



## **Dry Sorbent Injection and Gas Co-Fire / FLGR for Small to Medium Plants**

**McIlvaine Hot Topic Hour:**

**Dry Sorbents and Systems and Material Handling in Coal-fired Power Plants**

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# The Balance of Power

## Regulations:

MATS

CSAPR

NAAQS

Coal Residuals

Wastewater

GHG BACT

## Economics:

Fuel Cost

Fuel Flexibility (Coal V/S Gas)

Cost of Compliance

Demand

Repower?

Retire Plants?



ANCE ISSUES, MANAGING EMISSIONS, BALANCE-OF-PLANT IMPACTS, EMISSIONS CONTROL, PROFITABILITY

# THE BALANCE OF POWER

- **MATS (in effect)**
  - HCl (0.002 Lb/MMBtu) (SO<sub>2</sub> Surrogate – 0.2 lb/MmBtu)
  - Hg (1,2 Lb/Tbtu)
  - PM (0.03 lb/MMBtu)
- **CSAPR (Currently Stayed)**
  - SO<sub>2</sub> (Reduction of Approx 50 to 60 % from 2005 Levels)
  - NO<sub>x</sub> (Reduction of Approx 40 to 50 % from 2005 Levels)

- **MATS**

- HCl (Scrubber)
- Hg (SCR – Oxidizes; Scrubber – Captures)
  - ACl to Augment as necessary; *DSI can help with SO<sub>3</sub> interference*
- PM (SO<sub>3</sub> contributes to Method 5)
  - *DSI can help*

- **CSAPR**

- SO<sub>2</sub> (Scrubber)
- NO<sub>x</sub> (SCR)

- **In general, there is a path to compliance**



# Plants without SCR & Scrubber

Typically 300 MW and below



- **MATS**

- HCl (*DSI*)
- Hg (ACI + *DSI for SO<sub>3</sub>*)
- PM (*DSI for SO<sub>3</sub>*)

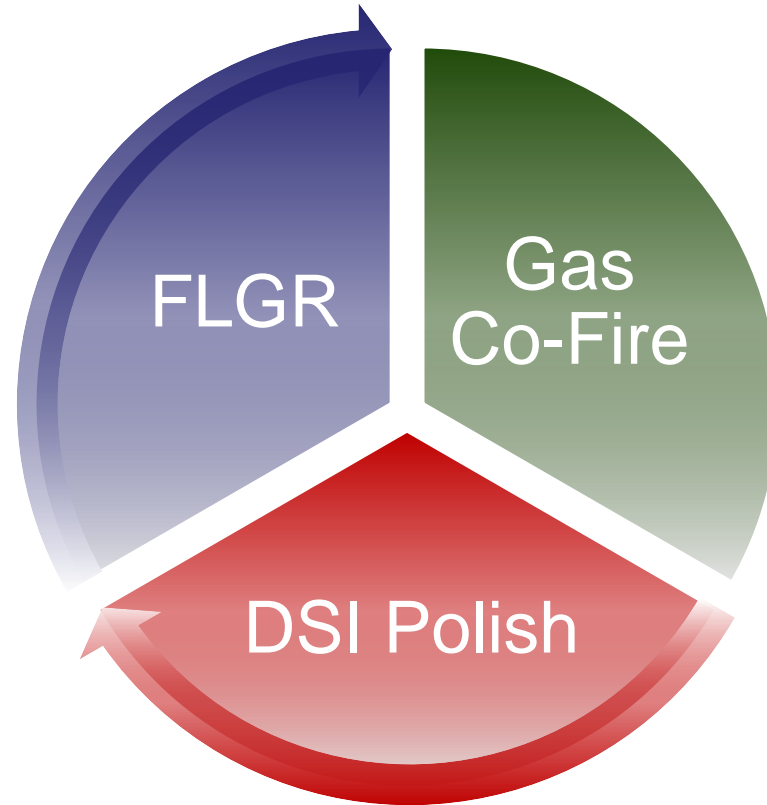
- **CSAPR**

- SO<sub>2</sub> (*DSI?*)
  - Sodium Bicarb can deliver 90% reduction. ESP Loading and Flyash sales are a concern
  - Hydrated Lime can deliver 50 to 70% reduction. ESP Loading is a concern
- NO<sub>x</sub> (SNCR?)
  - SNCR performance is limited to less than 30% and inconsistent based on temperature fluctuations and boiler operations

- **In general, not many good options available. DSI is not viable by itself.**
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## Maybe a Sequential Approach would work?

1. Convert some heat input to gas to realize  $\text{SO}_2$  and  $\text{NO}_x$  reductions and take advantage of lower fuel pricing
2. Couple the entire combustion output with FLGR to reduce  $\text{NO}_x$  with an additional  $\text{SO}_2$  drop,
3. Polish the  $\text{SO}_2$  with DSI now that the net particulate is reduced



**Partial Natural Gas Conversion**

**Natural Gas Co-Fire**



- **Uses Existing Major Assets:**
  - No Heat Transfer Modifications or Derates required
  - Allows for Fuel Flexibility as Coal/Gas Pricing moves
- **Dispatch Consideration**
  - Gas in Upper Registers can improve Load Ramp and Superheat Temperature control
  - Gas In upper registers may allow for reduced MSL
- **Co-Firing will require flexible modifications to burners**
  - Should be accomplished mill by mill
  - Introduction of natural gas ports surrounding the main coal pipe

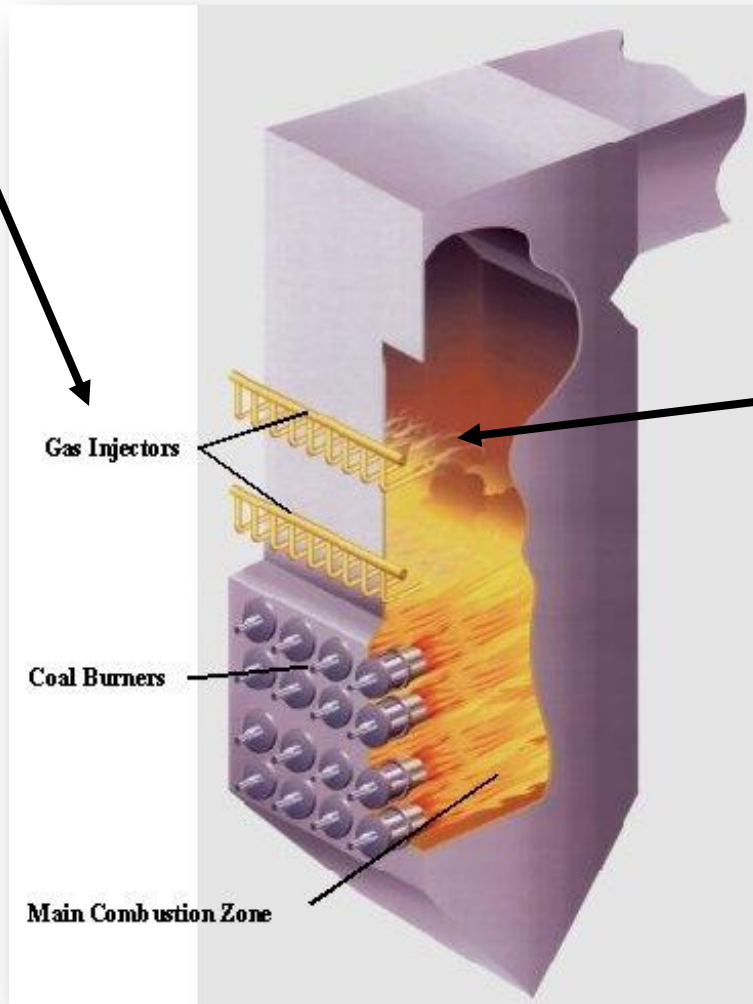


## Fuel Lean Gas Reburn



# Fuel Lean Gas Reburn (FLGR)

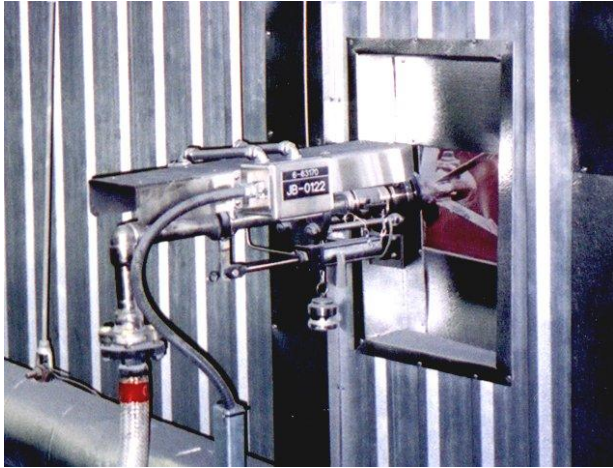
- **Injects 3 to ~10% of Fuel into Upper Furnace**



- Locally Fuel-rich Pockets with-in Fuel-lean Upper Furnace
- 3 - 5% NO<sub>x</sub> Reduction for each 1% Fuel

Commercially applied in  
13 Utility Boilers!

- Natural Gas Injected in Upper Furnace in amount sub stoichiometric to total flue gas oxygen,
- Localized gas pockets create fuel RICH zone where  $\text{CH}_4$  reduces  $\text{NO}_x$  to  $\text{NH} + \text{CO} + \text{H}_2\text{O}$
- Upon re-entrance into  $\text{O}_2$  rich zones,  $\text{CO}$  completes to  $\text{CO}_2$
- When passing the 1750 F temperature zone, some  $\text{NH}$  compound provides a secondary SNCR action



FLGR Performance:

Up to 30% NO<sub>x</sub>

Amine-Enhanced FLGR  
(AE-FLGR) can deliver 50%  
NO<sub>x</sub> reduction

SO<sub>2</sub> equal to Gas Rate



**Dry Sorbent Injection**

**Hydrated Lime/Sodium Bicarbonate**



# Equipment and Layout



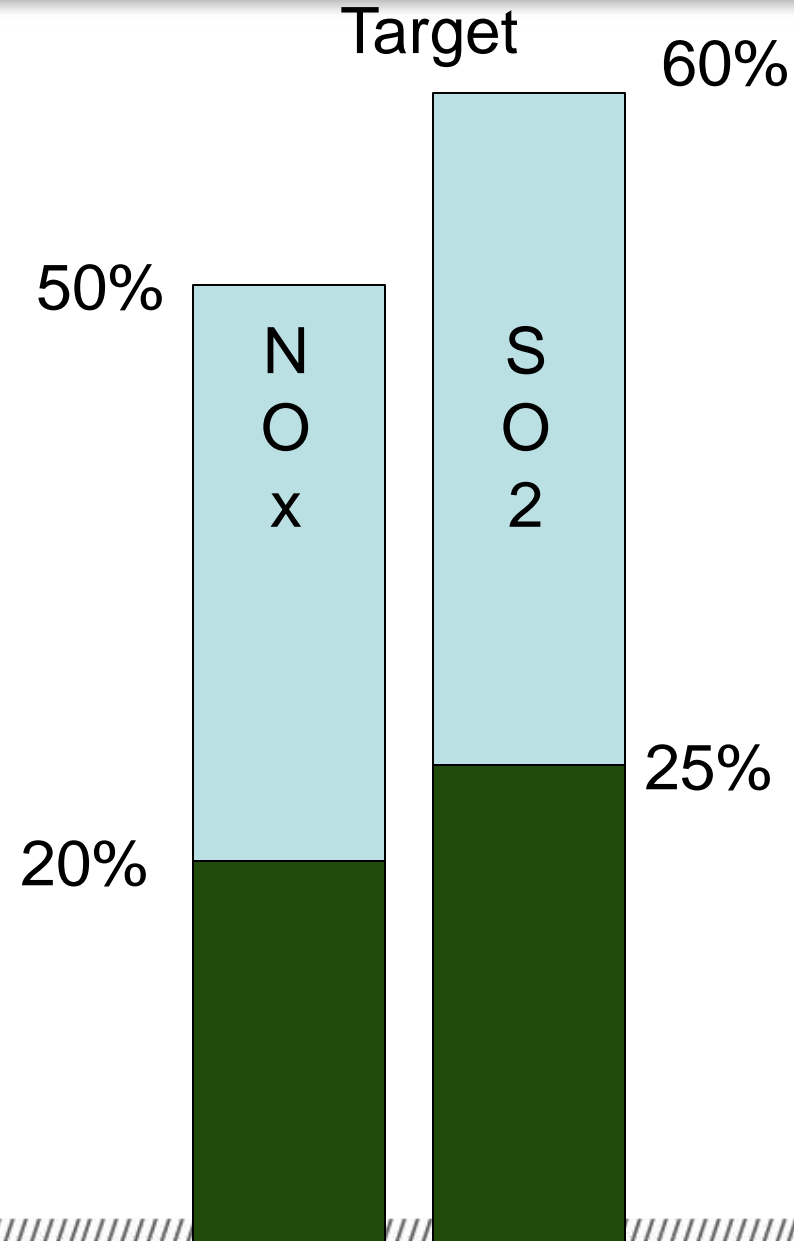
# Equipment and Layout



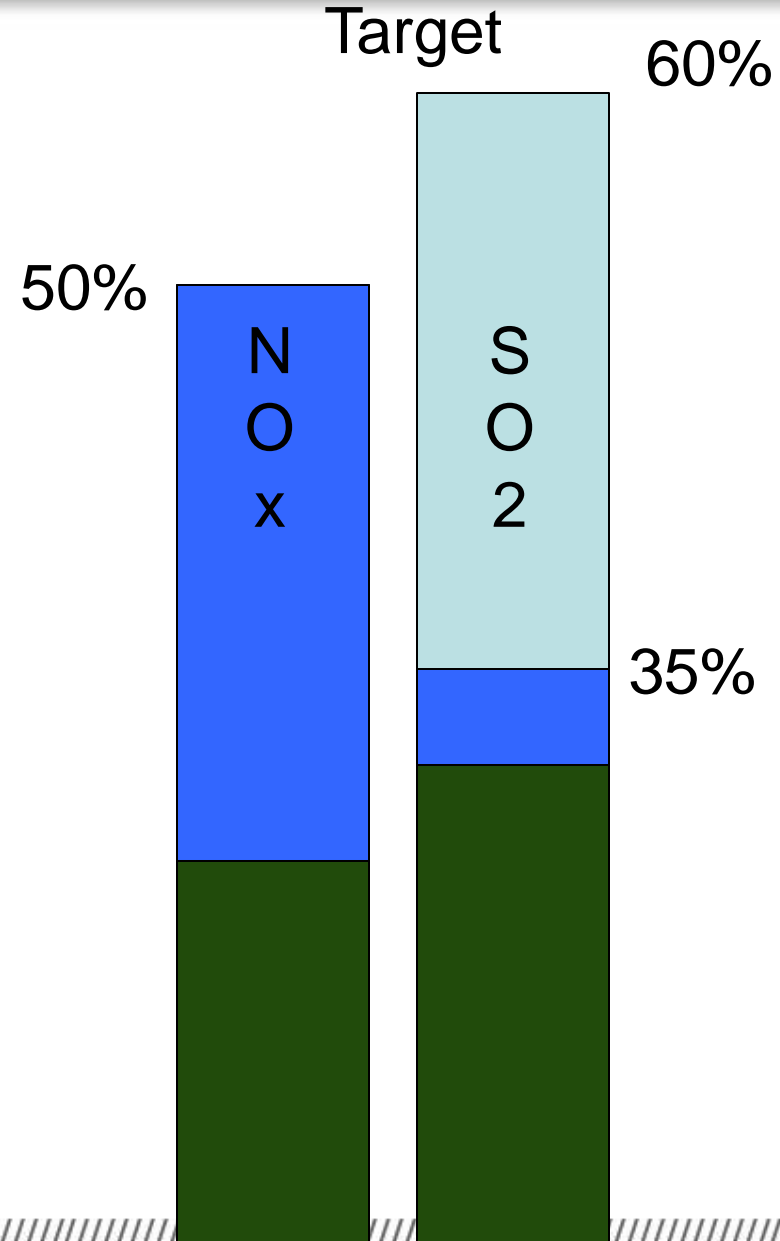
- **A Great deal is known about this work:**
  - Removal rates up to 90+% with SBC
  - Removal rates between 50% and 70% with Hydrate
  - Effects on fly ash utilization potential
  - Effects on particulate collection system
  - Effects on ash handling system



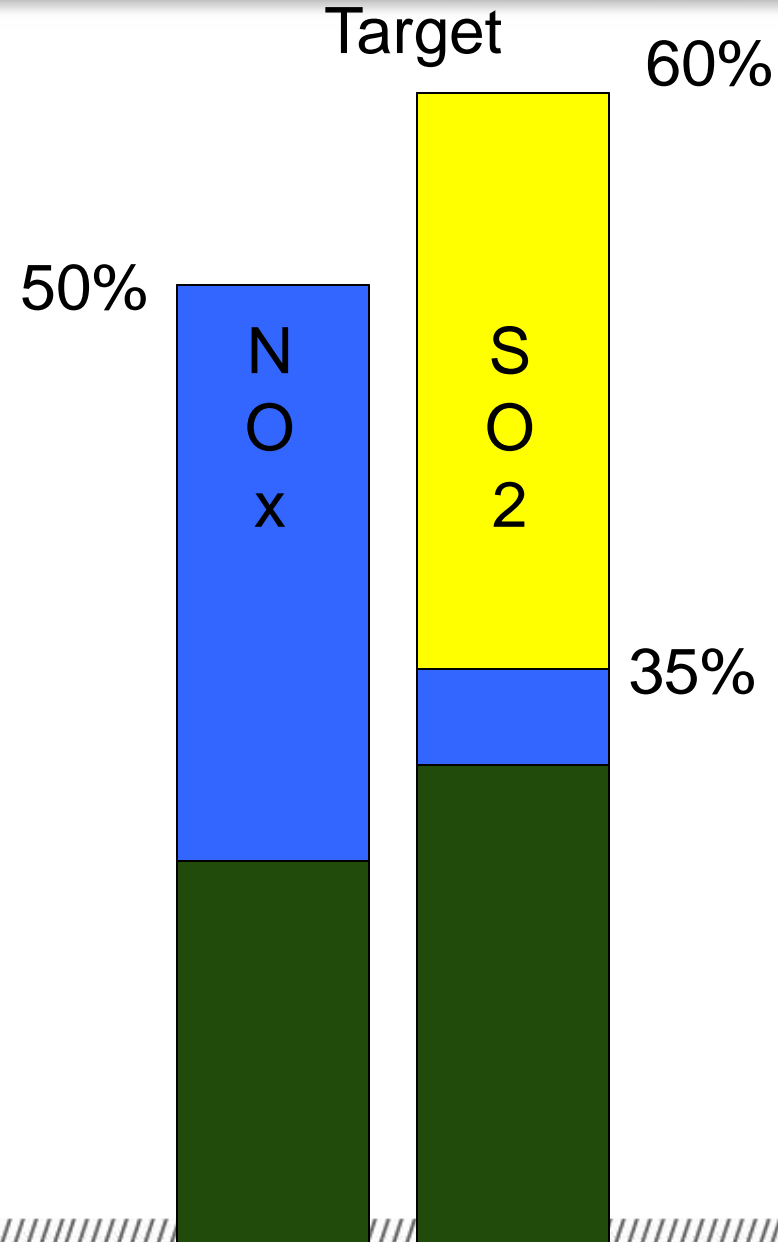
- **Co-Fire @ 25%**
  - SO<sub>2</sub> Reduction: 25%
  - NO<sub>x</sub> Reduction: 20%
  - Flyash reduction: 25%



- **Gas Injection Rate @ 10%**
  - SO<sub>2</sub> Reduction: 10%
  - NO<sub>x</sub> Reduction: 30%
  - Flyash Reduction: 10%




- **SO<sub>2</sub> reduction required = 25% of base or 40% of remaining**
- **Easily achieved by DSI**
- **Additional Particulate loading of DSI  $\leq$  reduction in flyash**



- **Hidden advantages**

- Improved load following and low load turn-down,
- Improved ignition system and warm-up,
- Increased peaking, and Unit capacity & reliability,
- Better SH/RH control,
- Reduced fan loading of both primary & secondary fans,
- Reduced fuel inventory,
- More uniform and increased flame zone O<sub>2</sub>,
- Consequently reduced slag formation problems.

- **Operating advantages**

- Lower O<sub>2</sub> operation,
  - Reduced SO<sub>3</sub>, acid, air-heater, back-end and plume problems,
  - Reduced LOI, leading to cleaner ash and better ESP operation,
  - More salable ash,
  - Dedicated fuel supply contracts.
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- **DSI is a useful technology for HCl and SO<sub>3</sub> mitigation for plants with SCR and Scrubber**
- **DSI can be a viable technology for compliance for plants without an SCR and Scrubber as part of a package that includes Gas Co-Fire and FLGR**

**Questions?**

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