



#### **CEMS for Measurement of** Ammonia, SO<sub>3</sub>, and Low Level NOx

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#### **Presentation Overview**

- Compliance versus process control
- In situ versus extractive
- EPRI monitor evaluation approach
  - Lab assessment
    - Establish monitor accuracy
  - Field demonstration
    - Operability and reliability characteristics
  - Cost benefit application demonstration
- Low level NOx measurement
- Ammonia measurement
  - Issues and approaches taken to address
  - Successful applications
- SO<sub>3</sub> measurement
  - SO<sub>3</sub> + H<sub>2</sub>SO<sub>4</sub>





## **Compliance vs Process Control**

- Compliance Measurements
  - Stack gas application
    - Near particulate free
    - Lower temperature
  - Representative average concentration
  - Daily zero & span checks
  - Span gases meet NIST traceability standards
  - Quarterly and annual QA/QC requirements
  - Availability
- Process Control
  - Economizer exit / air heater inlet applications
    - Ash particles
    - Higher flue gas temperature (i.e. 650 +/- 50 F)
  - Spatial differentiation more important
  - Less rigorous QA/QC required
  - Typically less documentation

## In Situ vs. Extractive Measurement

- Issue of getting reactive species to monitor favors in-situ methods
  - Typically dealing with trace level concentrations
  - SO<sub>3</sub> / NH<sub>3</sub> reactive with potential reactions including:
    - $SO_3 + H_2O \longrightarrow H_2SO_4$  Acid dewpoint •  $SO_3 + CaO_{(s)} \longrightarrow CaSO_{4(s)}$  < 2000 F•  $NH_3 + SO_3 + H_2O \longrightarrow (NH_4)HSO_{4(l)}$  400-500 F•  $2NH_3 + SO_3 + H_2O \longrightarrow (NH_4)_2SO_{4(s)}$  400-500 F
  - Sample stream temperature needs to be maintained above highest
    - reaction temperature
  - Potential impacts of sample stream contact with filtration media
- In situ measurements provide potential benefits over extractive approach
  - Limited measurement bias
  - Faster system response
  - Line of sight measurements more representative relative to single point



## **EPRI Monitor Evaluation Approach**

#### **Three Step General Approach**

- 1. Laboratory Assessment
  - Establish accuracy, detection limits, and possible interferences
    - Test over range of target gas concentrations and cell conditions
      - Vary temperature, moisture, background gas composition
- 2. Single Path Field Demonstration
  - Establish operability and reliability characteristics
    - Test over range of path lengths with particulate laden flue gas
    - Assess alignment and signal to noise ratio over time and operating conditions
    - Assess maintenance requirements
- 3. Cost Benefit Application Demonstration
  - Structured test with end use of data stream (i.e. process control, operator advisory, etc.)
  - Document implementation specification, capital and installation costs, benefits from end use



## **CEM Measurement of Low Level NOx**

- Important issues identified
  - Instrument Performance
  - NO<sub>2</sub> NO Converter
  - Linearity / Drift Studies
  - Sample Conditioning Systems
  - Sample Lines





## **CEM Measurement of Low Level NOx**

#### NO<sub>2</sub> Converter Efficiency

	Efficiency
Converter Type	%
Molybdenum	96.9
Molybdate-Carbon	94.3
Molybdate-Carbon (hot & wet)	85.5
Stainless Steel	97.3
Vitrous Carbon (hot & wet)	83.3

#### Linearity and Drift

Converter		Zero	Calibration
Туре	Linearity	Drift	Drift
Molybdenum	0.9999	0.26	0.24
Stainless Steel	1.0000	0.74	0.13
Moly-Carbon	0.9999	0.29	0.82
VitCarbon h/w	0.9997	NA	NA
Moly-Carbon h/w	0.9985	1.24	6.07



wet

## **CEM Measurement of Low Level NOx**

#### Sample Conditioning Systems

- Dilution extractive
- Permeation dryer
- Thermoelectric cooler (impinger type)
- Refrigerated (coil type) condenser
- Glass impingers in ice bath
- Duel type (ambient temp. water removal followed by permeation dryer)

#### Sample Lines

- Stainless Steel 25°C
- Stainless Steel 175°C
- Silcosteel 107°C
- Silcosteel 175°C
- PFA Teflon 107°C
- Dilution extractive sampling probe
- Hot converter & analyzer
- Upfront converter/thermalelectric



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#### **Ammonia Measurement Status**

- Lab evaluations indicate TDL ammonia monitors tested work well under controlled conditions
- Application to coal-fired boilers introduce complications
  - Optical measurement issues
    - Port installation and alignment
      - Laser signal implications
    - Variable fly ash in flue gas
      - Laser beam attenuation and variable S/N
    - Long path lengths (reduced power and maintenance of alignment)
  - Current uses
    - Non-spatially resolved measurements for data trending
    - Spatially resolved measurements for open loop control
    - Process control and/or optimization





## **Ammonia Monitor Field Applications**

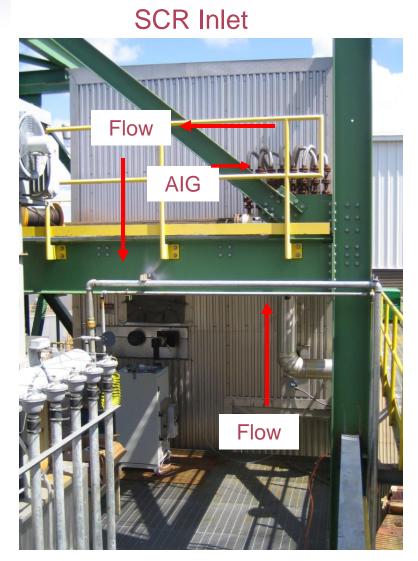
#### Successful ammonia monitor field applications

- SCR process control with NEO monitor
  - 1200 MW unit
  - 15' line of sight cuts corner of reactor
    - Excellent mixing going into SCR
    - Just downstream of expansion joint
- SNCR process control with Siemens monitor
  - 140 MW unit
  - Hot side ESP eliminates particle effects
  - Nominal 18 foot path length
- SNCR process control with Unisearch monitor
  - 300 MW unit
  - Partial shielded path
    - Reduces 20' path to ~14' path





#### **Continuous SO<sub>3</sub> Measurements FTIR Measurement Location**



# • MRC FTIR tests not able to attain target detection limit for SO<sub>3</sub>

- New high power IR source developed
- Increased signal to be tested for improved SO<sub>3</sub> detection
- FTIR used at MRC for continuous monitoring of HCI, SO<sub>2</sub>, NH<sub>3</sub> during SCR testing
  - FTIR results used to vary additive injection rates to compensate for variations in coal used
- System operated completely by MRC personnel
- System maintained alignment over 2 meter path after restarting of SCR

