

# Meeting Regulatory Needs with Hydrated Lime

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*June 22, 2012*

# Regulatory Reasons for Acid Gas Mitigation

- Pre-MACT

- Offset additional SO<sub>3</sub> generated from SCR installation
- Control blue plume at stack from Wet FGD addition
  - Appearance
  - Local concerns

- Future

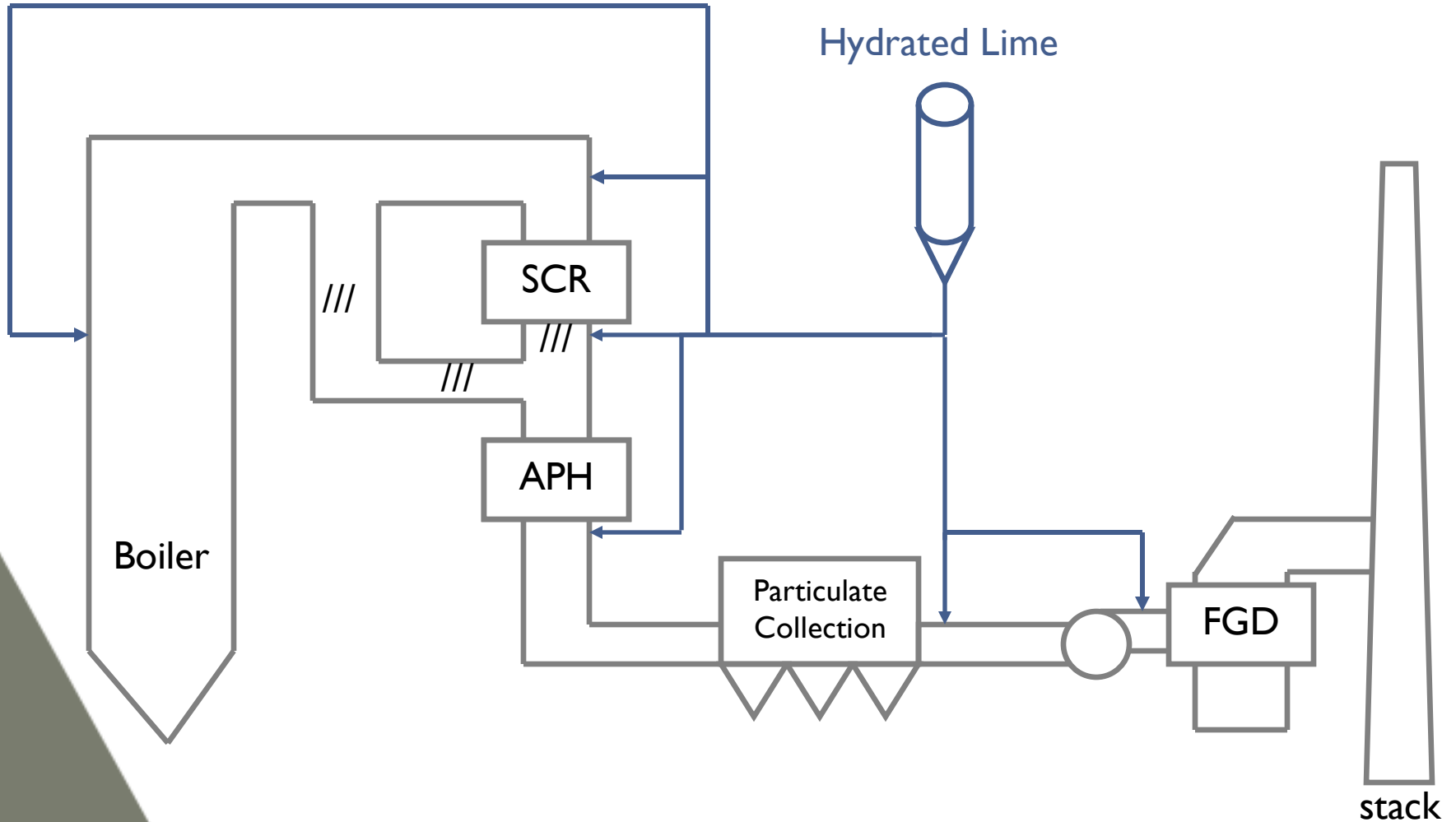
- Consent decree on acidic gases
  - Specified amount at the stack
    - Limitations of Method 8A
- Particulate
  - 0.030 lb/MM Btu (filterable)
- HCl as acid gas surrogate
  - 0.002 lb/mmBTU
  - Protection of PAC for Hg control
- Consistency and OST of mitigation system will be critical



# Questions to Answer

- Are you buying tons or moles of sorbent?
  - Forecast annual usage in tons for comparison of sorbents
- Where are you and where do you have to get with pollutants?
  - Potential side benefits of acid gas mitigation
  - Hydrated lime effective for  $\text{SO}_3$  and  $\text{HCl}$  at a wide temperature range
- What will your injection system look like?
  - Expectations on Operations and Maintenance
  - Hydrated lime systems with good design principles are in place and working well in the industry
- Implications of sorbent choice
  - Supply
  - Solid, multi-location supply base
  - Logistics
  - Availability via truck or rail; low working capital and short lead time
  - Ash
  - No leaching issues

# Injection Location Options for Hydrated Lime



# Acid Gas Emission Control – Baghouse Shawnee



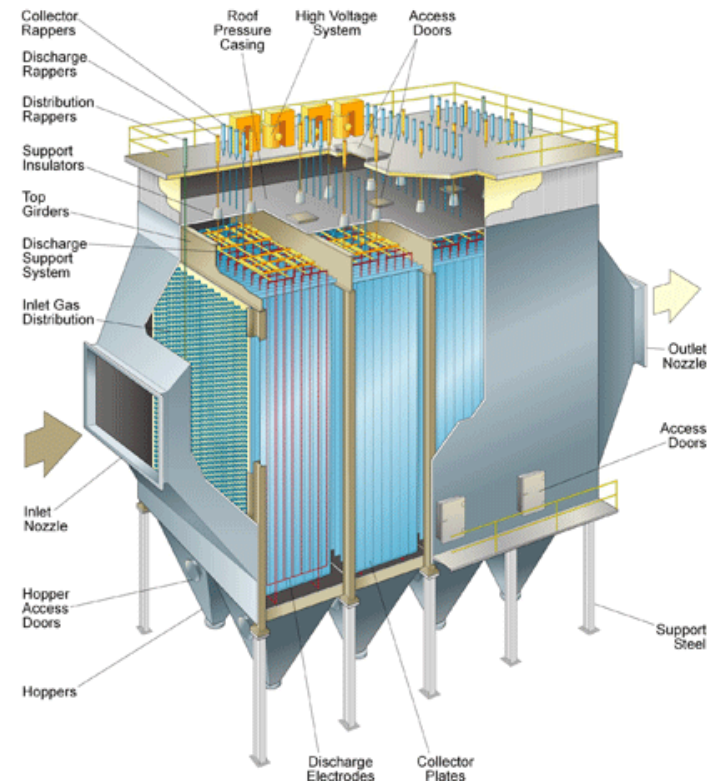
## DSI Program targeting HCl emissions to meet 2015 MATS

- Baghouse seasoning is essential for test program (*yellow vs green*)
- HCl limits easily met with low hydrate requirements
  - Lower limit of feeder capability for consistency
- Results of follow-up study also optimistic

Hydrate Injection Rate	HCl (lb/MMBTU)	HF (lb/MMBTU)	H <sub>2</sub> SO <sub>4</sub> (ppmvd)
0 lb/hr - Baseline	0.0030	0.0045	1.3
600 lb/hr (in flight)	0.0016	0.0046	0.46
1,000 lb/hr (in flight)	0.0016	0.0043	0.42
350 lb/hr	0.0005	0.0006	0.37
350 lb/hr	0.0007	0.0007	0.35
300 lb/hr	0.0008	0.0006	0.35

# SO<sub>3</sub> Control with Hydrate ESPs

- SO<sub>3</sub> conditions ESP
- Ash resistivity
  - Sodium reduces; Calcium increases
- Strategy for Unit-specific issues
  - Distribution of particulate in duct
  - Balance hydrate feed and SO<sub>3</sub> levels
    - Important to maintain ESP conditioning
    - ~3ppm SO<sub>3</sub>
  - Short Residence time in front of ESP
    - Manage with split injection



*Courtesy B&W*

Lodge Cottrell presentation from 2011 APC conference  
– Reinholdenvironmental.com library section

# Typical SO<sub>3</sub> Removal Rates - ESP systems

- Residence time effects
  - Short (<2 sec) will require more sorbent
- Injection system efficiencies
  - Flue gas coverage
  - Feed system

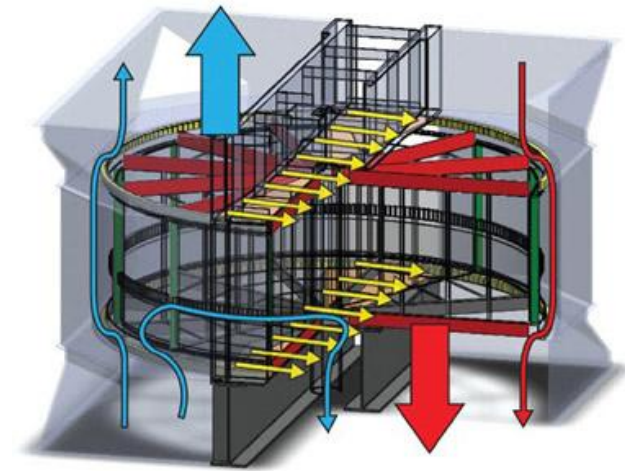
## *Removal Rate Examples Using Hydrated Lime*

Plant	<i>lb hydrate: lb SO<sub>3</sub></i>	Treated Stack
550 MW	3.9 : 1	<1.5 ppm
1300 MW	3.9 : 1	3 ppm
700 MW	3.5 : 1	3.5 ppm
>500 MW	1.9 : 1	<6 ppm
	3.8 : 1	<2 ppm
>500 MW	2.5 : 1	4 ppm
	3.9 : 1	<2 ppm

# Hydrate Prior to Air Preheater

Hot side injection offers additional benefits:

- Better utilization of sorbent
  - Longer reaction time
- APH operation
  - Eliminate ABS buildup from ammonia slip
  - Flexibility on SCR operation
- Lower heat rate
  - Reduce acid dew point through APH



*Courtesy BreenES*

Neutralization of  $\text{SO}_3$  by hydrate will occur at pre-APH temperatures

- Sodium sorbents:
  - Byproducts and intermediates can form without temperature and concentration control
- Calcium sorbents
  - No issues with reaction byproducts or intermediates
  - Multiple trials of Pre-APH since '09
  - Utility – Pre-APH since 2010
    - No issues reported



# Pre-SCR Injection with Hydrated Lime for SO<sub>3</sub>

- Potential benefits
  - Residence time
  - Mixing/sorbent utilization
- Initial program
  - Unit <250MW
  - Bituminous coal
  - Injected over several days
- Observations
  - No operational issues during this limited test period
  - Noticeable reduction in hydrate required to achieve low SO<sub>3</sub> levels measured at APH outlet (vs injection at SCR outlet)
- Additional testing planned



# Summary

Hydrated lime DSI is effective for acid gas mitigation

- Meeting HCl MATS Requirements
- ESP applications
- Pre-APH
  - Additional benefits of early  $\text{SO}_3$  removal
- Interesting results with Pre-SCR injection

# Contact Information

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