

# McIlvaine NOx Reduction Innovations for Coal Fired Plants

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**steag**

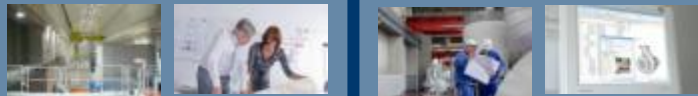
## STEAG GmbH



### Power Operations and Engineering Services

Power O&M services Worldwide  
Operations in India, Spain, Brazil, Colombia, Philippines, etc.  
Ownership & Operations of solar, wind, fossil fuel, natural gas,  
biogas and geothermal  
Over 20,000 MW's of operation worldwide

## STEAG Energy Services GmbH



### Engineering and Consulting Services

Complete Plant Integration Services  
Owners A/E Services  
Operations in Europe, India, Turkey, South Africa and the US

## STEAG Energy Services LLC



### Engineering and Consulting Services (USA)

Worldwide STEAG group NOx Expert  
HQ and Plants in NC - Offices in PA, IL, DC  
500,000 ft<sup>2</sup> of warehouse space  
60,000 m<sup>3</sup> regenerated, 4,000 XRF's annually,  
2 x 2013 VGB certified bench scale reactors

# “The Basics”

## The SCR Catalyst / Reactor



### Catalyst Oxidation Reactions

- NO<sub>x</sub> Reaction -  $\text{NH}_3 + \text{NO} (\text{NO}_2) \rightarrow \text{H}_2\text{O} + \text{N}_2$
- SO<sub>x</sub> Reaction –  $\text{SO}_2 + \text{O}_2 \rightarrow \text{SO}_3$
- Mercury Reaction –  $\text{Hg} + \text{O}_2 \rightarrow \text{HgO}$

### Where / When do the reactions occur?

- NO<sub>x</sub> Reaction – Quick Reaction
- SO<sub>x</sub> Reaction – Slow Reaction
- Mercury Reaction – Quick Reaction – NO<sub>x</sub> is preferential

### What is STEAG Doing on it's Units for Mercury

- Primary Mercury oxidation is layer
- Secondary is Bromide Addition
- Re-emission is by PAC into the FGD Unit

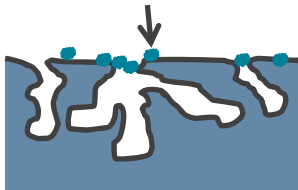


# “The Basics” Catalyst Regeneration



- Chemically removing De-activating compounds

Small Fly Ash Particles



i.e. Fly Ash

Dense Second-phase Coating



i.e. Calcium,  
Magnesium

Pore System Catalyst Surface Active Sites



i.e. Arsenic,  
Phosphorus, Sodium,  
Potassium

PRB

- Removal of Chemicals and Ions from Catalyst
- Addition of the activating compound (Vanadium) and strength metals (Tungsten or Molybdenum) back onto the catalyst



# “The Basics” Longevity of Catalyst



- **STEAG has catalyst that has been regenerated 7 time (26 years in operation)**
- **What should a customer buy?**

	Honeycomb	Plate
Wall Thickness	> 0.8 mm	> 0.7 mm
Tungsten or Molybdenum	>7%	
Metal Substrate	N/A	Austenitic Stainless

- **Anything less will lead to throw away catalyst!**
- **Catalyst Disposal Issues:**
  - **Ash disposed of as non-hazardous (40 CFR)**
  - **Ceramic Material Non-hazardous**
  - **Metal recycled. China working on ceramic recycle**
  - **Future CCP could affect this!**



# Innovation: Co-coupling of SCR & SNCR



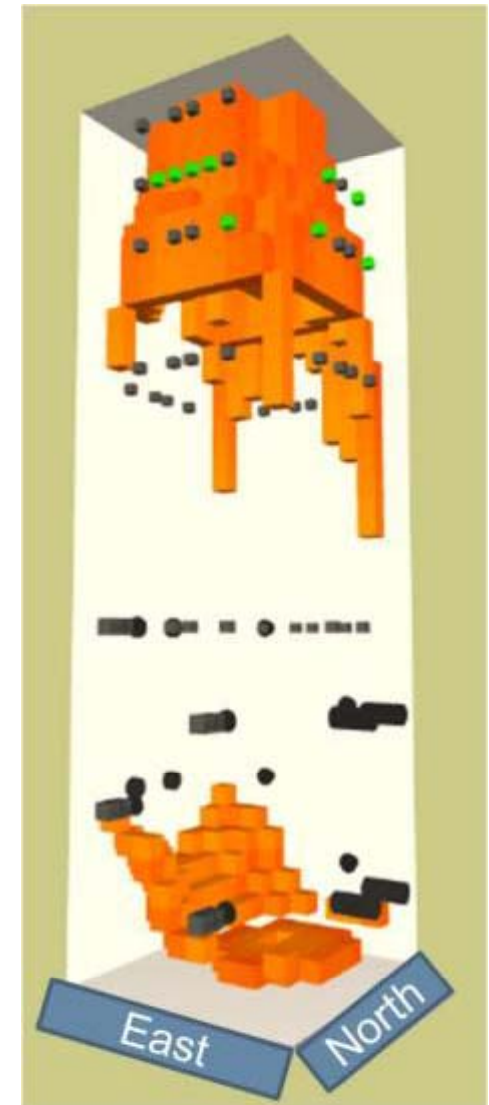
**STEAG is working on Strategy on STEAG units for co-coupling of SNCR with SCR.**

- **Need for additional removal on STEAG units 60% to 80% or 80% to 90%.**

	Case 1: Stretching the SCR			Case 2: Stretching the SCR		
	No SNCR	Typical SNCR	STEAG Approach	No SNCR	Typical SNCR	STEAG Approach
Boiler Inlet	250	250	250	250	250	250
SNCR Reduction	0%	25%	50%	0%	25%	50%
SCR Inlet	250	188	125	250	188	125
SCR reduction	60%	60%	60%	80%	80%	80%
NOx Outlet	100	75	50	50	38	25
Total Reduction	60%	70%	80%	80%	85%	90%

**How to achieve 50% reduction with SNCR?**

- **More injectors**
- **Live CFD modeling (STEAG Powitec System)**



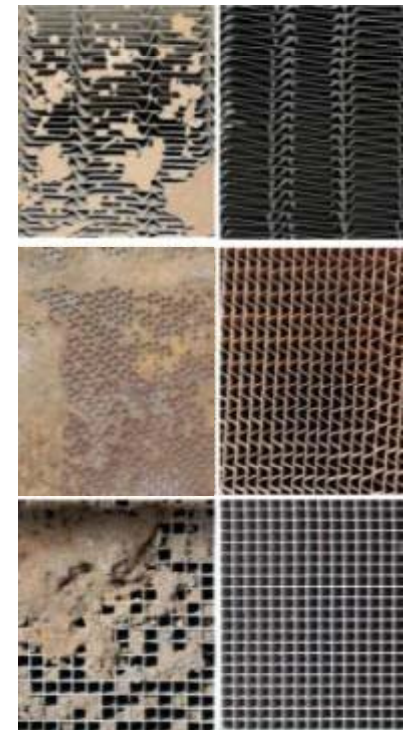
# Innovation: In-situ Dry Cleaning in the Reactor



United States Patent No 8,268,743 B2

Removal Systems	Benefits	Challenges
Vacuuming	Large ash removal	Top ash only
Air Lancing	Mechanical/light ash removal	Only 4-6 inches of pluggage removal
Mechanical Shakers	Large ash removal	On-site plate removal Honeycomb "verboden"
Reactor Shakers	Large ash removal	Unknown long-term reactor effects
Scraping / Poking	Mechanical/light ash removal	Damages the catalyst surface – Logs normally need to be replaced before regeneration
High Pressure Wash	Large ash removal	Water reacts with SO <sub>3</sub> to form sulfuric acid, which deteriorates the metal substrate in plate, solidifies any remaining ash and releases iron oxide in ash to increase SO <sub>2</sub> /SO <sub>3</sub> conversion rate
Dry Ice Blasting	Mechanical cleaning for all types of catalyst	Unable to undo damages caused by other cleaning techniques

Before After



- **Most effective and very safe cleaning method**
- **Our process has reduced pluggage from 100% down to < 5%**
- **Savings in Pressure Drop alone provides 6 to 8 month payback**
- **Successful performed on all Catalyst Types**

# Innovation: Regeneration & Mercury

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- **Catalyst Re-calcination**
  - Heat treatment above 800 °F but below 850 °F
  - Time is 9 to 12 hours
  - Regain strength, bond material and eliminate inherent water
- **Single Impregnation of Vanadium (activating compound) with tungsten or molybdenum (strength metals)**
- **Mercury Testing**
  - STEAG has acquired the testing facility from Martin Luther University (Halle-Wittenberg) – Research before 2002
  - STEAG continues the work and has several testing contracts
- **What is STEAG doing on it's Units for Mercury**
  - Primary Strategy - Mercury oxidation is lower layer of catalyst
  - Secondary Strategy – Trim with Bromide Addition
  - Capture Oxidized Mercury in the wFGD with Re-emission is by PAC into the FGD Unit
  - STEAG has Patented Mercury removal technology for wFGD water





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