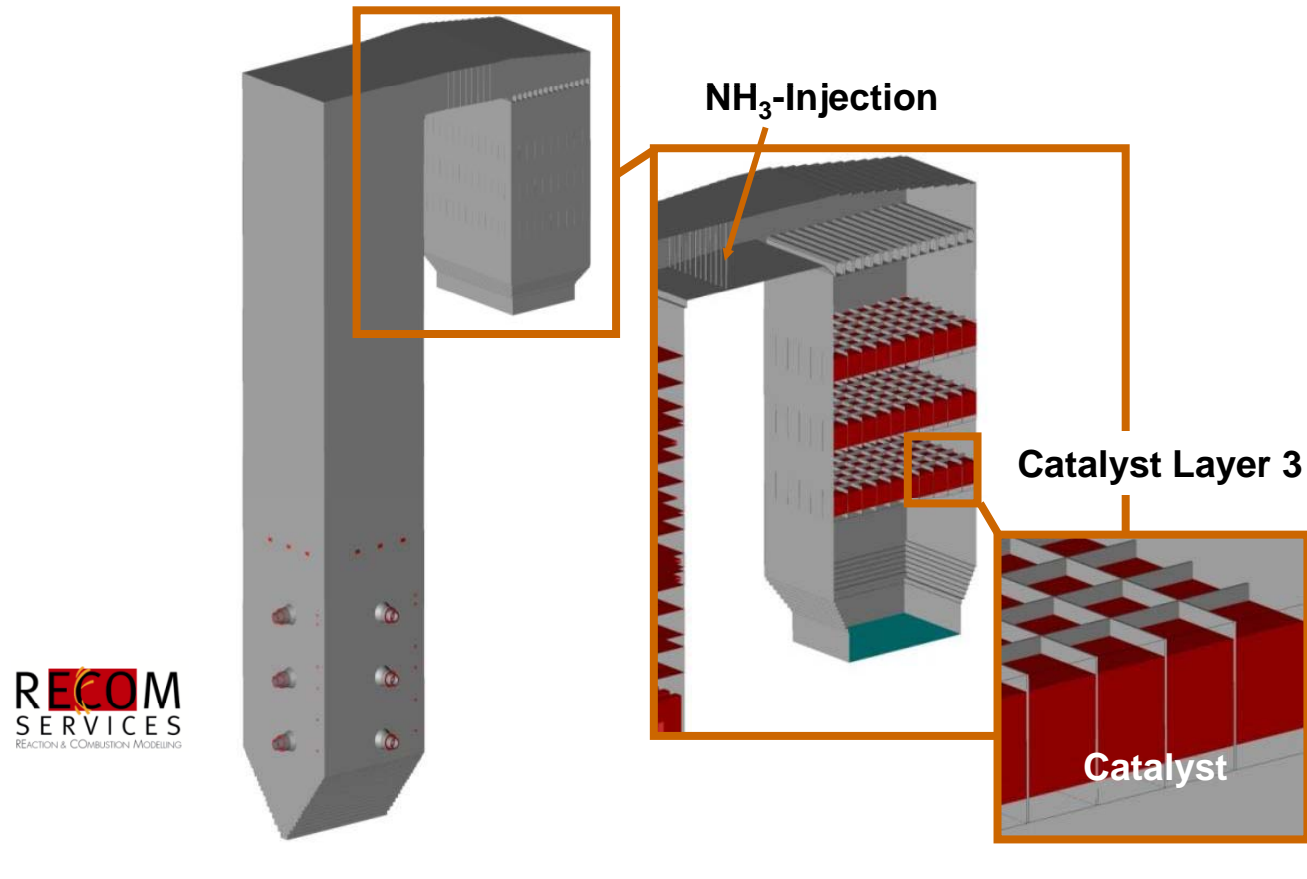
Coal Chlorine 62 ppm

Sulfur 0.43%



# Implementation into Simulation Model

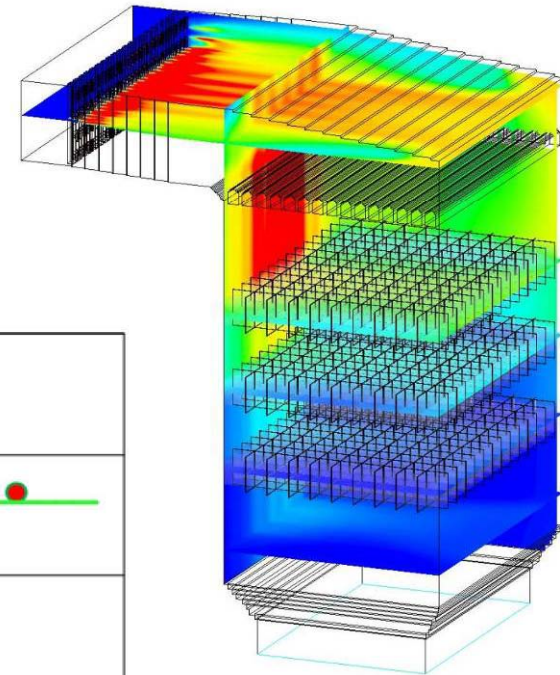
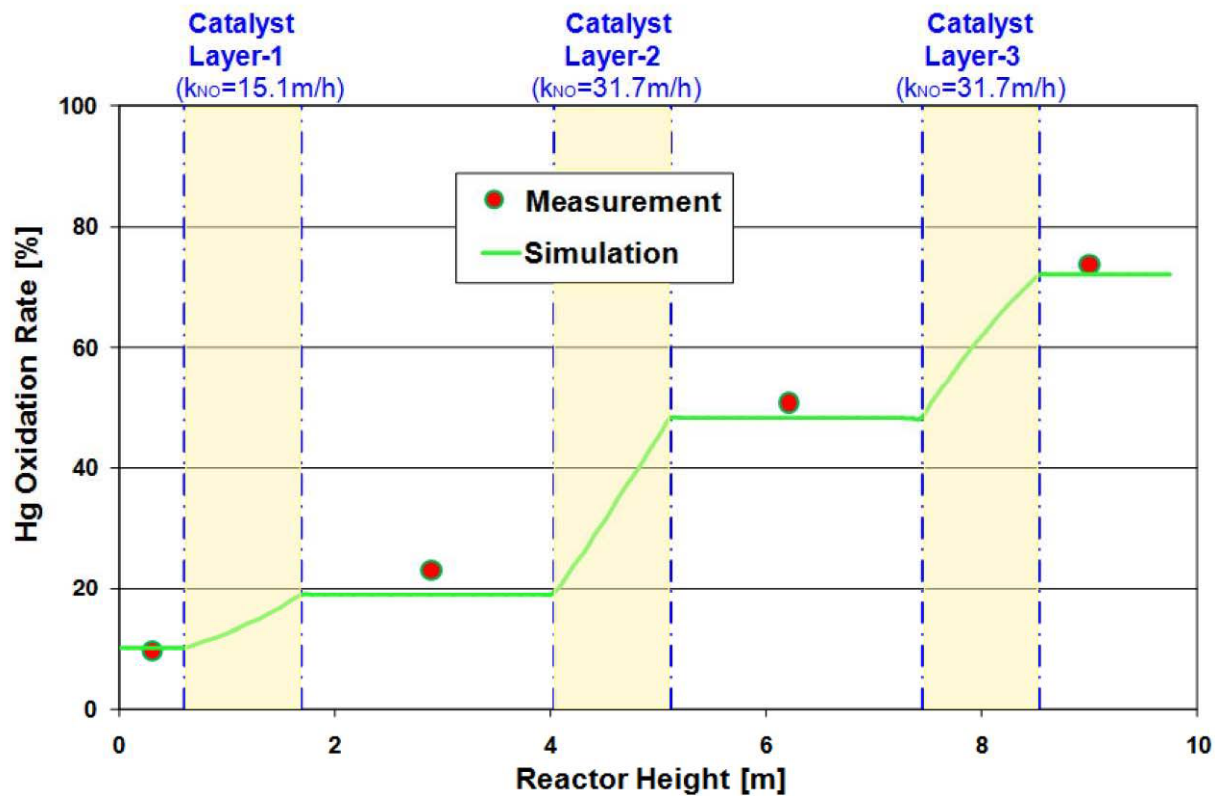
- Use Existing 3D-CFD Simulation Model for Boiler
- Developing and Applying New Model for SCR system
- Implementation of Catalyst Chemistry ( $\text{NO}_x$ , Hg,  $\text{SO}_2/\text{SO}_3$  conversion)
- Input Data from Full-scale and Lab Measurements for Model Validation





# Assessment of Model Predictive Quality

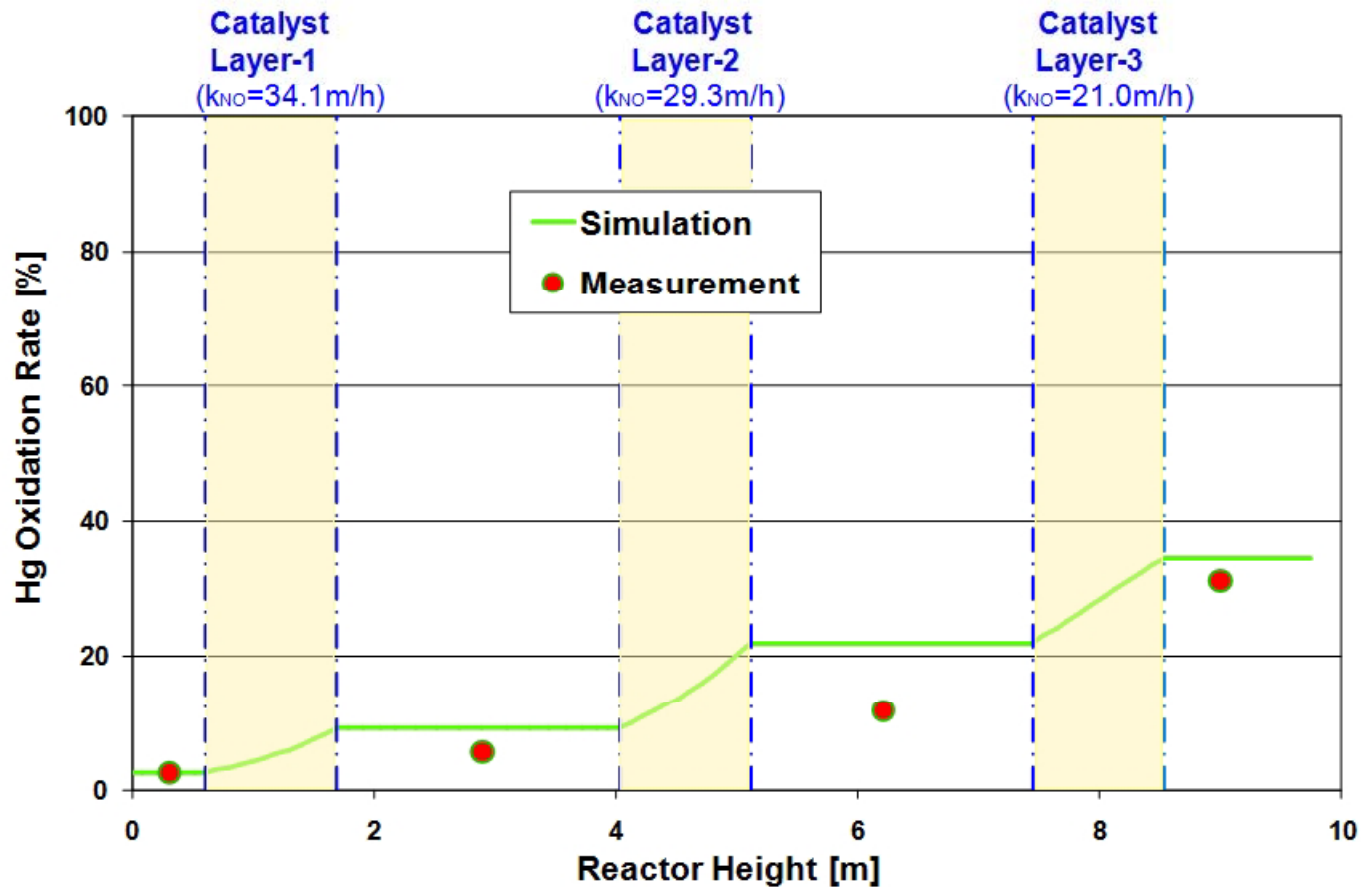
Hg Oxidation Rate along Reactor



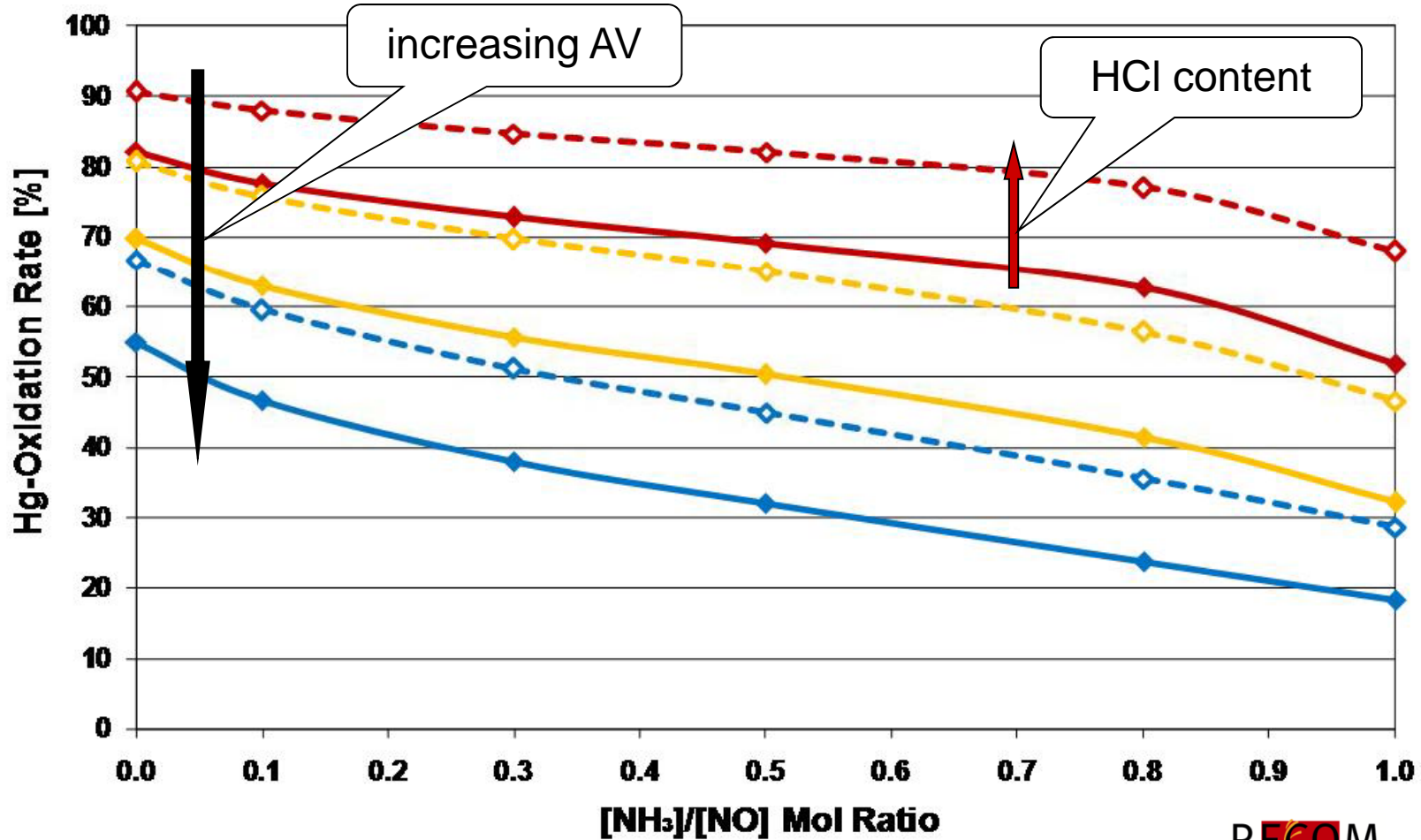
**RECOM**  
SERVICES  
REACTION & COMBUSTION MODELING

# Assessment of Model Predictive Quality (2)

Hg Oxidation Rate along Reactor



# Mercury Oxidation Kinetic Model



# Representative U.S. Results for CERAM Catalyst

	Plant 1	Plant 2	Plant 3
NOx Removal	>91%	>90%	>92%
Coal Sulfur	>3%	>3.5%	>3.5%
Coal Chlorine	0.13%	0.15%	>0.1%
Operating Temperature	700 F	720 F	770 F
SO <sub>2</sub> to SO <sub>3</sub> Conversion Rate Across Reactor	<0.5%	<0.5%	<0.5%
Catalyst Layer Design	3+1	3+1	2+2
Catalyst Age	4,000 hr (3)	4,000 hr (1) 21,000 hr (3)	21,000 hr (2)
Mercury Removal	>95%	>80%	>85%

# Summary

- CERAM Participating in Comprehensive Long Term Mercury Oxidation Characterization and Optimization Test Program
  - DENOPT Program Complete
  - DEVCAT Program Ongoing Through 2013
- Mercury Oxidation Reactions are Complex and Vary as a Function of...
  - Flue Gas Composition (HCl, Other Halogens, SO<sub>2</sub>, etc.)
  - Reactor Operating Conditions (NH<sub>3</sub>/NO<sub>x</sub>, Area or Space Velocity, Temperature, etc.)
  - Catalyst Composition
  - Surplus Reactor Potential Present
  - Exposure to Flue Gas (Catalyst Aging)
  - Mercury Oxidation Possible with Low SO<sub>2</sub>/SO<sub>3</sub> Oxidation Catalyst
- Simulation Model Developed to Better Predict Performance
- Low Temperature Mercury Oxidation Process is Developmental but Promising