

Severe Service Control Valves



Ory Selzer

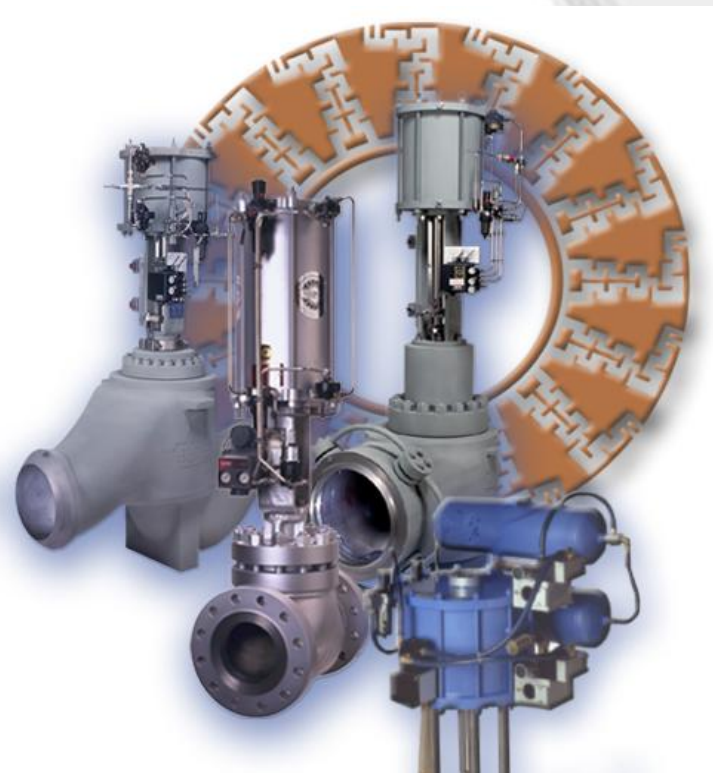
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Today's Seminar



- Introduction - CCI
- Severe Service Applications
 - Control valve hierarchy
 - Definition of severe service
 - Common applications
- Some Key Parameters
- Severe Service Trim Designs
- Q&A



Introduction - CCI

- **Founded in 1961 in Southern California**
 - Purchased by Babcock & Wilcox in 1971
 - Sold to IMI plc, out of the UK in 1981
- **Largest dedicated severe service valve manufacturer in the world**
- **Custom engineered – made to order products**
- **Fossil Power, CHP, Oil & Gas, Nuclear**
- **Global footprint – sales, service, manufacturing, etc.**



Babcock & Wilcox

Bailey

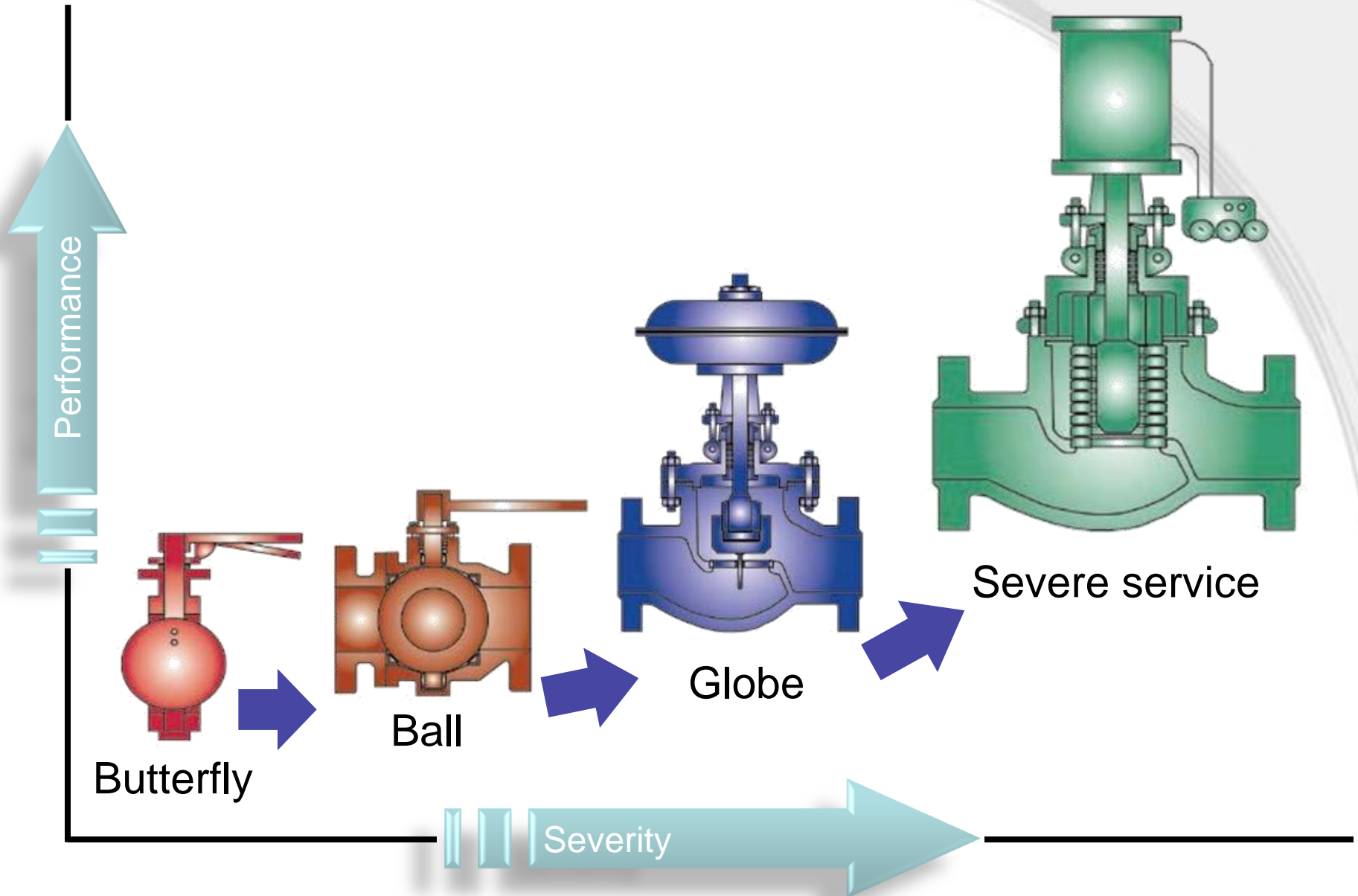
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Control Valve Hierarchy



Severe Service Definition



- Cavitation potential exists (Water Valves)
- High vibration / noise expected (Steam Valves)
- Flashing service
- $\Delta P/P_1 > 0.5$
- Historical knowledge
- Needs continuous maintenance
- Plant manager knows about the valve



Severe Service = High Pressure Drop = High Velocity = **ENEMY**

Velocity Related Damage Mechanisms



- Cavitation damage varies as a 5th to 6th power of velocity
- Erosion damage varies as a 2nd to 4th power of velocity
- Control valve noise varies as logarithmic with mach
- Vibration is caused by excessive fluid velocities & turbulence
- Corrosion is accelerated by velocity & fluid turbulence

Common Severe Service Applications – Combined Cycle Power Plants



- **Main Boiler Feedpump Recirculation**
- **Start-up & Main Feedwater Regulation**
- **Turbine Bypass Systems**
- **Attemperation & Spraywater Control**
- **Auxiliary Steam**
- **Vent Valves**
- **Condensate Recirc valves**



Key Application Parameters



➤ Plant type

- Combined Cycle, Supercritical, Sub-critical, CHP
- Cycling, Base Loaded, Peaking, Process Steam

➤ Identify the function of the control valve in the loop

- Flow control, Pressure control, Temperature control, Safety function
- System design and solution: Installation, Piping, Drains, Controls, etc.

➤ Review data sheet and establish operating parameters based on:

- Specified operating conditions
- Extrapolation between specified conditions
- Historical knowledge of the valve application and industry

Key Process Parameters



➤ Pressure Drop

- High pressure drops can lead to high velocities - multi-stage pressure letdown is required
- High velocities can lead to cavitation in water service and noise in steam service when left uncontrolled

➤ Rangeability

- Many applications require high rangeability for process control, i.e. Drum Level Control and Spraywater control
- Valve trim design, capacity and stroke length have a dramatic impact on rangeability

➤ Temperature

- High temperature designs require higher strength materials; CrMo, Inconel, Surface treatments
- Adding spraywater introduces thermal stresses – full system must be reviewed and designed together to provide proper control and protection from thermal fatigue

➤ Noise Requirements

- High pressure letdown in steam valves can create high velocities leading to noise levels near >110 dBA
- Steam kinetic energy must be controlled using multi-stage pressure letdown to reduce noise and vibration and keep plant operating safely

ISA guide: Velocity Control Limits



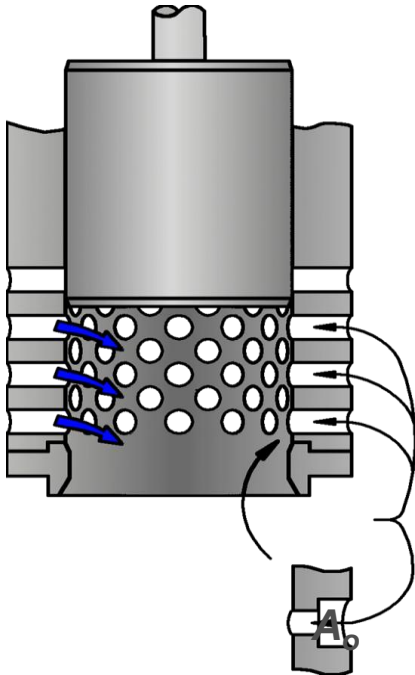
Trim outlet kinetic energy criteria

| $KE = \frac{\rho V^2}{2g_c}$ Service conditions | Gas / steam kinetic energy criteria | Equivalent liquid / water velocity |
|--|-------------------------------------|------------------------------------|
| | psia | ft / s |
| Continuous service single phase fluids | 70 | 100 |
| Cavitating & multiphase fluid outlet | 40 | 75 |
| Vibration sensitive system | 11 | 40 |
| Intermittent duty | 150 | - |

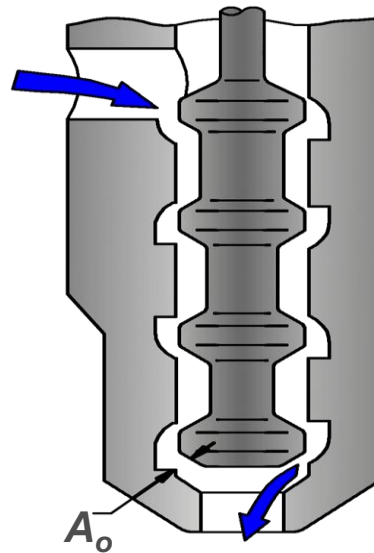
Severe Service Control Valve Trims



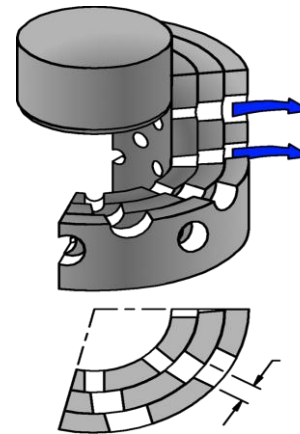
Single-Stage
Multi-Path



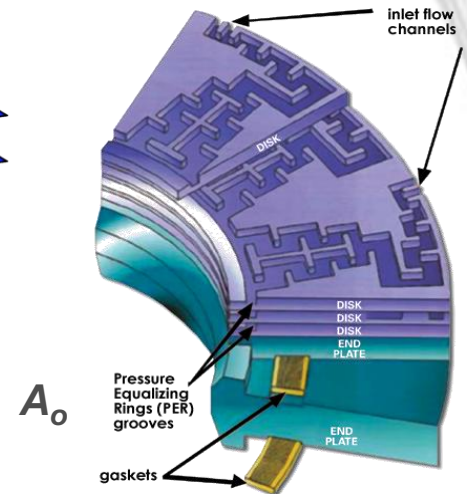
Multi-Stage
Single-Path



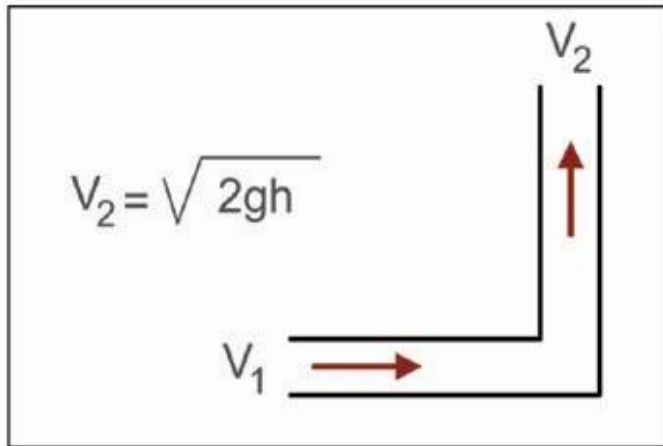
Multi-Stage
Multi-Path



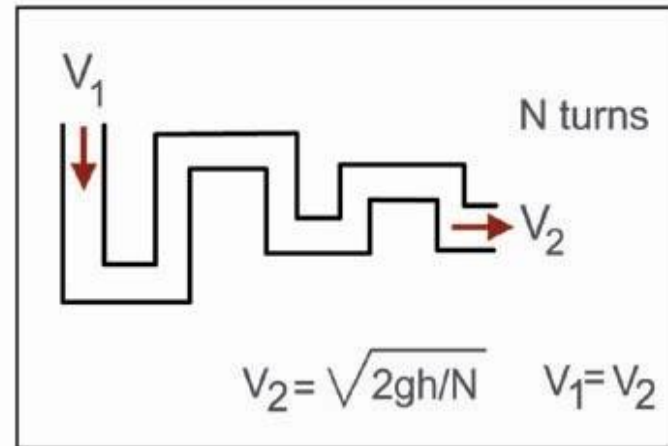
Torturous Path
DRAG®



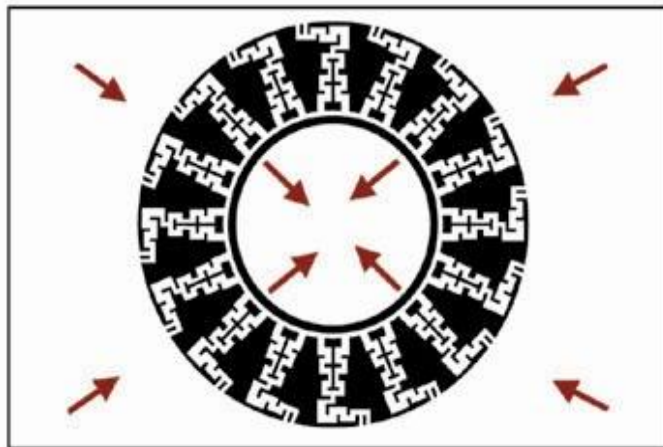
DRAG[®] velocity control principle



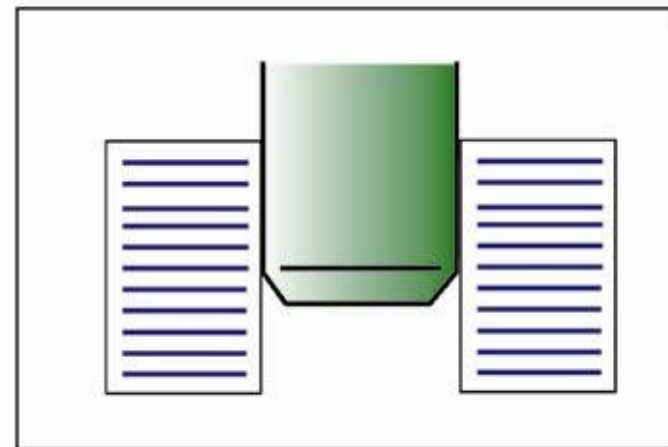
Single stage pressure reduction



Multi stage pressure reduction



Multi path multi stage disk



DRAG[®] disk stack

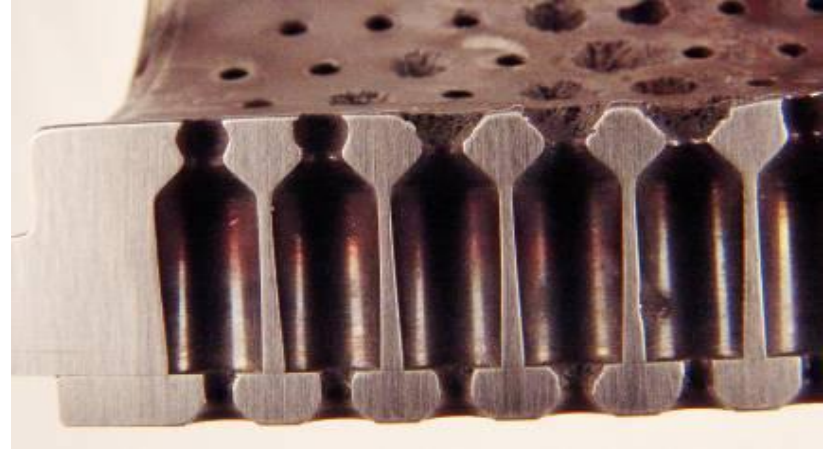
What happens when not enough stages are used?



| Number of stages | ΔP , psi | | | |
|------------------|------------------|------------|------------|------------|
| | 500 | 1400 | 2300 | 4100 |
| | ft/s | ft/s | ft/s | ft/s |
| 1 | <u>155</u> | <u>259</u> | <u>332</u> | <u>441</u> |
| 3 | <u>103</u> | <u>172</u> | <u>220</u> | <u>293</u> |
| 4 | < 100 | <u>148</u> | <u>190</u> | <u>253</u> |
| 8 | < 100 | < 100 | <u>121</u> | <u>161</u> |
| 12 | < 100 | < 100 | < 100 | <u>113</u> |
| 16 | < 100 | < 100 | < 100 | < 100 |

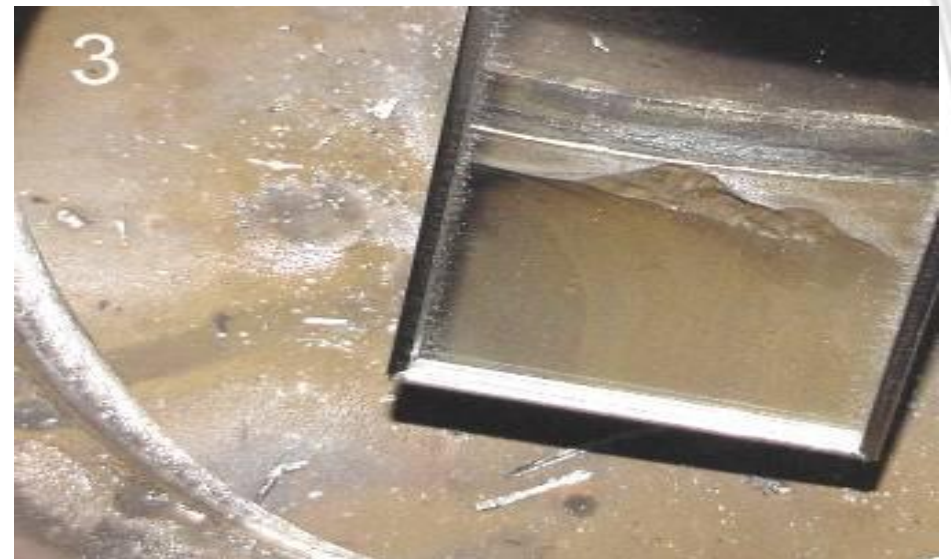
Assumes ambient temperature water

Cavitation Damage – Not Enough Stages



Application – BFP Recirculation, 1700 psid

Erosion in HP Feedwater valve



Summary

- Though small in number, severe service applications pose the highest challenges in the steam and water systems
- Each application should be reviewed and treated appropriately based on key application and process parameters
- Once severe service applications are identified the correct valve design needs to be applied to assure proper valve and plant performance
- ISA guidelines for sizing control valves are a great starting point: “Control Valves – Practical Guides for Measurement and Control” published by ISA



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