



Energy, Utility & Environment Conference

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#### SO<sub>2</sub> Control Using Dry Sorbent Injection Technology with Hydrated Lime

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#### Agenda



- Why Dry Sorbent Injection (DSI)?
- Hydrated Lime Sorbents
- DSI Case Studies
- Conclusions



Summary



## Why Dry Sorbent Injection (DSI)?



#### Why Dry Sorbent Injection (DSI)?





- Equipment is low installed capital cost
- System relatively easy to retrofit to most plants
- Small equipment footprint
- Mechanically simple system
  - ~1 year schedule
    - award to installation
  - Low consumable requirement
    - 🗸 air, power



### **Hydrated Lime Sorbents**



#### **Range of Products**

# Choist North America

Sorbent	Standard Hydrated Lime	Sorbacal® H	Sorbacal® SP	Sorbacal® SPS	Units
Figure					_
Typical Available Ca(OH) <sub>2</sub>	92 – 95	93	93	<b>АСТ</b> 93	IVATION %
Typical Surface Area	14 – 18	> 20	~40	~40	m²/g
Typical Pore Volume	~0.07	0.08	~0.20	~0.20	cm³/g



### **DSI Case Studies**



#### **DSI Case Studies #1a and #1b**



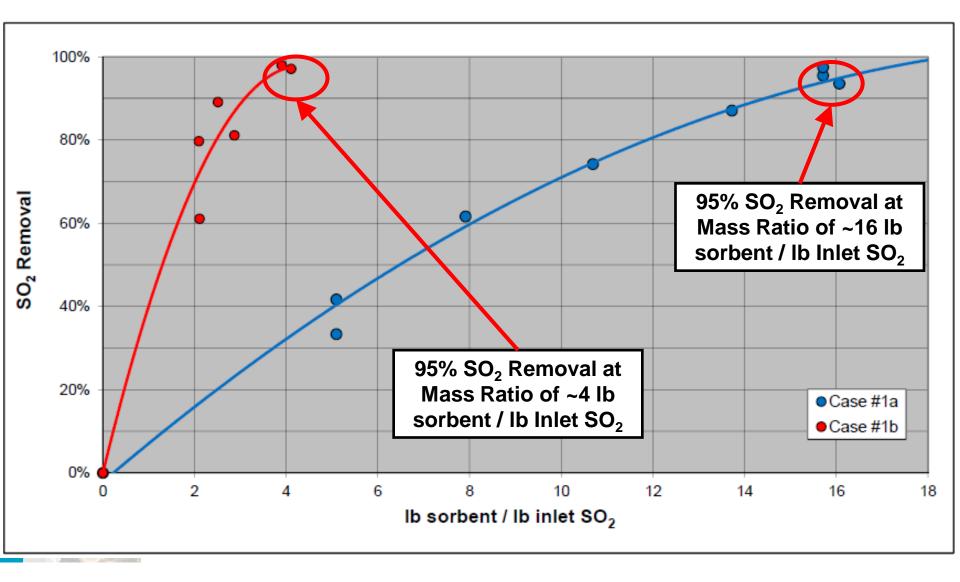
- Application  $\rightarrow$  Industrial Manufacturing Process
- Goal  $\rightarrow$  95+% SO<sub>2</sub> Removal Efficiency
- Why  $\rightarrow$  Meet Future SO<sub>2</sub> Permit Limit
- Process  $\rightarrow$  SDA  $\rightarrow$  Multi-Clone  $\rightarrow$  DSI  $\rightarrow$  FF
- Flue gas temperature at DSI location 300-350°F
- DSI  $\rightarrow$  One (1) Injection Lance @ Fabric Filter Inlet
- Sorbent  $\rightarrow$  Sorbacal<sup>®</sup> SPS

Case	Flue Gas Volume	Moisture Content	Baseline SO <sub>2</sub> Conc.
	ACFM	Vol. %	ppmv
1a	10,000	~14	100
1b	55,000	~36	300



#### **DSI Case Studies #1a and #1b**

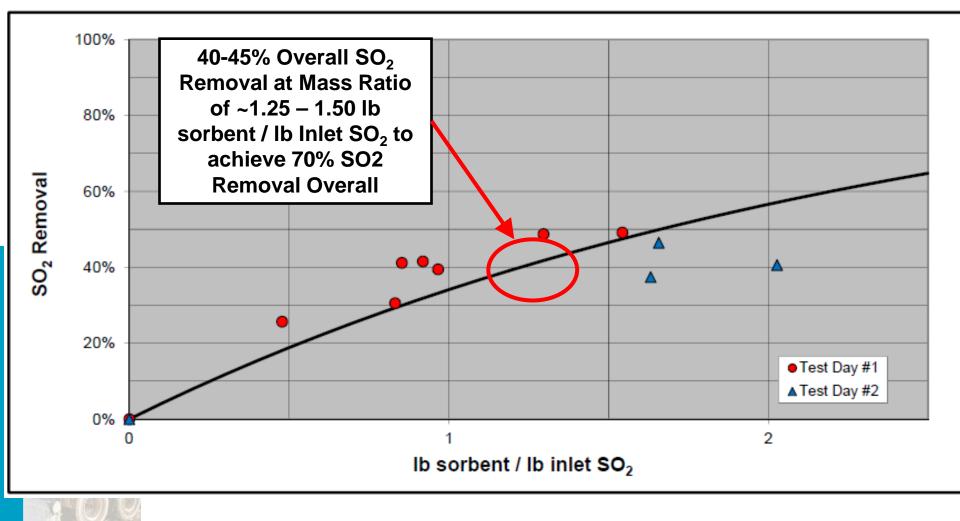






- Application  $\rightarrow$  500 MW Electric Generating Utility (EGU)
- Goal → Increase Overall SO<sub>2</sub> Reduction to ~70% (40-45% Incremental SO<sub>2</sub> Removal with DSI)
- Why  $\rightarrow$  Meet Future SO<sub>2</sub> Limit
- Low Sulfur Coal  $\rightarrow$  Boiler  $\rightarrow$  Air Heater  $\rightarrow$  DSI  $\rightarrow$  SDA  $\rightarrow$  FF
  - Process Conditions
    - ✓ Flue gas moisture ~20% relative humidity at stack
    - ✓ Baseline concentration ~225-250 ppmv SO<sub>2</sub>
    - ✓ Flue gas temperature at DSI location 275-300°F
  - DSI  $\rightarrow$  Five (5) Injection Ports @ DSI Location
- Sorbent  $\rightarrow$  Sorbacal<sup>®</sup> SPS





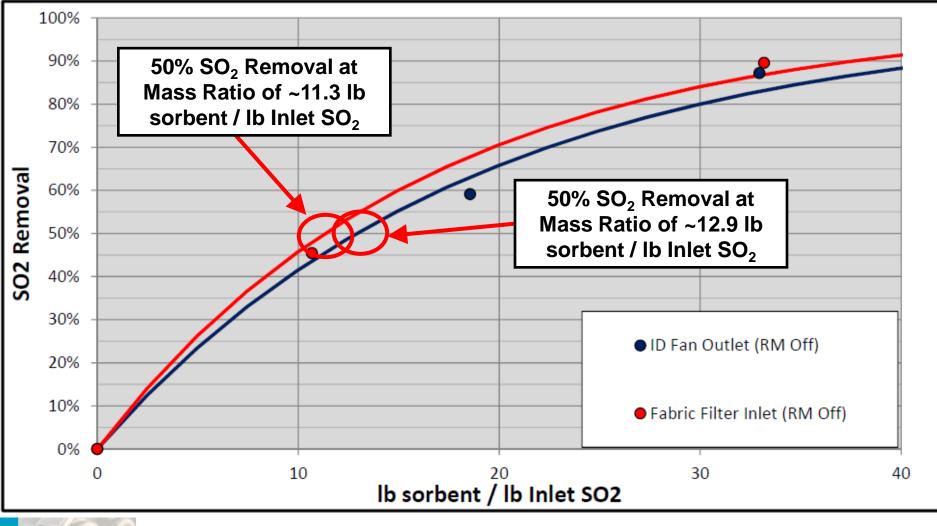
- Application  $\rightarrow$  985,000 ACFM Cement Plant
- Goal  $\rightarrow$  At Least 50% SO<sub>2</sub> Removal Efficiency
- Why  $\rightarrow$  Comply with Future Permit SO<sub>2</sub> Limit
- Raw Feed & Fuel → Kiln → Pre-Heater → ID Fans
  → Raw Mill → Fabric Filter

Lhoist North America

- Process Conditions
  - Flue gas moisture unknown
  - Baseline concentration 15 ppmv SO<sub>2</sub> with Raw Mill on / 35 ppmv SO<sub>2</sub> with Raw Mill off
  - ✓ Flue gas temperature at DSI location
    - ID Fan Inlet 575-675°F / Fabric Filter Inlet 370-470°F
- DSI  $\rightarrow$  Four (4) Injection Lances per Duct @ DSI Location
- Sorbent  $\rightarrow$  Sorbacal<sup>®</sup> SPS

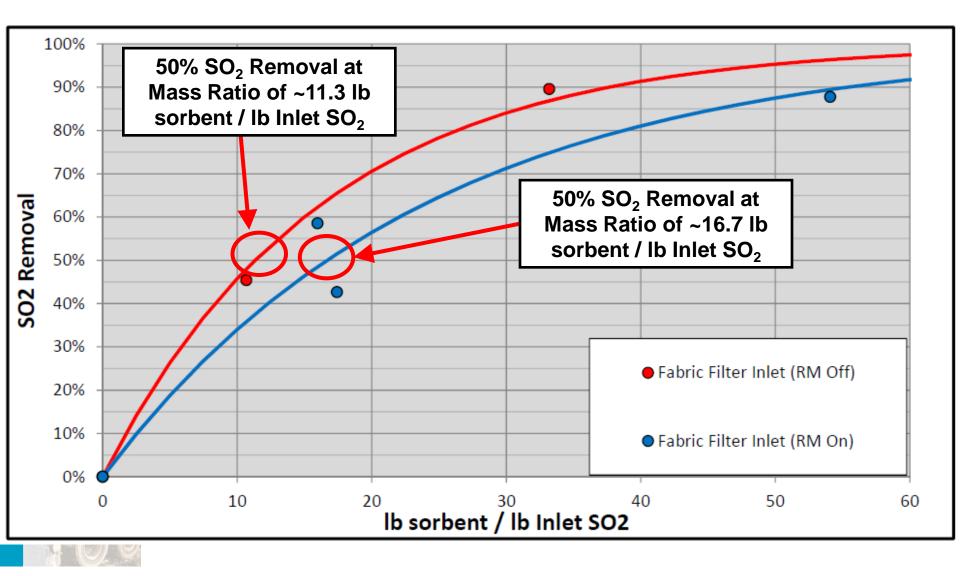








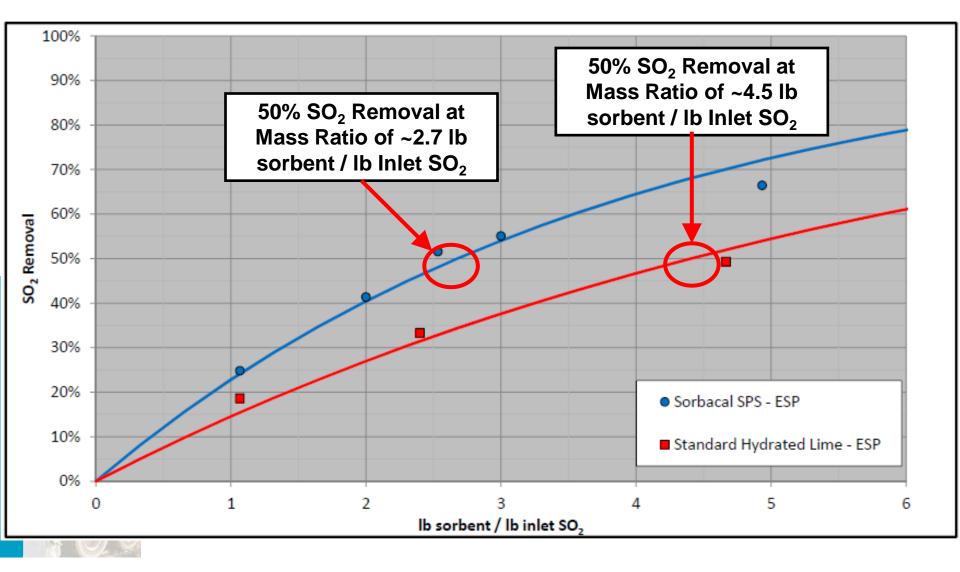






- Application  $\rightarrow$  580 SCFM Pilot Plant
- Goal  $\rightarrow$  Compare Relative SO<sub>2</sub> Removal Efficiency
- PRB Coal  $\rightarrow$  Boiler  $\rightarrow$  DSI  $\rightarrow$  Heat Exchanger  $\rightarrow$  ESP
- Process Conditions
  - ✓ Flue gas moisture ~9% by Volume
  - ✓ Baseline concentration ~150 ppmv SO<sub>2</sub>
  - ✓ Flue gas temperature at DSI location ~700-750°F
- DSI  $\rightarrow$  One (1) Injection Lance @ DSI Location
  - Sorbents  $\rightarrow$  Standard Hydrated Lime & Sorbacal<sup>®</sup> SPS







### **Conclusions / Discussion**



#### Conclusions

- Choist North America
- All cases were successful in achieving target SO<sub>2</sub> removal efficiency using DSI technology with hydrated lime sorbent
- Cases 1a and 1b
  - DSI using Sorbacal<sup>®</sup> SPS able to achieve high SO<sub>2</sub> removal efficiencies (> 95%)
  - Flue gas moisture content appears to be primary factor driving better performance in Case 1b

### Case 2

 DSI using Sorbacal<sup>®</sup> SPS effective solution for SO<sub>2</sub> trim application even on large scale



#### Conclusions



- Case 3
  - DSI using Sorbacal<sup>®</sup> SPS able to achieve target SO<sub>2</sub> removal at various injection locations under varying conditions
  - Demonstrated high SO<sub>2</sub> removal (85-90%) at three (3) injection locations
  - Illustrates why each site must be evaluated on case by case basis
  - Case 4
    - ✓ DSI using Sorbacal<sup>®</sup> SPS was ~40% more efficient than standard hydrated lime for SO<sub>2</sub> control at 700-750°F injection temperature based on PRB coal





### **Summary**



#### Summary

- Choist North America
- DSI technology using hydrated lime sorbents viable SO<sub>2</sub> compliance solution
- Flue gas moisture important for performance
- Sorbent properties also important
  - ✓ standard hydrated lime vs. enhanced hydrated limes
- Path Forward:
  - Additional SO<sub>2</sub> trials to understand how different parameters impact performance
  - Improve flue gas to sorbent mixing
  - Improve understanding of impacts of competitive reactions, flue gas temperature, flue gas moisture, sorbents, etc. on SO<sub>2</sub> removal
  - ✓ High temperature applications (furnace injection)





#### Thank you!!

#### If you have any questions feel free to contact,



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