



**EMO<sup>®</sup>**

March 28, 2013

**Bobby I.T. Chen**  
*Client Program Manager*



# Shaw Group is now Chicago Bridge & Iron



- ▶ Chicago Bridge and Iron (CB&I) has completed the acquisition of the Shaw Group.
- ▶ The effective date of the transaction was February 14, 2013.
- ▶ The combined organization brings the capabilities and experience of over 50,000 employees to the marketplace.
- ▶ Even though Shaw will undergo many changes under our new company, the people remain and will provide the same level of service and dedication to clients as before.



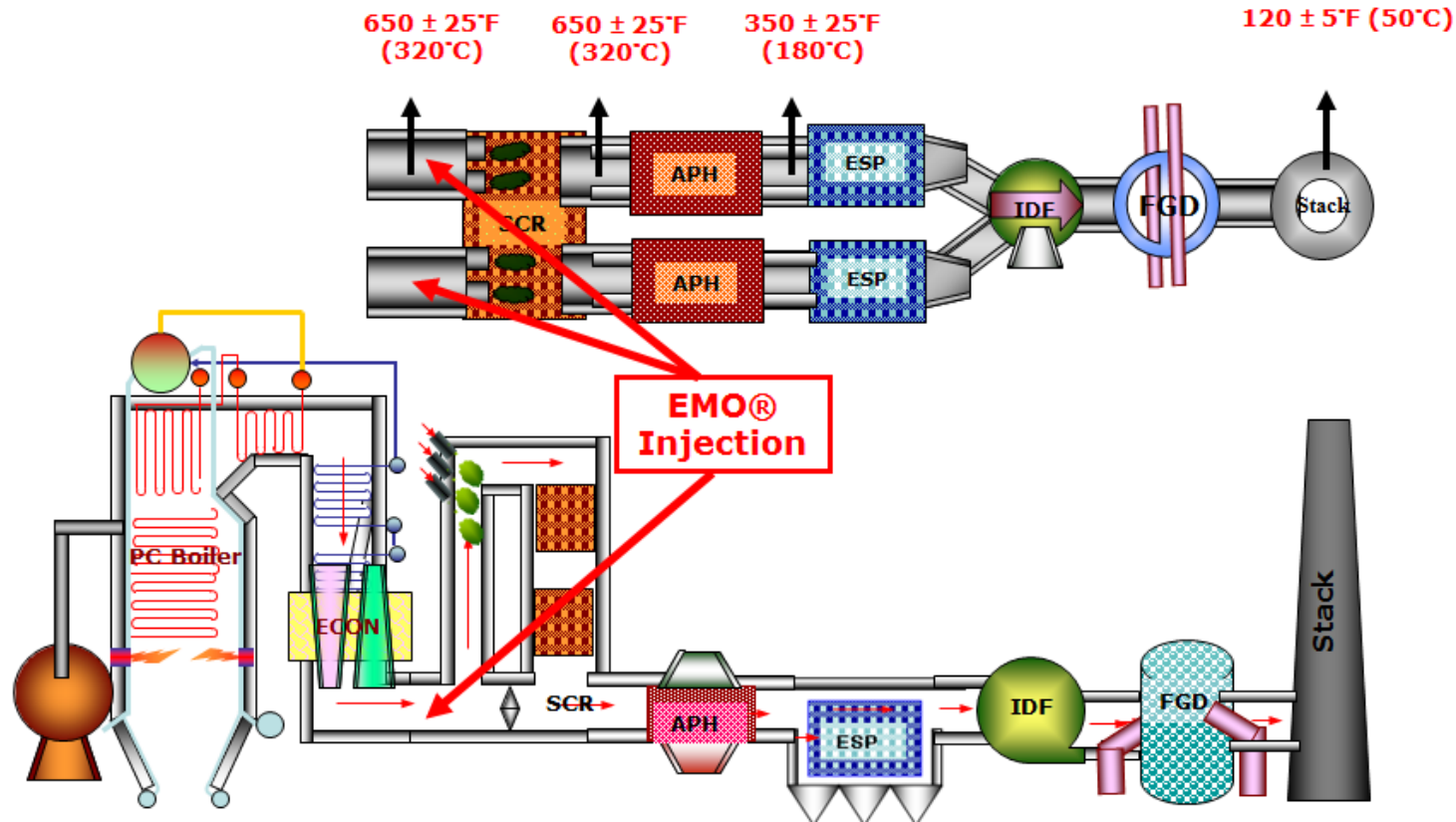
# MATS Overview



Subcategory	Total Filterable Particulate Matter (PM)	Hydrogen Chloride (HCl)	Mercury (Hg)
Existing coal-fired unit designed for coal > <b>8,300</b> Btu/lb	<b>0.030</b> lb/MMBtu ( <b>0.30</b> lb/MWh)	<b>0.0020</b> lb/MMBtu ( <b>0.020</b> lb/MWh)	<b>1.2</b> lb/TBtu ( <b>0.010</b> lb/GWh)
Existing coal-fired unit designed for coal < <b>8,300</b> Btu/lb	<b>0.030</b> lb/MMBtu ( <b>0.30</b> lb/MWh)	<b>0.0020</b> lb/MMBtu ( <b>0.020</b> lb/MWh)	<b>4.0</b> lb/TBtu ( <b>0.040</b> lb/GWh)

- ▶ Mercury and Air Toxics Standard (MATS) published on 2/16/2012, which became effective 60 days later. Compliance needs to be demonstrated by the 1<sup>st</sup> quarter of 2015
- ▶ Final PM limit for Filterable PM only (per EPA Method 5)
- ▶ Use of the alternate SO<sub>2</sub> limit is not allowed if EGU does not have some form of FGD system and SO<sub>2</sub> CEMS installed.
- ▶ Where alternate limits are designated with “or” in Table 2 Section 1 of MATS, these pollutants may be used in lieu of pollutants listed in same subsection (e.g. Total non-HAPs may be used in lieu of Filterable PM).
- ▶ The Hg limit is **based on a 30-day boiler operations rolling average**

# EMO<sup>®</sup> Injection General Arrangements



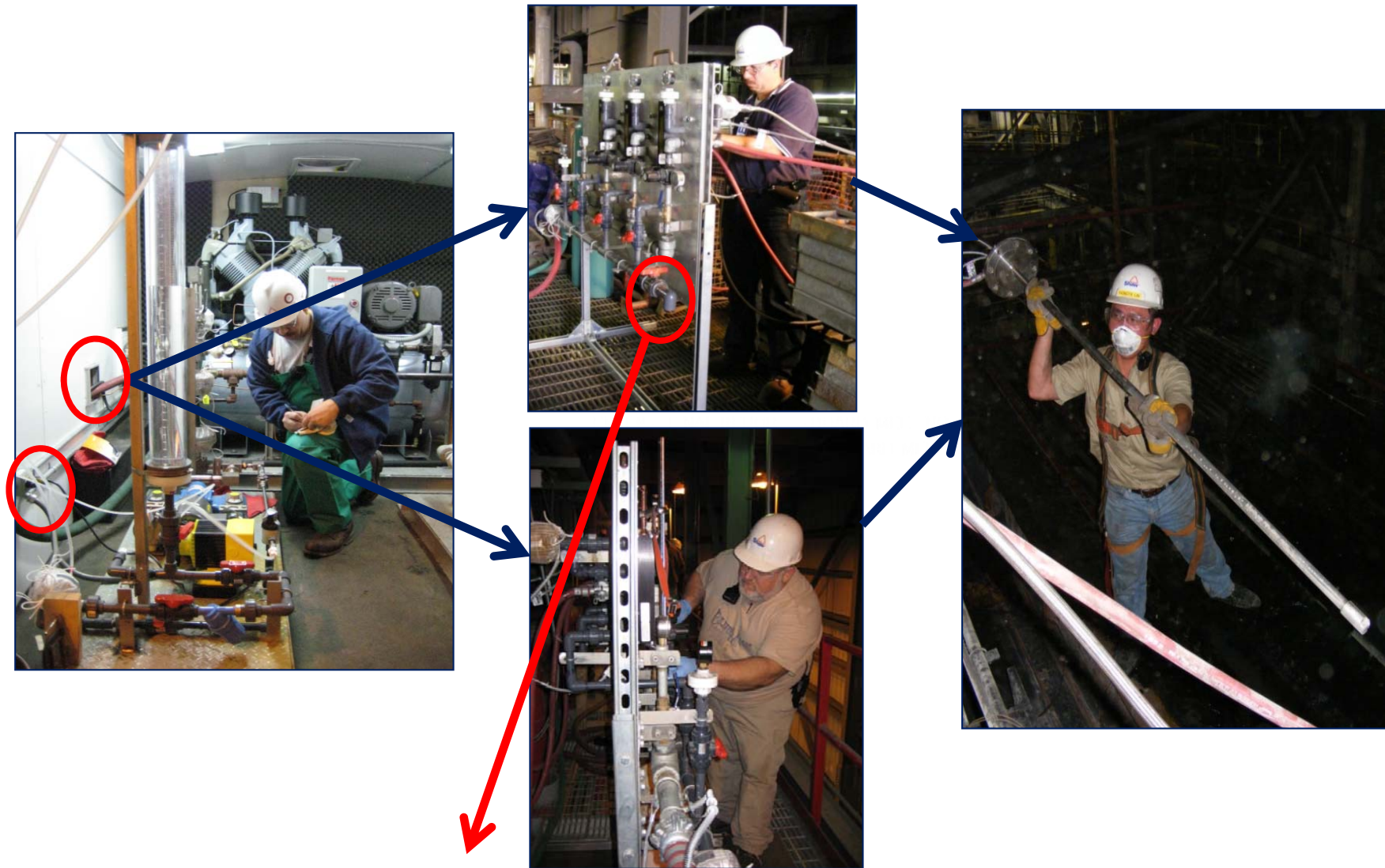
- ▶ Injecting chemical: EMO<sup>®</sup> chemical additives

Mercury Oxidization: **Hg(0)** → **Hg(2+)**

Mercury Absorption/Adsorption: in the existing PCD and scrubber

- ▶ Injection location and temperature: Economizer outlet (> **650°F**) or PCD outlet (**320°F**)

# EMO<sup>®</sup> Injection General Arrangements

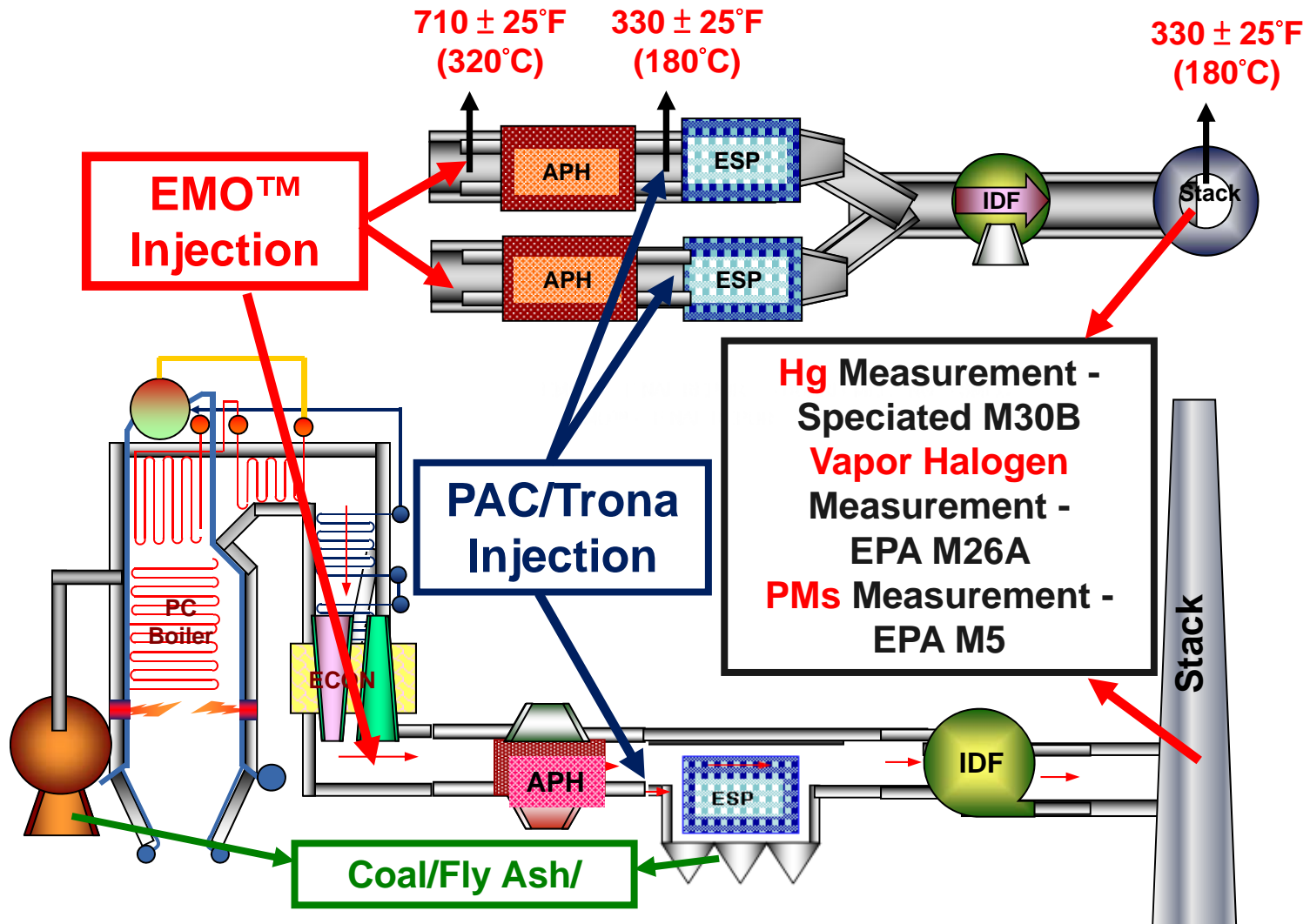


- ▶ the **X** ppmv of EMO<sup>®</sup> injection rate was precisely determined by direct sample titration

# Reference Unit 1 Testing Arrangement



- ▶ 220 MW, ESP only, 100% PRB



# Reference Unit 1 Hg Data Overview



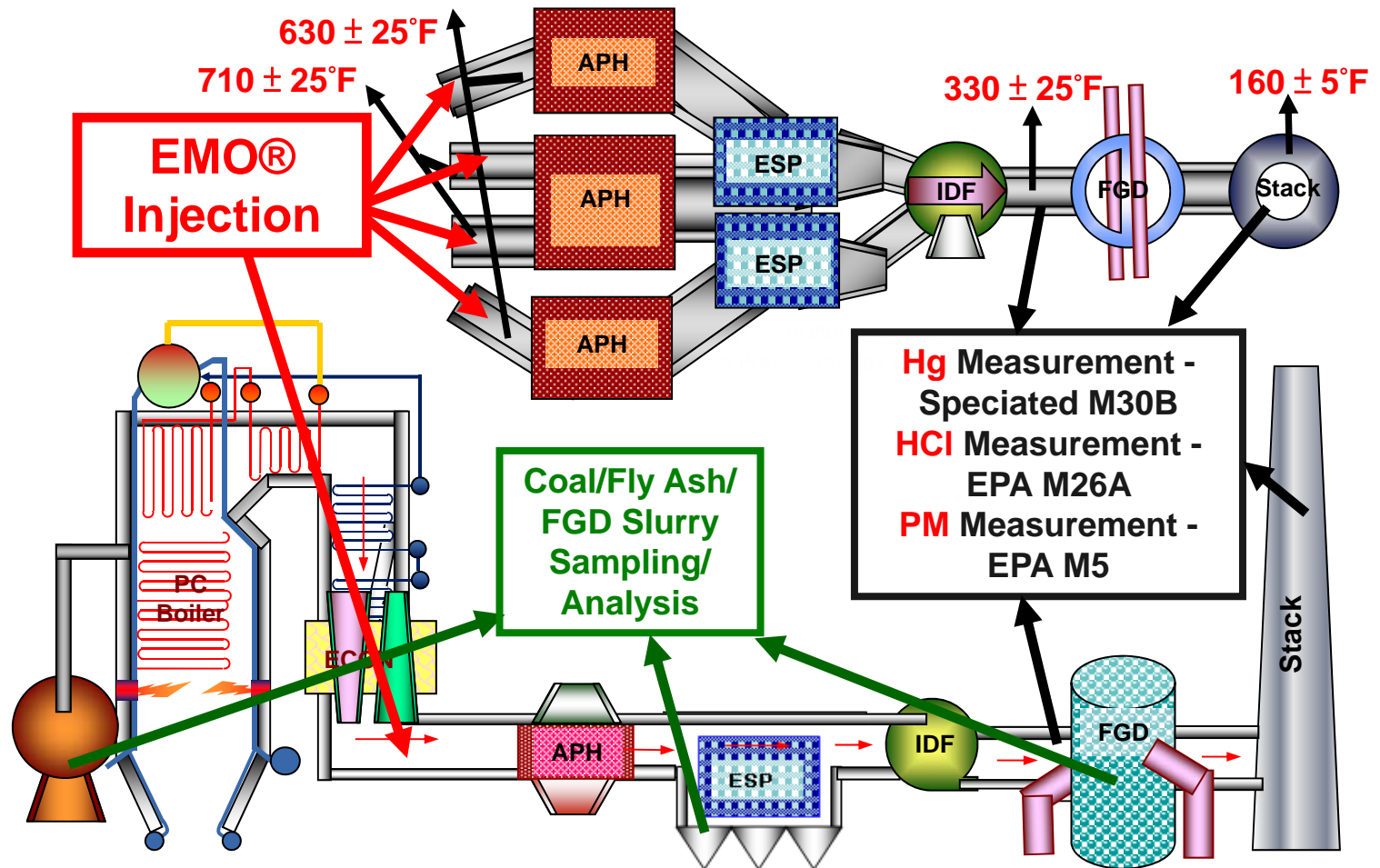
Date	Unit Load	Max. Hg From PRB	EMO™ Injection Rate	PAC Injection Rate	Trona Injection Rate	Stack Hg	Stack Hg	Hg Oxidization at Stack	Overall Hg Removal	NOx	Opacity
mm/dd/yy	(MW)	(lb/TBtu)	(ppmvd)	lb/mmact	(lb/Hr)	(lb/TBtu)	(lb/GWh)	(%)	(%)	(lb/MMBtu)	(%)
5/27/12	236	7.8	0.0	0	0	7.50	0.07317	3.8%	3.8%	0.044	4.5
	235	7.8	0.0	0	0	7.90	0.07707	6.4%	-1.3%	0.042	4.5
6/7/12	234	7.8	4.4	0	0	1.49	0.01457	97.4%	80.9%	0.043	4.2
	237	7.8	6.5	0	0	1.16	0.01136	97.7%	85.1%	0.045	3.4
6/8/12	235	7.8	5.5	0	1200	3.66	0.03570	91.7%	53.1%	0.045	3.6
6/8/12	235	7.8	10.0	2	1200	0.60	0.00585	99.0%	92.3%	0.045	3.5

- ▶ Baseline Hg emission at the Stack, **7.73** lb/TBtu on average, with above **95%** Hg (0)
- ▶ EMO was observed to produce above **96.5%** Hg oxidization efficiency, improved from **5%**
- ▶ EMO was observed to produce above **83.5%** overall Hg removal efficiency
- ▶ Combined with Trona, EMO still produced Hg oxidization rat **91.7%** Hg oxidization efficiency, overall Hg removal efficiency decreased down to **53.1%**
- ▶ Combined with Trona/PAC, EMO produced Hg oxidization rat **99.0%** Hg oxidization efficiency, overall Hg removal efficiency was determined at **92.3%**

# Reference Unit 2 Testing Arrangement

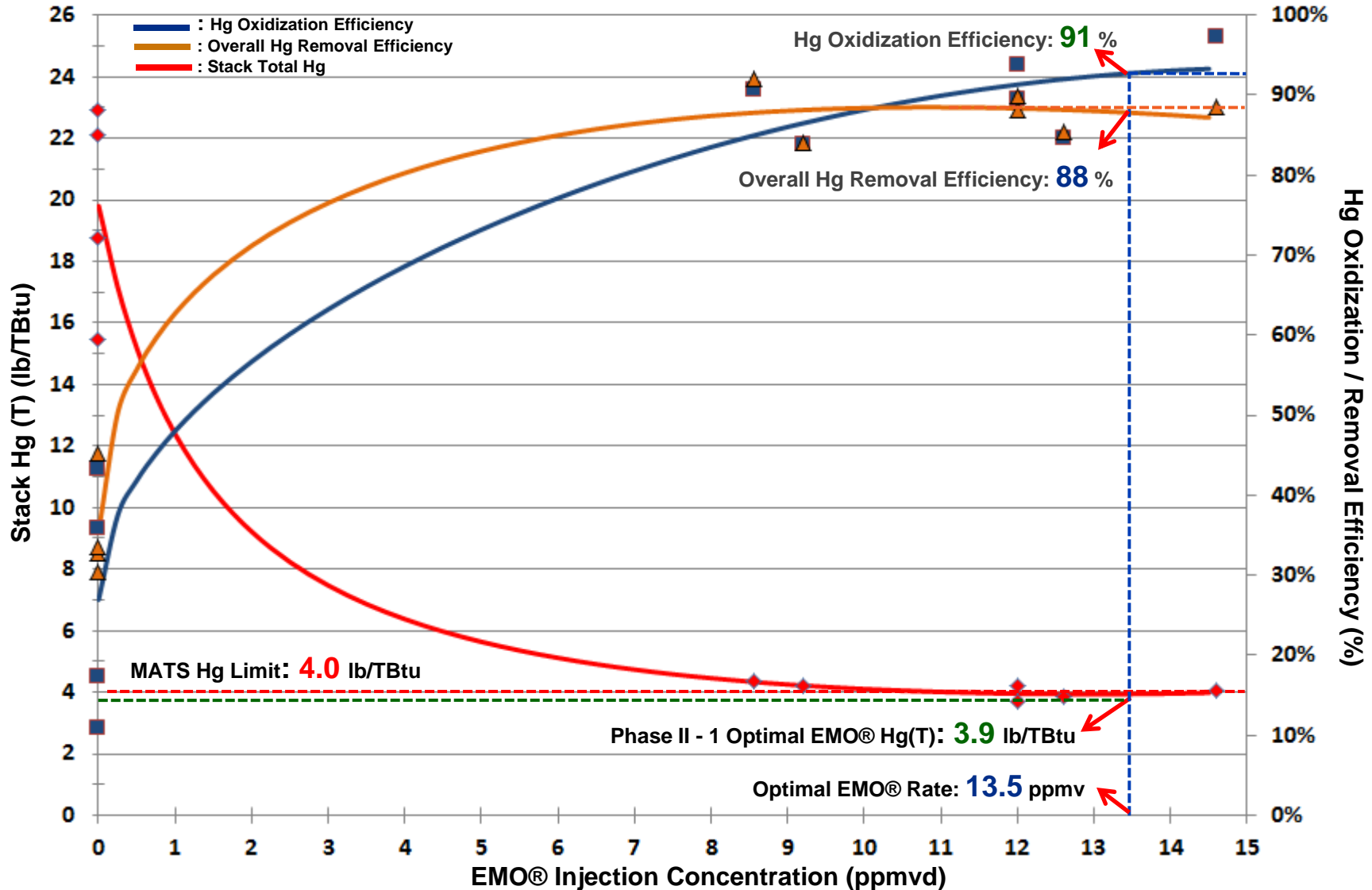


- ▶ 440 MW, ESP +FGD, 100% Lignite



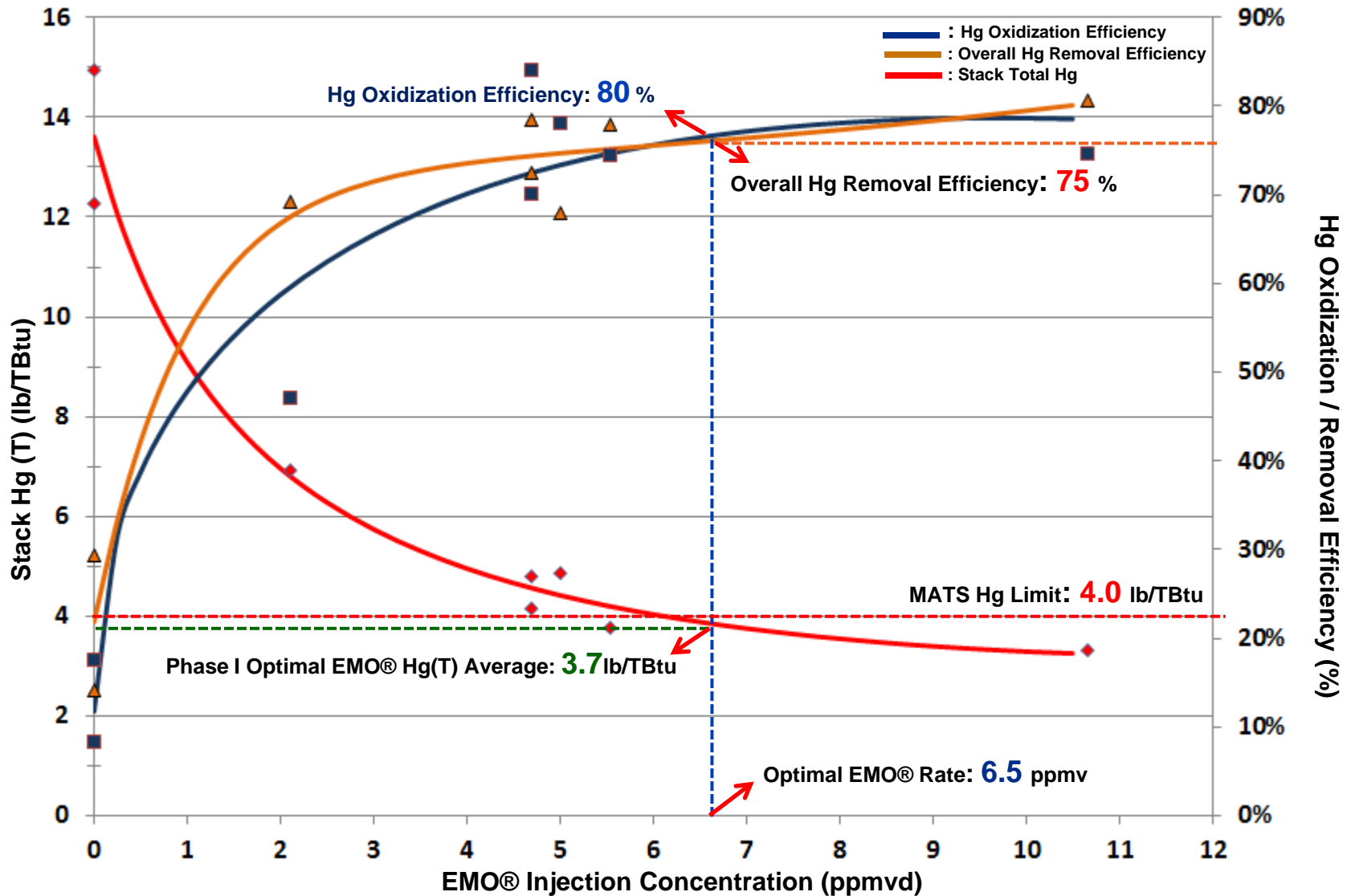


# EMO® Phase II - 1 Overview (5/22/2012 – 6/12/2012)



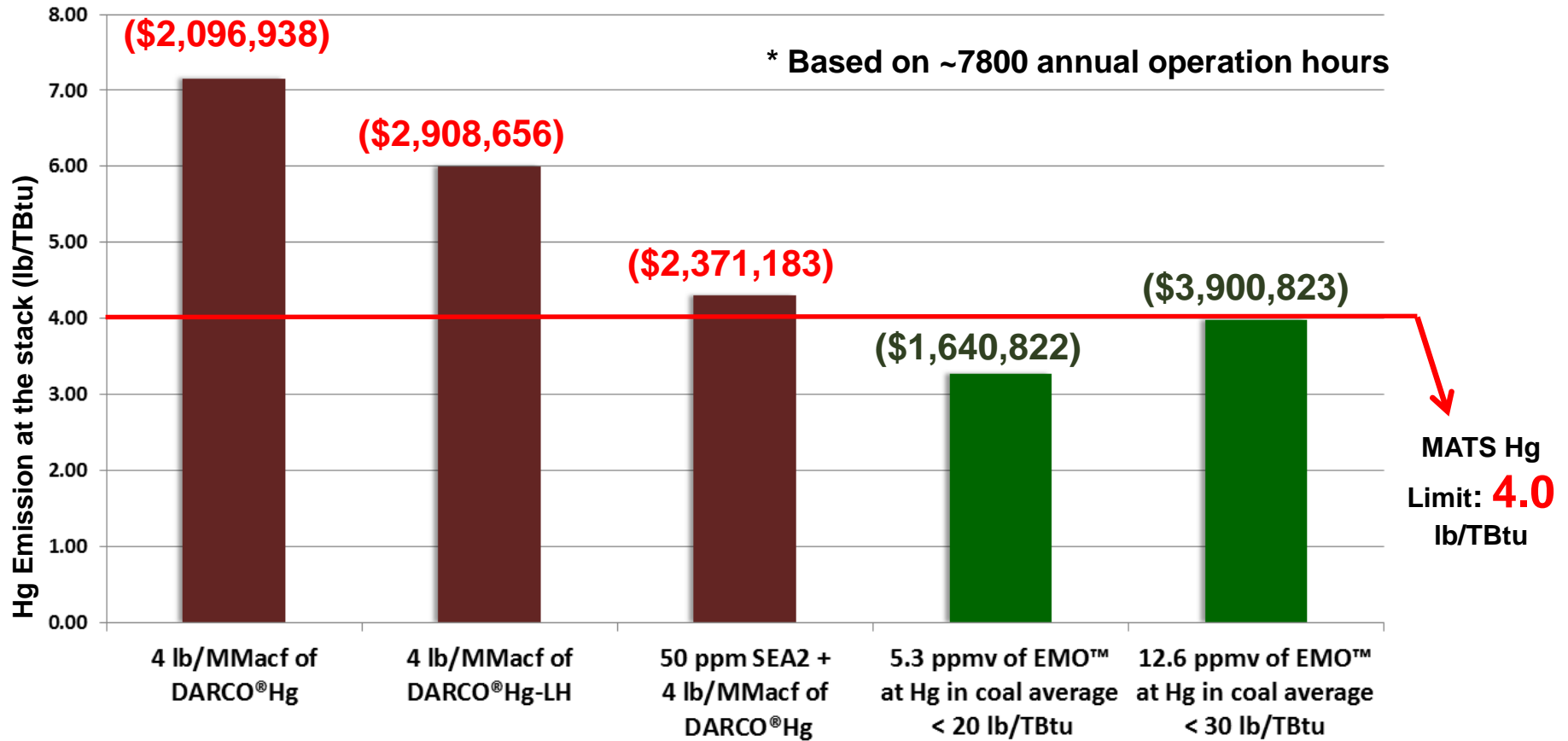
▶ Hg content in coal varied between 26.6 and 54.1 lb/TBtu, averaged at 33.7 lb/TBtu, Phase 1: 18.0 lb/TBtu

# EMO® Phase I Overview (11/14/2011-11/17/2011)



- ▶ Hg content in coal varied between **15.1** and **22.4** lb/TBtu, averaged at **18.0** lb/TBtu

# Reference Unit 3 Economics Analysis



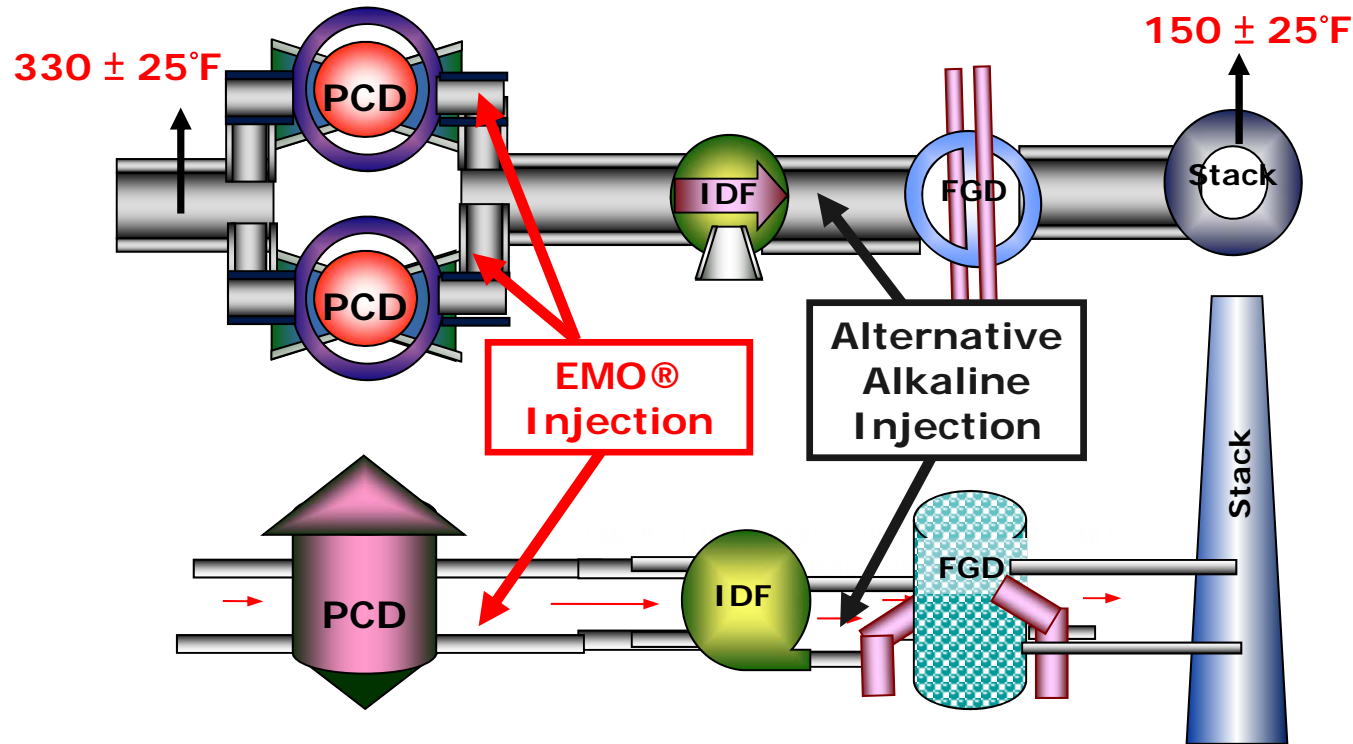
- ▶ The cost estimates for **the first 3 non-EMO™ injection options** were based on Hg Content in coal ~20 lb/TBtu. **None of them demonstrated MATS compliance!**

# Stack Visible Blue Plum – SO<sub>3</sub> Interferences



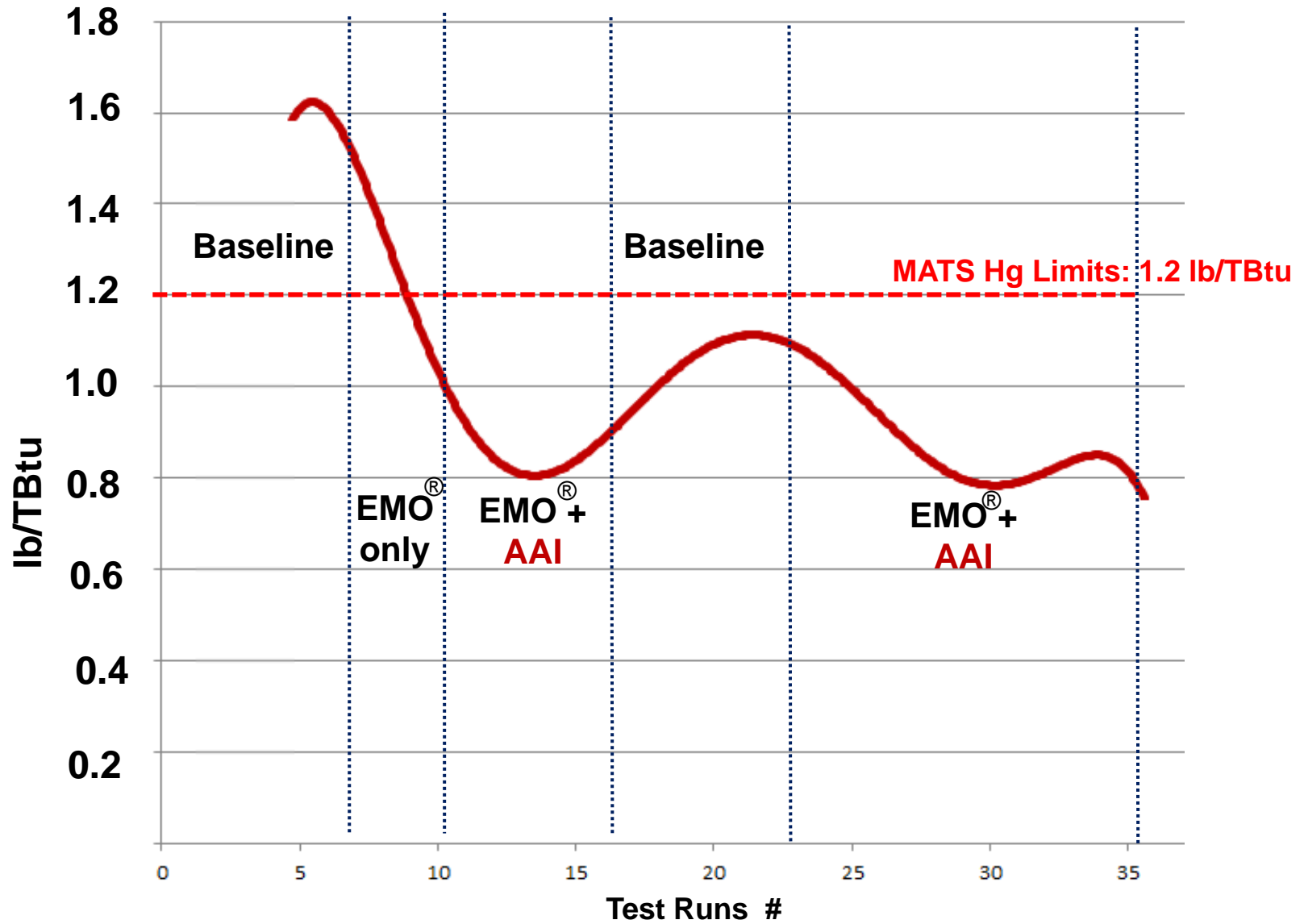
- ▶ From various CB&I EMO field trial, SO<sub>3</sub> has been observed to inhibit Hg oxidation Hg<sup>2+</sup> adsorption across the ESP, and Hg<sup>2+</sup> absorption across the FGD

# Testing Summary – Reference Unit 4



- ▶ **~300** MW Gross, SCR + PCD + FGD, AAI was **100'** downstream of the EMO®
- ▶ Hg in coal: **9.0** lb/TBtu, Sulfur in coal: **3.5%**, Stack SO<sub>3</sub> was visible at **~20** ppmv
- ▶ Baseline Hg stack Hg (T): **~1.7** lb/TBtu
- ▶ **5.0** ppmv of EMO® at PCD outlet, Stack Hg (T): **~1.1** lb/TBtu
- ▶ **2.5** of EMO® at the PCD outlet and AAI at the ID outlet Stack Hg (T): **~0.9** lb/TBtu

# Potential SO3 Interferences – Reference Unit 4



# Can Ca(Br)<sub>2</sub> Produce the Same Results? Not Really



Sampling Date	Test Condition	Start Time	End Time	CaBr <sub>2</sub> Target ppm	EMO Target ppmvd	Hydrogen Bromide		Relative Deviation %	Hg Oxidization Efficiency %	Stack Hg Removal Efficiency %
						M26A FGD inlet ppmvd	M26A Stack ppmvd			
7/12/2012	EMO - Baseline	9:00	10:00	0	0	0.18	0.10		17%	25%
7/12/2012	EMO - Baseline	11:15	12:15	0	0	0.09	0.10		6%	21%
7/12/2012	EMO Parametric	17:00	18:00	0	2.9	4.48	0.10	21%	54%	57%
7/13/2012	EMO Parametric	10:40	11:40	0	5.5	5.78	0.10	3%	71%	60%
7/16/2012	Trona - Baseline	8:00	9:00	260	0	3.27	0.10		61%	51%
7/16/2012	Trona - Baseline	9:30	10:30	260	0	3.47	0.10		61%	50%

- ✓ Blending **260** ppm of Ca(Br)<sub>2</sub> blending in coal requires 57 lb/hr Ca(Br)<sub>2</sub> (110 lb/hr of 52% Ca(Br)<sub>2</sub> solution). This equates to 0.28 lb-mol of Ca(Br)<sub>2</sub>, which generates **0.56** lb-mol available Br material in flue gas in the form of Br<sub>2</sub> or HBr.
- ✓ For **3.3** ppmv EMO™ injection at 195 MW gross generation, it would require 23.1 lb/hr of HBr injection (48 lb/hr of 48% HBr solution). This equates to **0.29** lb-mol of HBr, which generates 0.29 lb-mol available Br in flue gas.
- ✓ Hence applying Ca(Br)<sub>2</sub> could put approximately **50%** of the Br material to waste (**0.29** lb-mol vs. **0.56** lb-mol), **Excessive Stack Br<sub>2</sub> Emission – Title 3 HAPS**
- ✓ the difference in annual cost is approximately **\$120K** for a 200 MW unit
- ✓ **HBr is a more effective material promoting Hg oxidization**

- ▶ EMO® Injection successfully demonstrated Hg compliance to MATS (>**90%** plus stack Hg oxidization efficiency), for **Lignite, Bituminous, & Sub-Bituminous**
- ▶ EMO® has been repeatedly observed to Improve Hg re-emission across the scrubber with a means of precise control
- ▶ The flue gas SO<sub>3</sub> emission was observed to inhibit Hg oxidization and oxidized Hg capture across the scrubber - **Hydrated lime injection mitigated SO<sub>3</sub> interference improving Hg oxidation and removal**
- ▶ EMO® injection does not create impact for the fly ash beneficial use/disposal (No metal leaching issues observed)
- ▶ EMO® was proven to be **~70%** more cost-effective than PAC injection and **~50%** more cost-effective than other fuel halogen additives, such as Ca(Br<sub>2</sub>)



## CONTACT

**Bobby I.T. Chen**

*Client Program Manager*

**+1 865.670.2687 – Direct**

**+1 865.360.2823 – Cell**

**bobby.chen@cbi.com**

**Randall P. Moore**

*Business Line Manager*

**+1 865.694.7455 – Direct**

**+1 865.604.3945 – Cell**

**randall.moore@cbi.com**

