



Fuel Flexible Advanced Energy Systems for the Production of Syngas, Hydrogen and Fuels

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*U.S. Department of Energy
National Energy Technology Laboratory
Separations and Fuels Processing
McIlvaine Company Hot Topic Hour
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Outline

- 1. NETL Coal/Biomass Program Objective**
- 2. Technology Concept Overview**
- 3. Technical Challenges in Implementation**
- 4. Program Implementation Strategy**
- 5. Research Summary**
- 6. Program Organization**
- 7. Summary and Future work**

Program Objective

“By 2012, complete R&D to integrate this technology with CO₂ separation, capture, and sequestration into a “zero” emission configuration(s) that can provide electricity with less than a 10 percent increase in cost.”

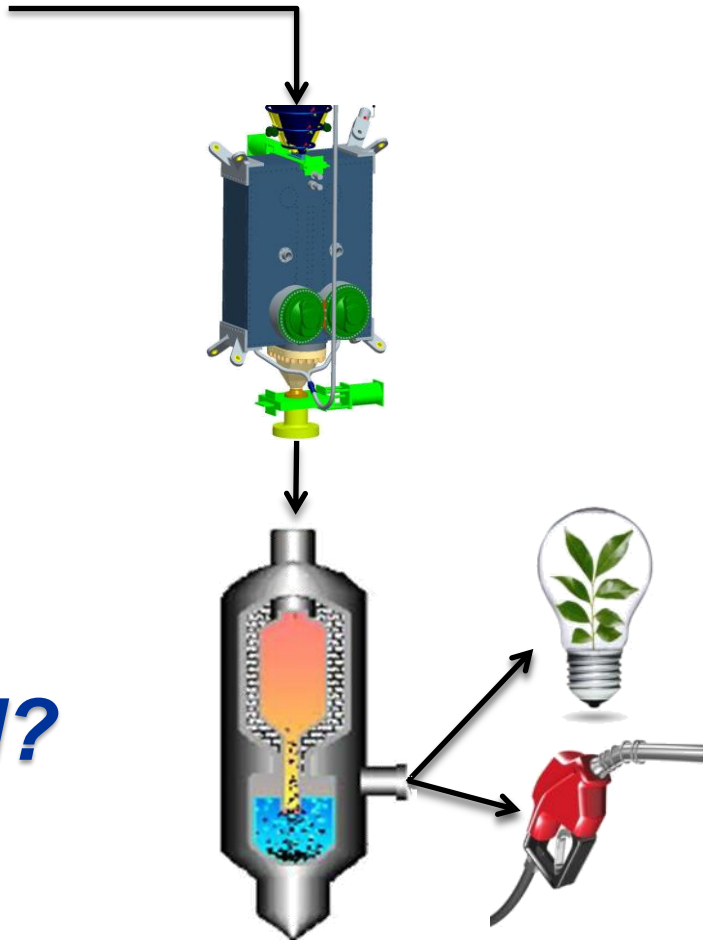
Project Goal

To identify, evaluate, and address the technical challenges involved in utilizing biomass in conjunction with coal in co-gasification systems



This study supports the expansion of DOE’s R&D portfolio with an intent to meet “zero emission” standards

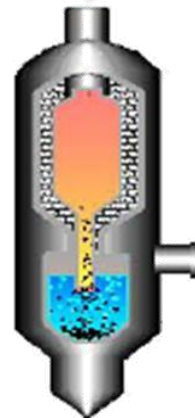
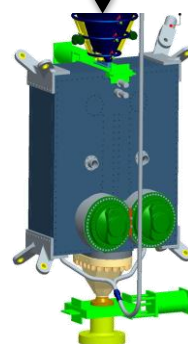
The Concept



***Conceptually
Simplistic...***

***Why not
commercialized?***

Technical Challenges



Raw Biomass

- *Material Variability (season, location, etc)*
- *Transportation (Energy Density)*
- *Storage (Degradation)*
- *Biomass Structure and Mechanical Properties*
- *Flowability*
- *Grindability*

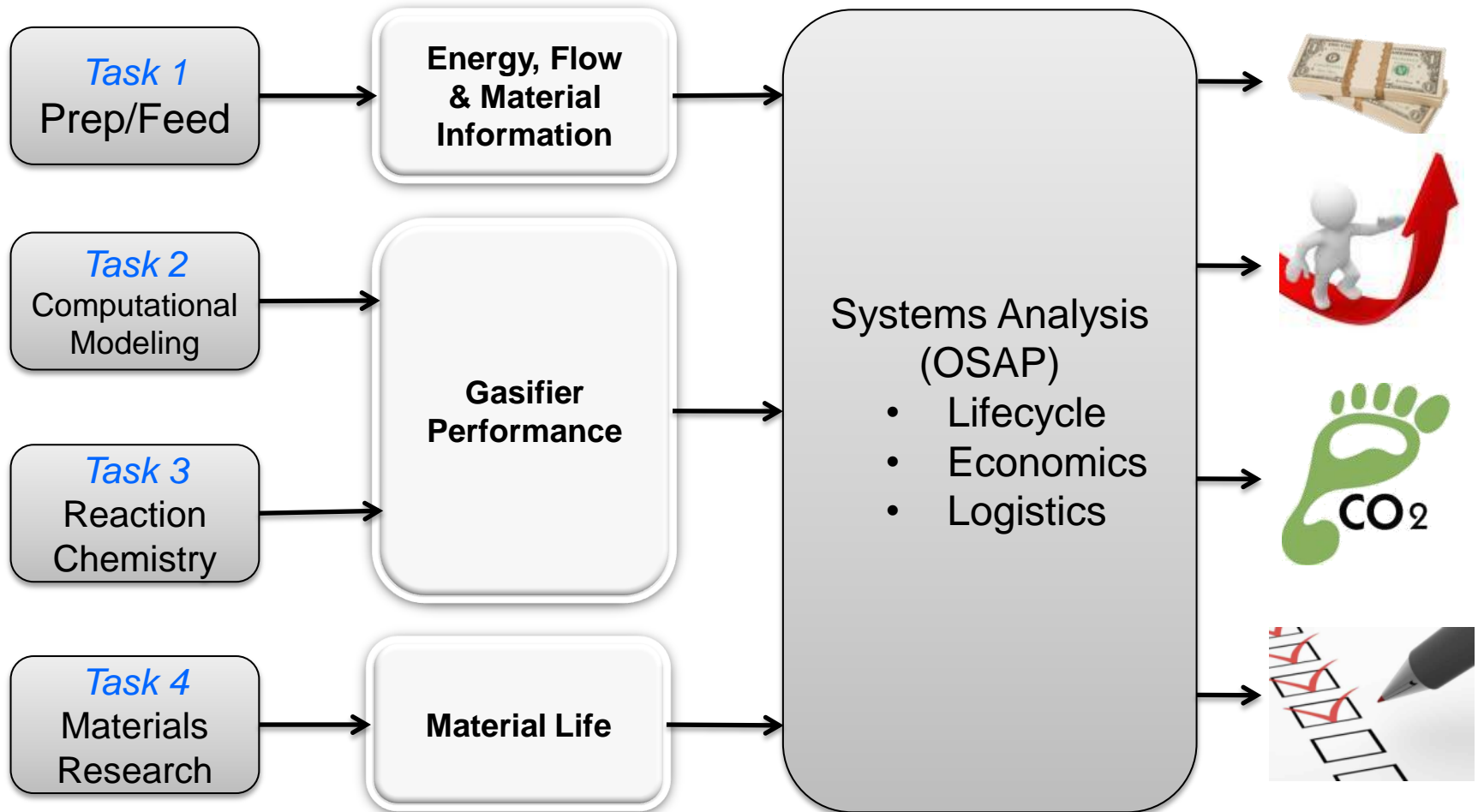
Pressurized Dry Feed

- *Technology is not mature*
- *Particle Size & Shape factors impact feeder performance*

Gasifier Performance

- *Reaction Kinetics*
- *Material Interactions*
- *Product Effects (Ash...)*
- *Models not Developed/Validated*

Program Implementation Strategy



Research Summary

Task 1 Prep/Feed

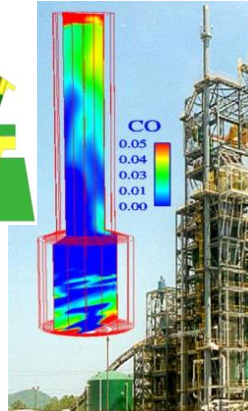
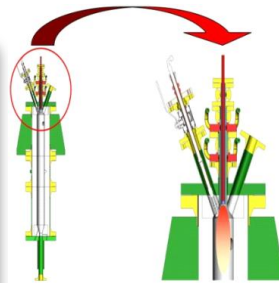
Focus

- Solve Technical Challenges in Biomass Preparation and Feeding

Active Research

- Chem./Heat Treatments
- Specific Grinding Energy
- Biomass Liquefaction
- HP Dry Feeder

Sympatec QICPIC Particle Size and Shape Analyzer



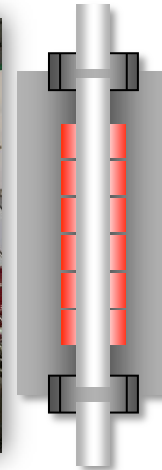
Task 3 Reaction Chemistry

Focus

- Measure Chemistry in Real Gasification Environments

Active Research

- Fixed Bed/Lurgy
- Entrained/Drop Tube
- Advanced HP



Task 4 Materials Research

Focus

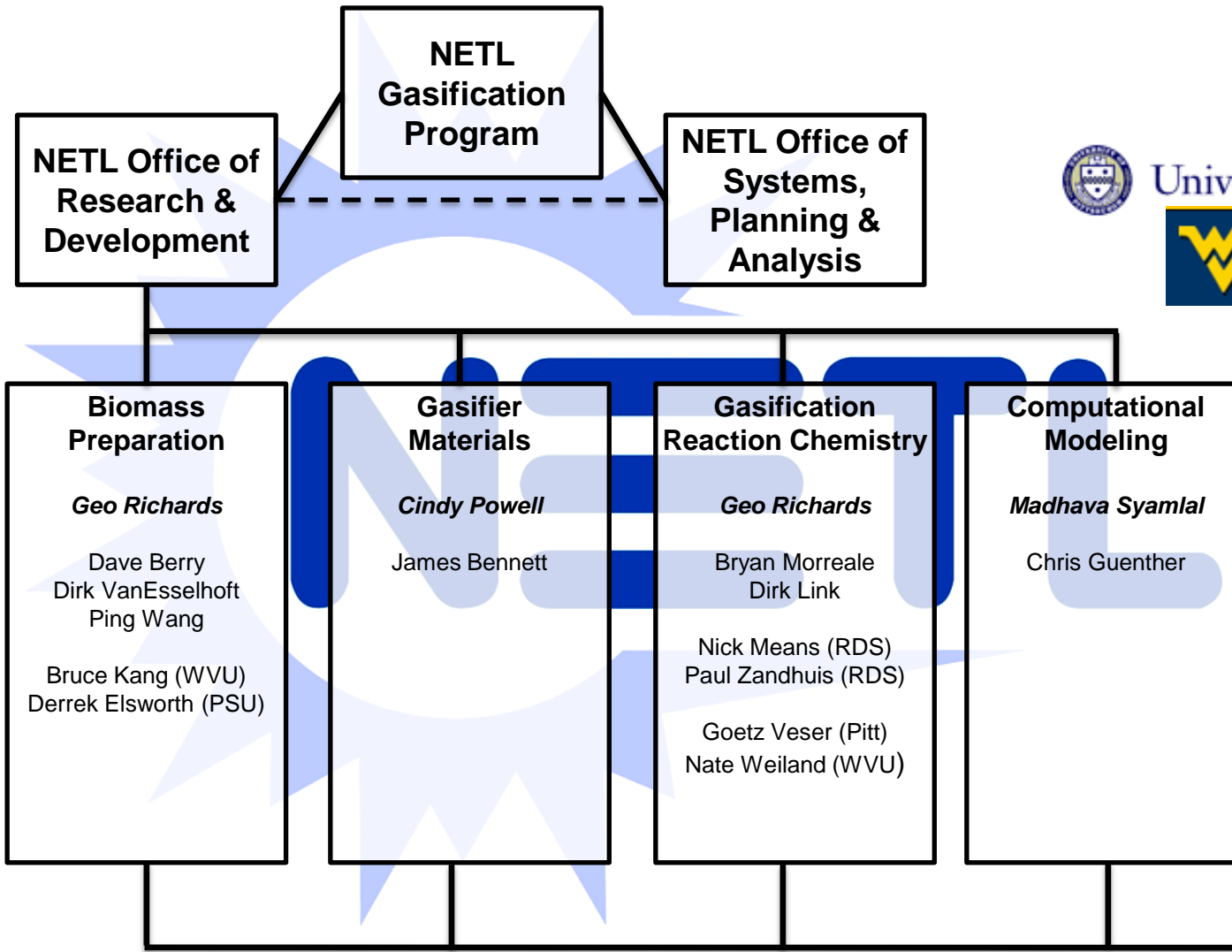
- Develop New Materials that Last Longer in Gasification Environments with Broader Chemical Compatibility

Active Research

- Refractory Materials
- Slag Modeling



Program Organization



University of Pittsburgh



Summary and Future Work

- **NETL has a wide ranging program with the goal of understanding and addressing the technical and logistical hurdles involved in co-utilization of biomass with coal in Gasification**
- **Always interested in collaboration to develop new research areas and apply technology**
- **NETL is expanding research and applying knowledge and expertise to other technical areas such as Oxy-Fuel Combustion**

Questions



Why High Pressure Dry Feeding?

Table 2 Key results for the computed IGCC cases. A single gas turbine was assumed and the plant gross power was in the 430-480 MW range. The complete power plant system was considered in the energy balance (e.g. the auxiliary power consumption for coal drying and CO₂ compression was accounted for)

Coal ID	Coal 1		Coal 2		Coal 3		Coal 4		Coal 5		
	Name		Wyoming Powder River Basin (PRB)		Illinois #6		Upper Freeport, PA		Pocahontas #3, VA		
Capture of CO ₂		Without	With	Without	With	Without	With	Without	With	Without	With
Case 1 (Dry feed with syngas heat recovery)											
Coal as-received [kg/s/MW]		0.131	0.171	0.115	0.149	0.089	0.115	0.071	0.091	0.083	0.082
Water removed [kg/s/MW]		0.038	0.049	0.028	0.036	0.003	0.004	0.000	0.000	0.000	0.000
CO ₂ captured [kg/kWh]		0.000	0.848	0.000	0.815	0.000	0.767	0.000	0.735	0.000	0.780
Net power [MW]		410	343	412	346	420	353	421	358	419	353
Thermal efficiency (ar, HHV)		44.1 %	33.7 %	44.3 %	34.3 %	44.2 %	34.1 %	45.6 %	35.7 %	45.7 %	35.3 %
Thermal efficiency (ar, LHV)		48.1 %	38.8 %	47.9 %	37.0 %	46.1 %	35.6 %	47.0 %	38.8 %	47.0 %	36.3 %
CO ₂ emitted [kg CO ₂ / kWh e]		0.762	0.147	0.740	0.143	0.698	0.137	0.679	0.132	0.709	0.138
Case 2 (Slurry feed with full water quench)											
Coal as-received [kg/s/MW]		0.305	0.432	0.199	0.251	0.120	0.140	0.088	0.098	0.076	0.089
CO ₂ captured [kg/kWh]		0.000	2.163	0.000	1.377	0.000	0.929	0.000	0.765	0.000	0.815
Net power [MW]		300	220	328	282	357	331	370	351	366	339
Thermal efficiency (ar, HHV)		18.9 %	13.4 %	25.7 %	20.4 %	32.6 %	27.9 %	37.6 %	33.0 %	38.1 %	32.4 %
Thermal efficiency (ar, LHV)		20.6 %	14.6 %	27.7 %	22.0 %	34.0 %	29.1 %	38.7 %	34.0 %	39.1 %	33.3 %
CO ₂ emitted [kg CO ₂ / kWh e]		1.704	0.253	1.227	0.168	0.907	0.131	0.790	0.136	0.817	0.143

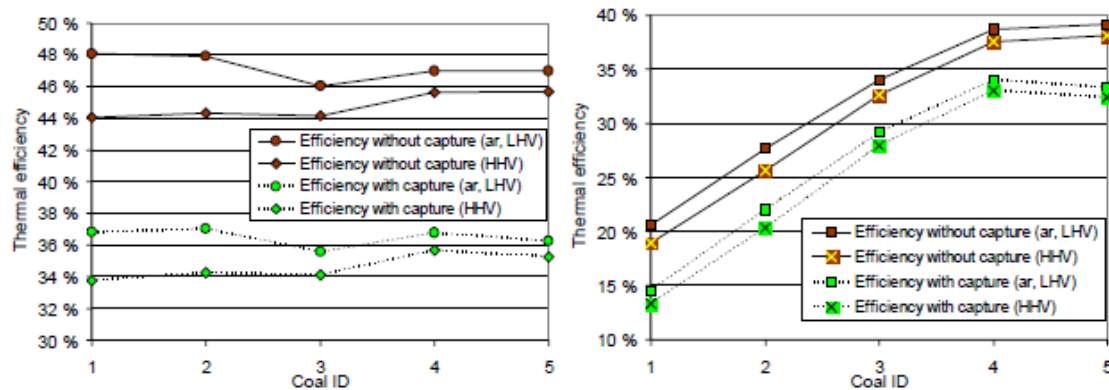


Figure 2 a) Efficiencies for Case 1 (IGCC with dry feed gasifier and heat recovery),
b) Efficiencies for Case 2 (IGCC with slurry feed gasifier and water quench)

Maurstad, O., H. Herzog, et al. (2006). Impact of Coal Quality and Gasifier Technology on IGCC Performance. 8th International Conference on Greenhouse Gas Control Technologies. Trondheim, Norway.

Background

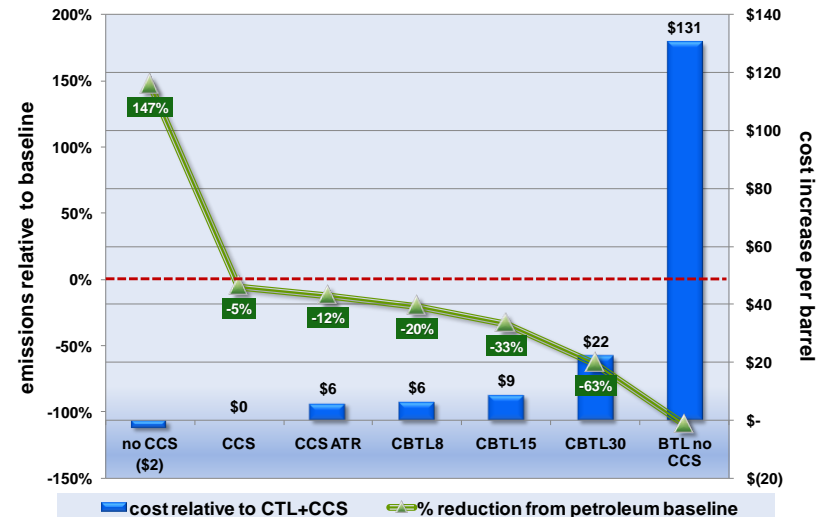
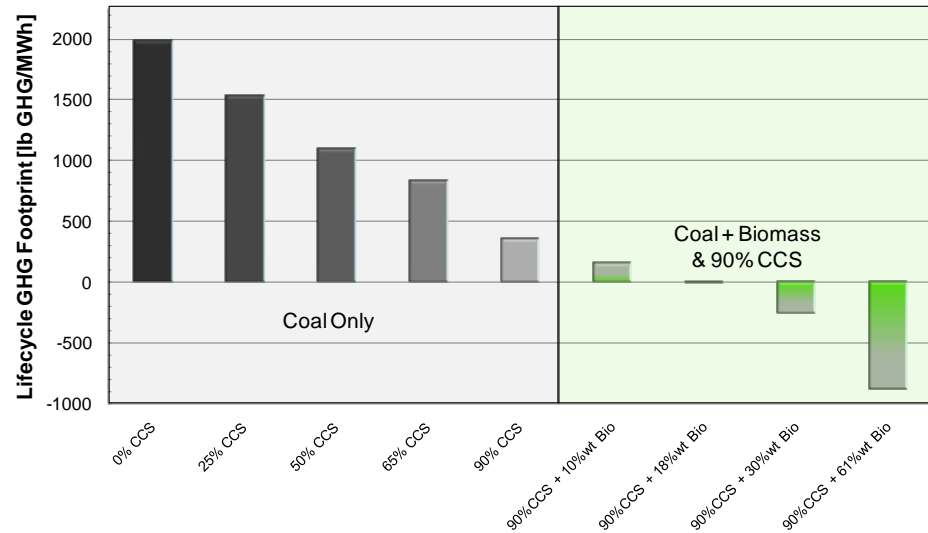
Coal

- National resource with over 200 years supply
- Currently supplies over 50% of US power
 - Potential to supply transportation fuels

Biomass

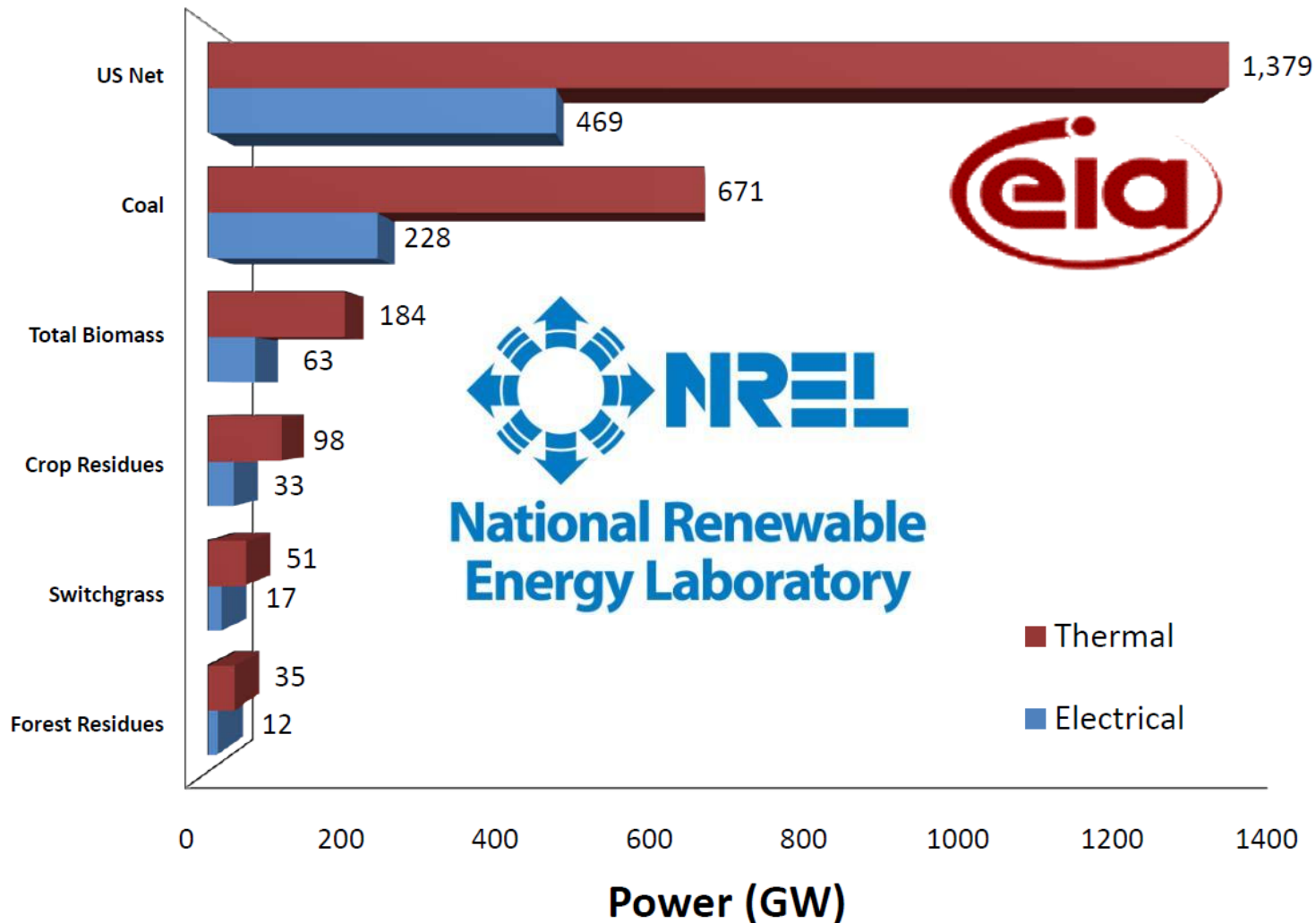
- Carbon neutral
- Renewable

Reducing GHG Footprint with Carbon Capture & Biomass



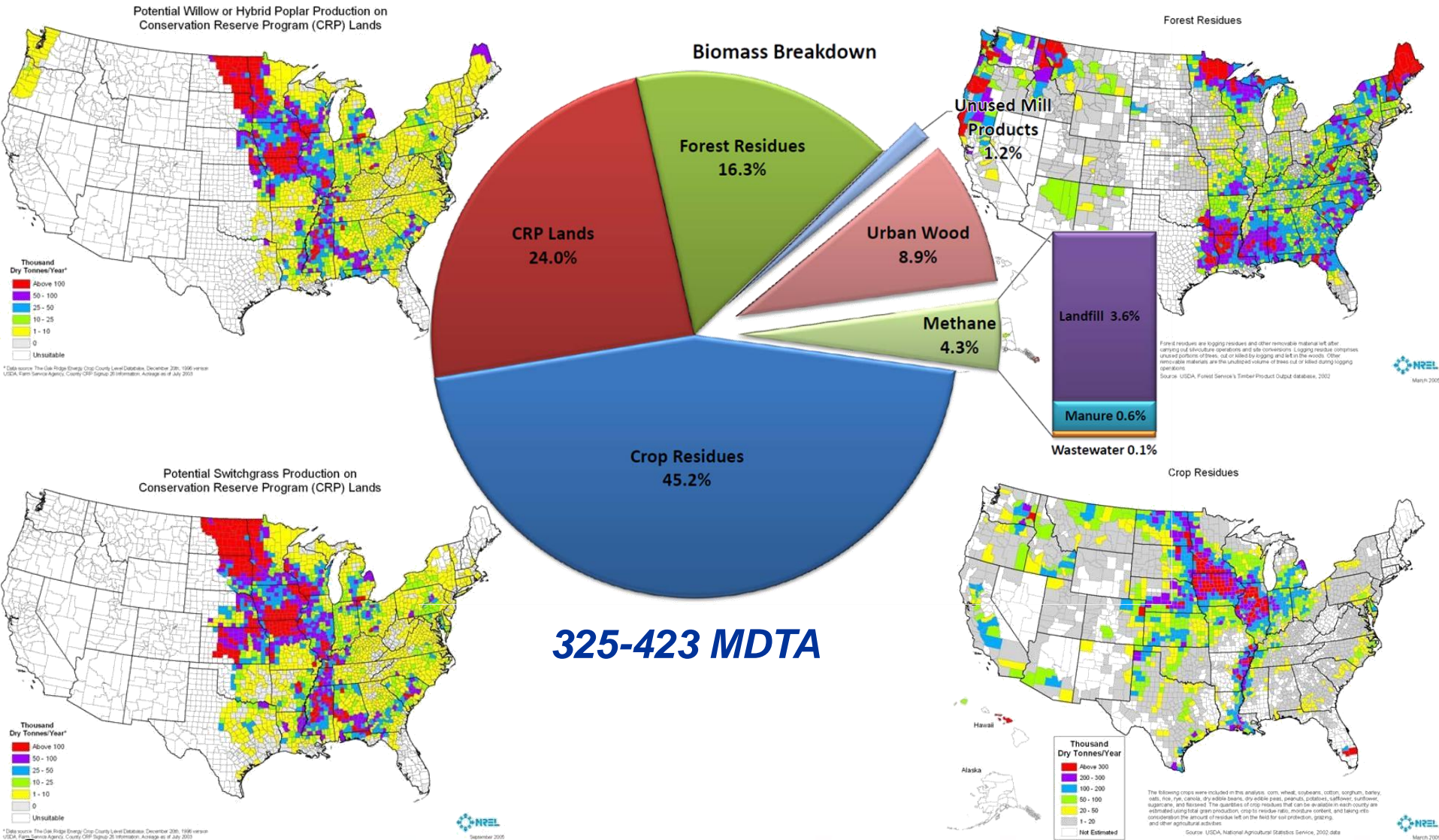
Project Overview

How Significant of a Resource is Biomass?



Project Overview

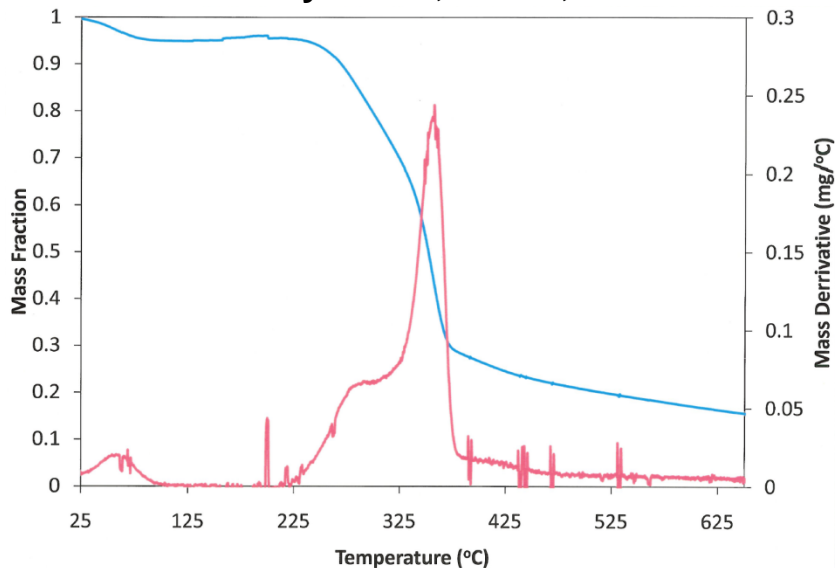
Where is Biomass Located in the US?



Task 1: Biomass Preparation & Feeding

Example of Preprocessing Results: Torrefaction

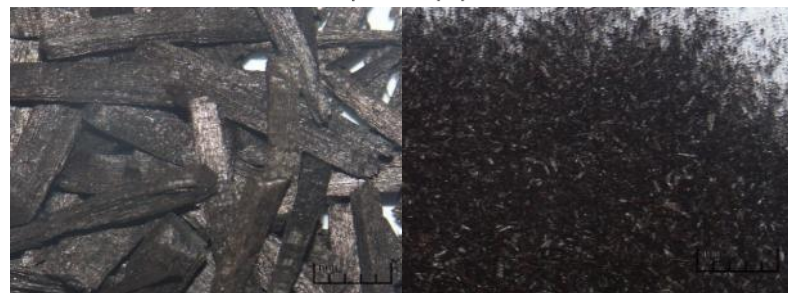
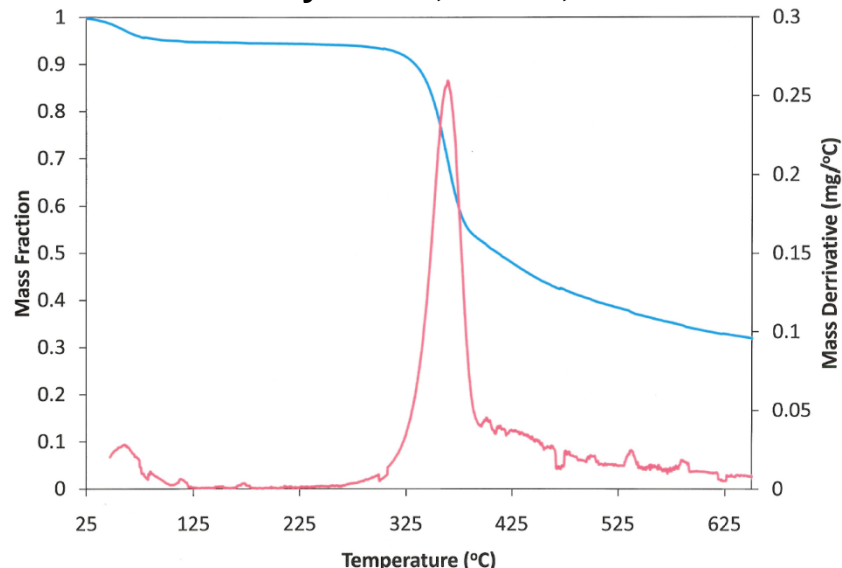
Cherry Wood, 200°C, 1hr



Before and After Grinding for 6 min in a 3" Ball Mill

Young's Modulus = 1.63 +/- 0.26

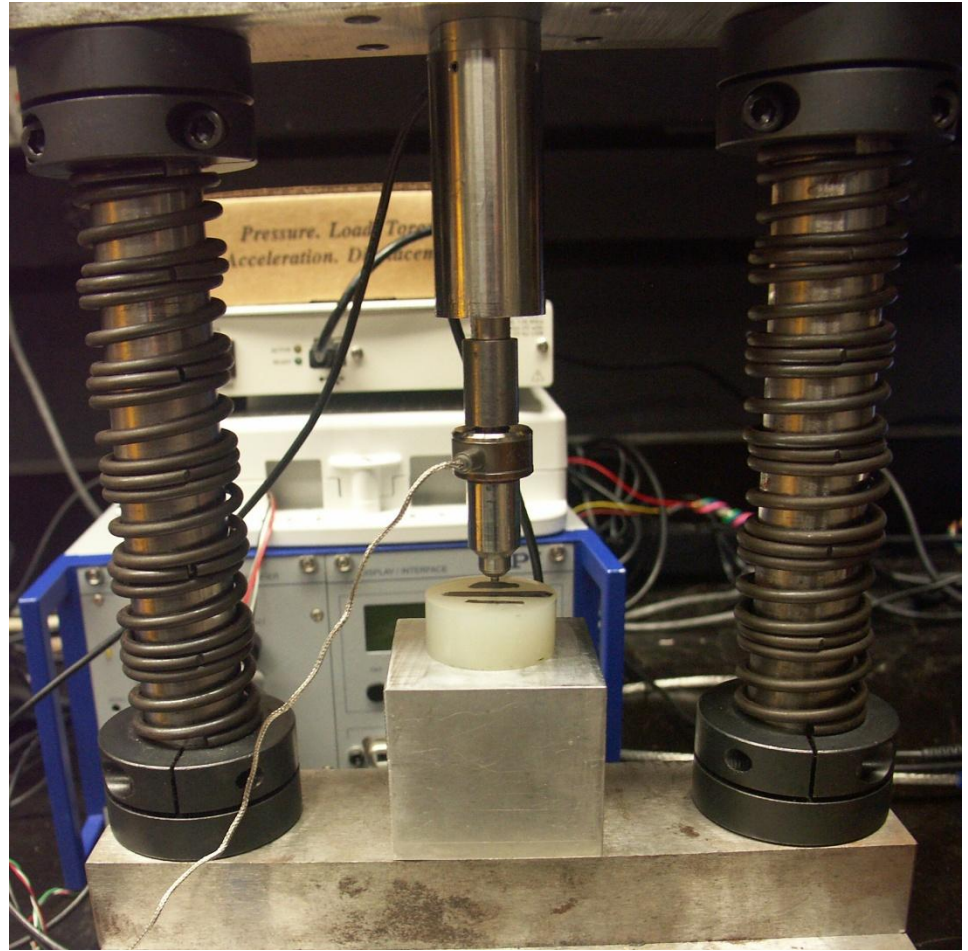
Cherry Wood, 280°C, 1hr



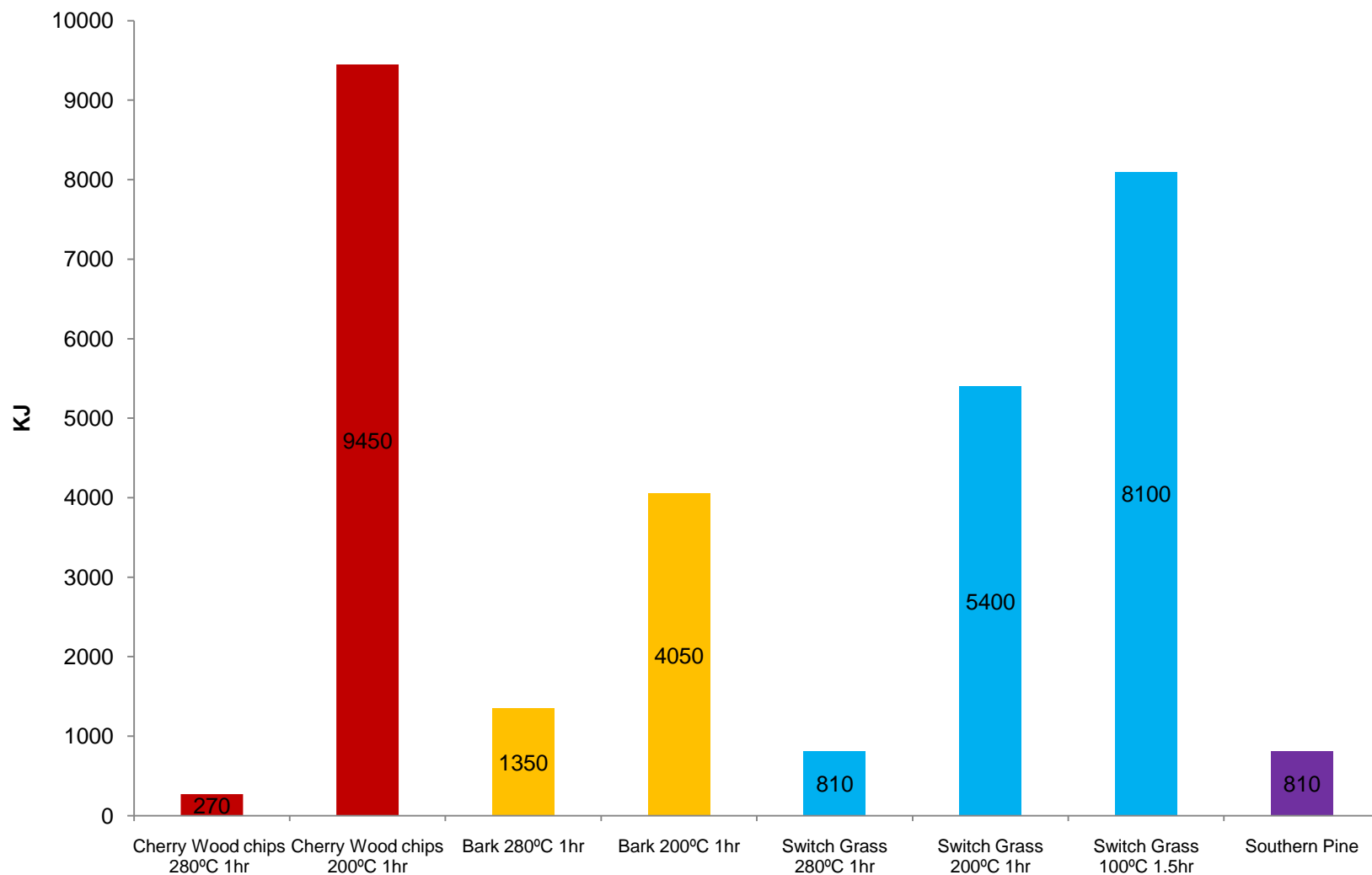
Before and After Grinding for 6 min in a 3" Ball Mill

Young's Modulus = 0.67 +/- 0.21

Young's Modulus Measurement

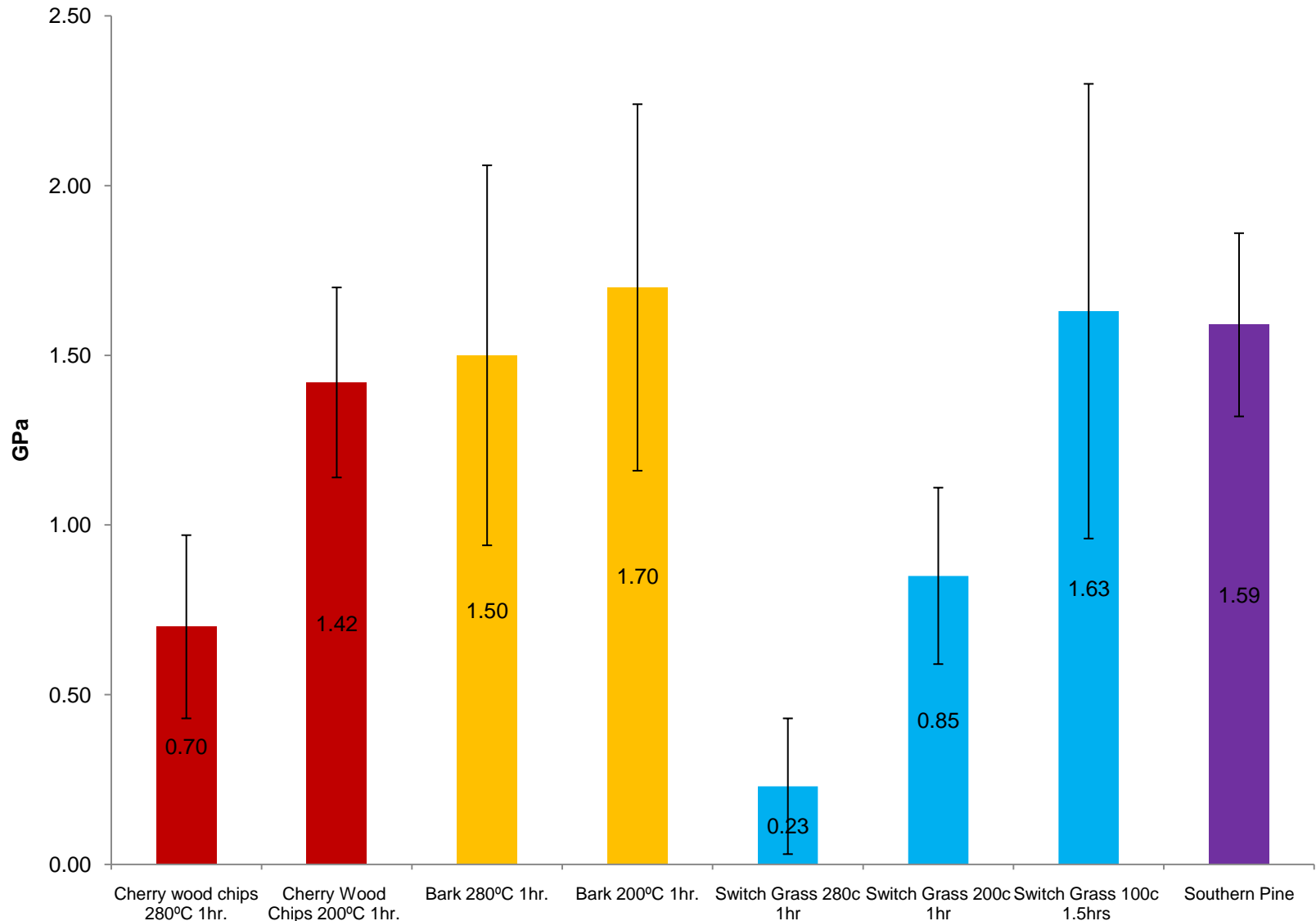


Energy Consumption



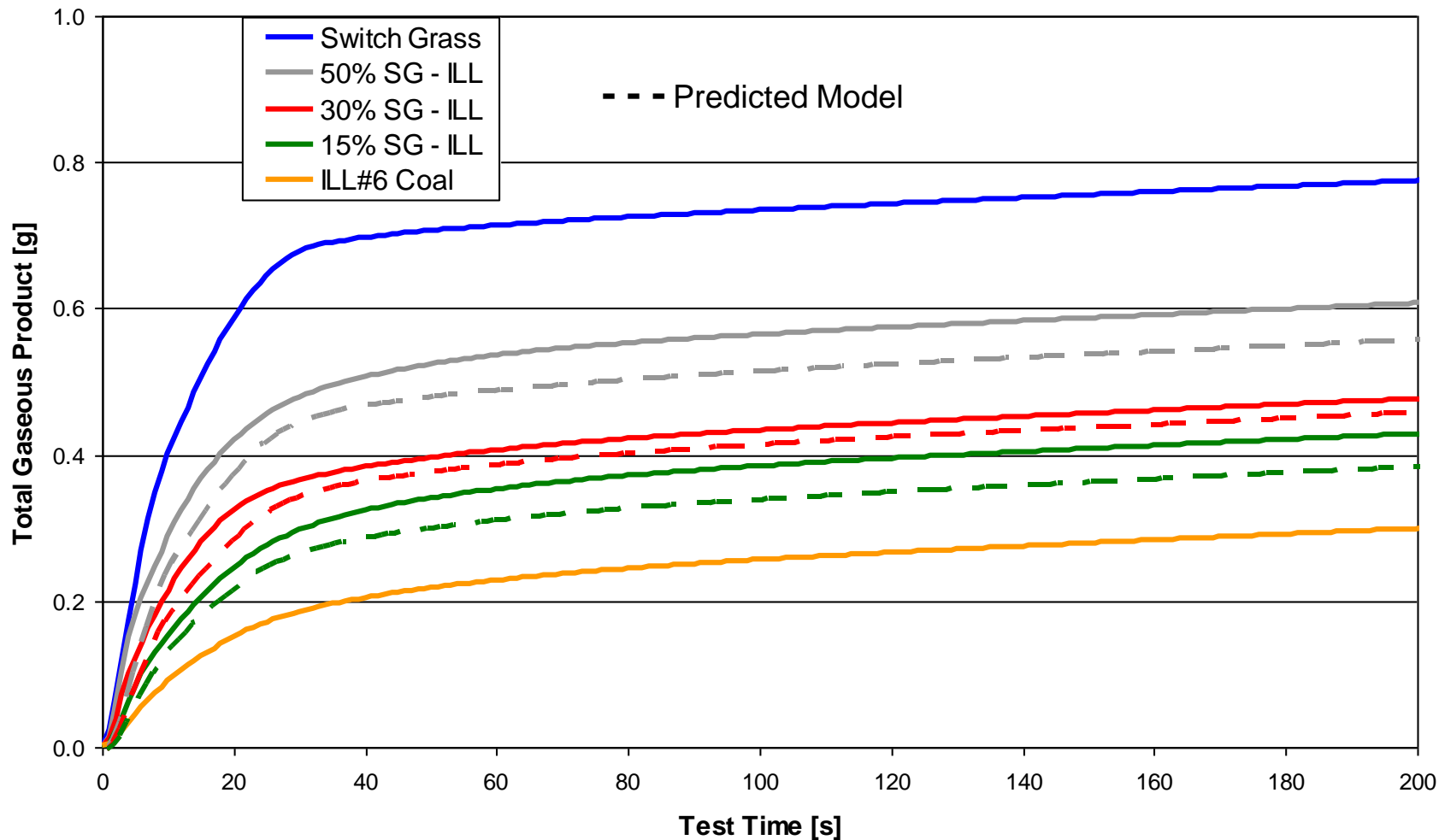
**** Energy consumption of the Ball Mill Instrument, not the actual grinding energy on the biomass materials**

Young's Modulus of Biomass Materials



Task 3. Gasifier Reaction Chemistry

Influence of Co-Feeding on Gaseous Products

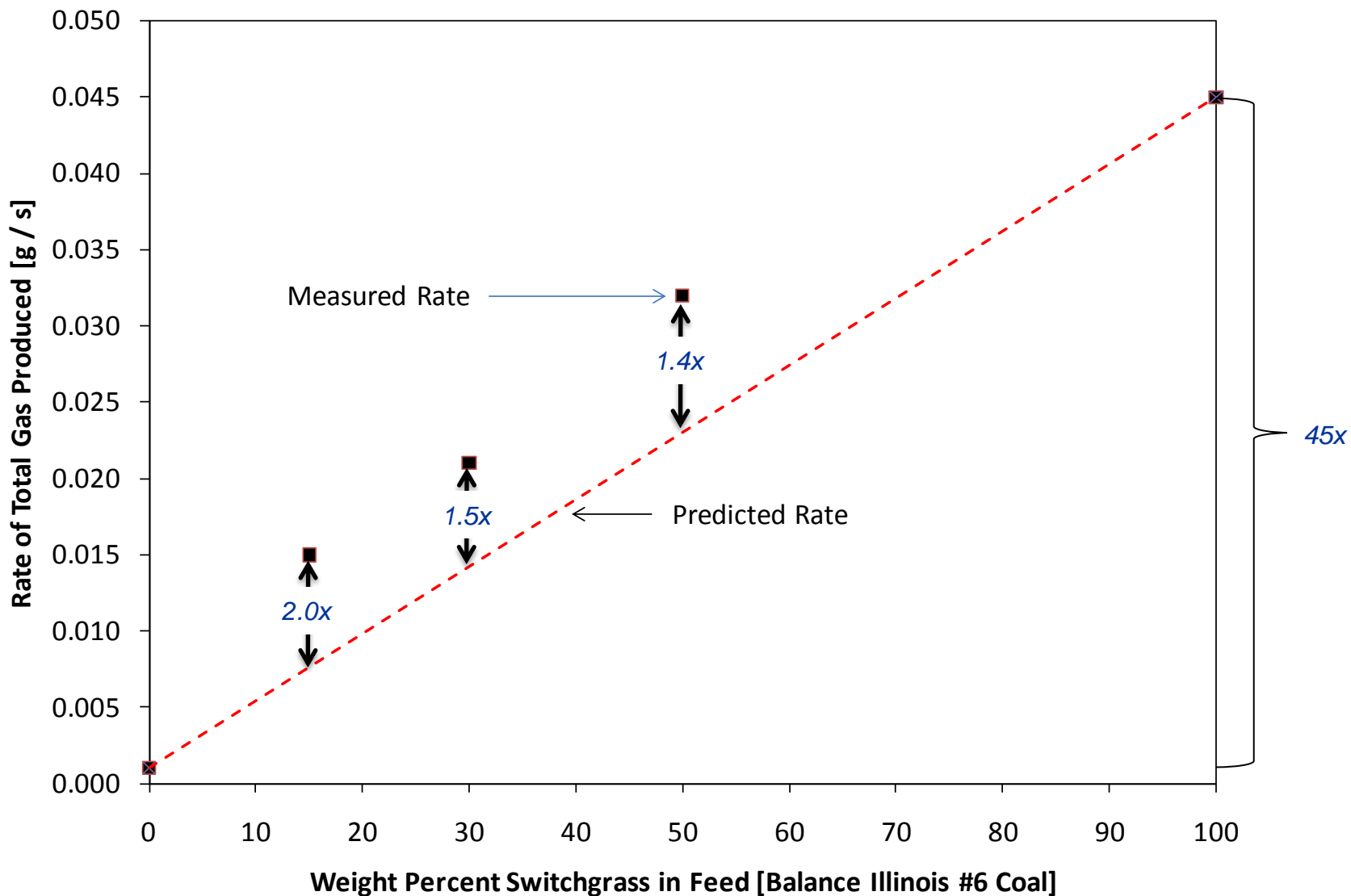


Total feed load of 1g

$$\text{Prediction} = [(x_{\text{biomass}}) * (m_{\text{biomass}})] + [(x_{\text{coal}}) * (m_{\text{coal}})]$$

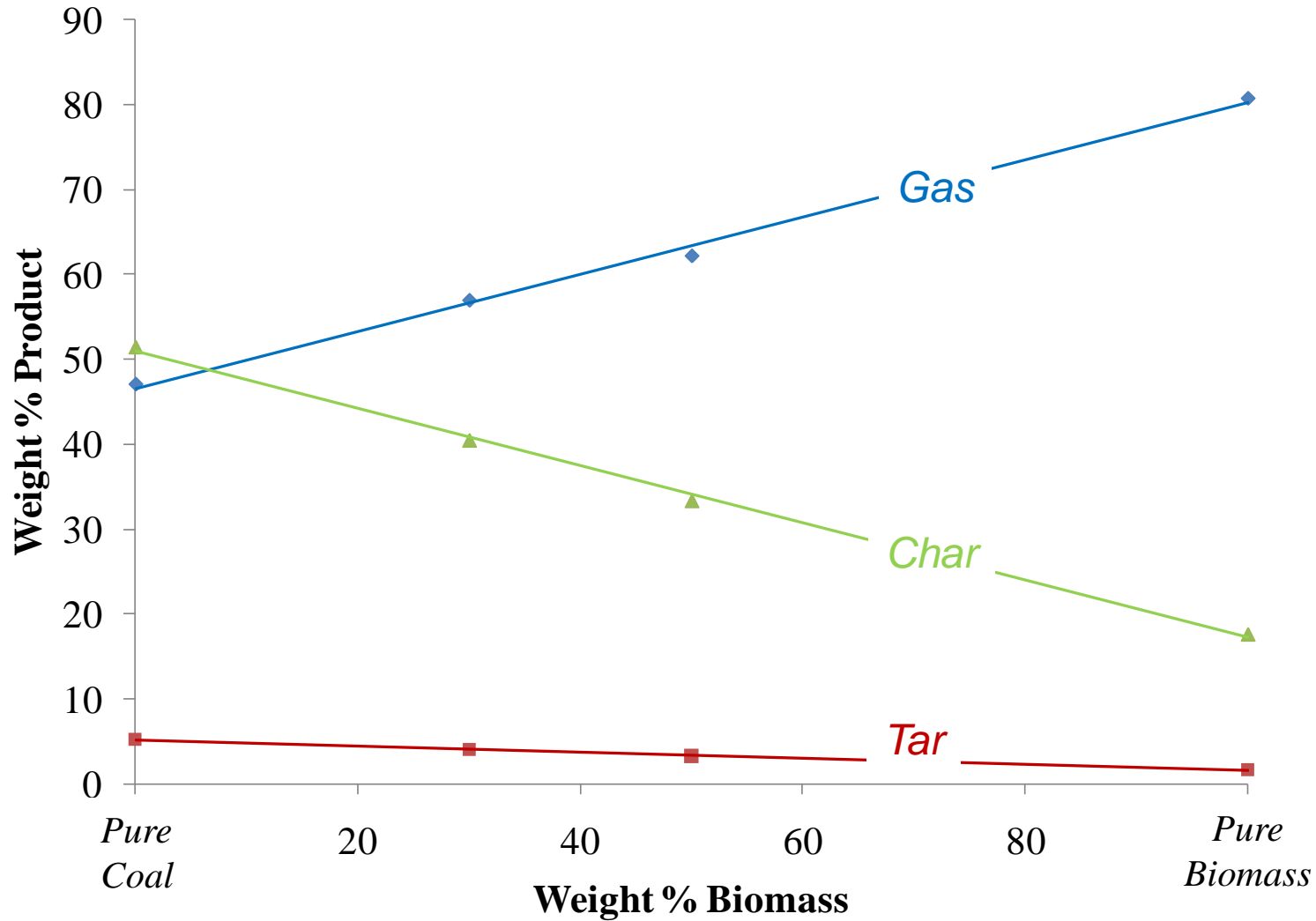
Task 3. Gasifier Reaction Chemistry

Influence of Co-Feeding on Gaseous Products



Task 3. Gasifier Reaction Chemistry

Product Distribution Trends



Task 4: Gasifier Materials

Refractory Material and Slag Testing

Biomass Data

Task 1
Task 3

INPUT

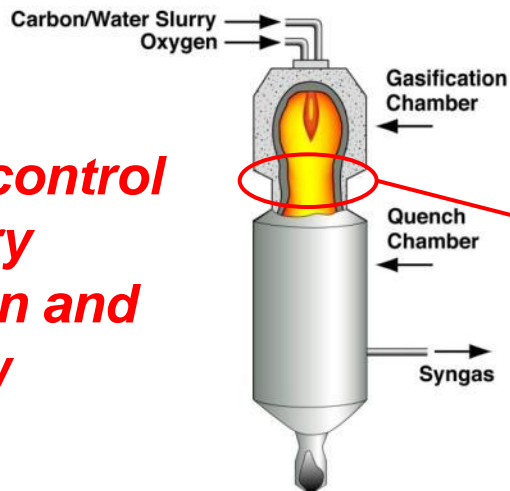
- Ash Data
 - chemistry
 - quantity
 - pct.
- Gasifier Conditions
 - temperature
 - gas environment

COMPUTER MODEL

- Thermodynamic Computations
- Computer Modeling Predictions
- Literature
- Laboratory Test Data

OUTPUT

- Melting point
- Solid Phases Formed
- Slag Viscosity
- Refractory/Slag Interactions
- Additives to Control Slag Viscosity/Corrosion
- Vapor Phases Formed



GOAL: control refractory corrosion and slag flow

