



Improving Silica Removal By EDI and GTM

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*Michael J. Snow, Ph.D.
President
SnowPure Water Technologies (USA)*

makers of
Electropure EDI
products

SnowPure
High Technology Water

makers of
Electropure EDI
products

Headquarters

San Clemente,
California



Electropure™ EDI Operating in 49 Countries



The Electropure™ EDI History

- **1977** Harry O'Hare EDI Prototype
- **1979** HOH Water Technology founded
- **1984** HOH EDI Patent Issued
- **1988** EPM series EDI
- **1996** HOH becomes Electropure
- **1999** Excellion™ IX Membrane Patents
- **1999** XL™ series EDI
- **2004** XL-HTS™ High Temperature Stable
- **2005** Electropure Management Buyout--SnowPure formed
- **2006** Electropure China Sales Office Opened
- **2007** XL-R™ series EDI improvements
- **2008** SnowPure International (Hong Kong) formed
- **2009** EXL™ series EDI introduced in China
- **2010** EXL™ series EDI introduced worldwide
- **2012** EXL-HTS high volume, high temperature for sanitization
- **2013** XL-DER EDI for Hemodialysis

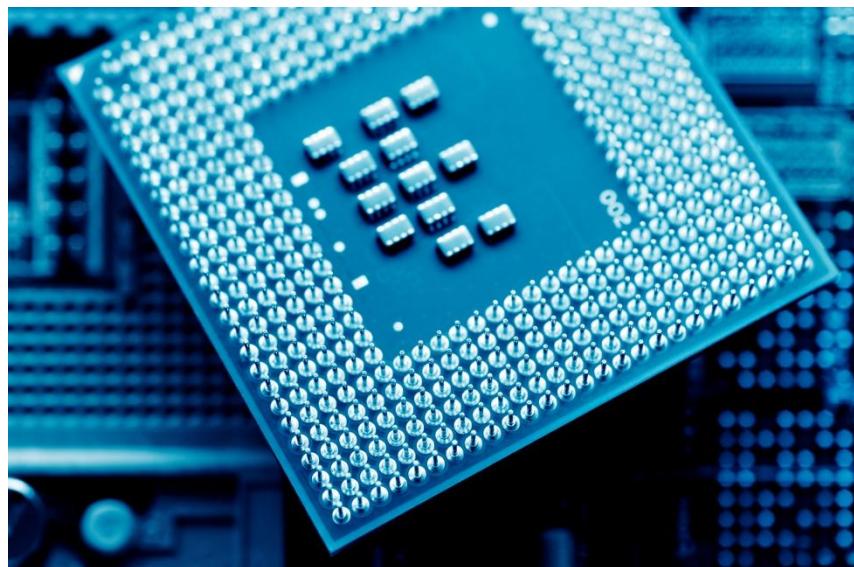
Agenda

1. Importance of Silica for Power Plants
2. Old EDI Model: Working Bed - Polishing Bed
3. New EDI Model: Electropure Specific Ion Model
4. Discussion: Specific RO-EDI Cases
5. Rules to Optimize SiO_2 in EDI

Silica is Important in Power Plants and Electronics

Semiconductor Fabs

$\text{SiO}_2 < 0.1 \text{ ppb}$

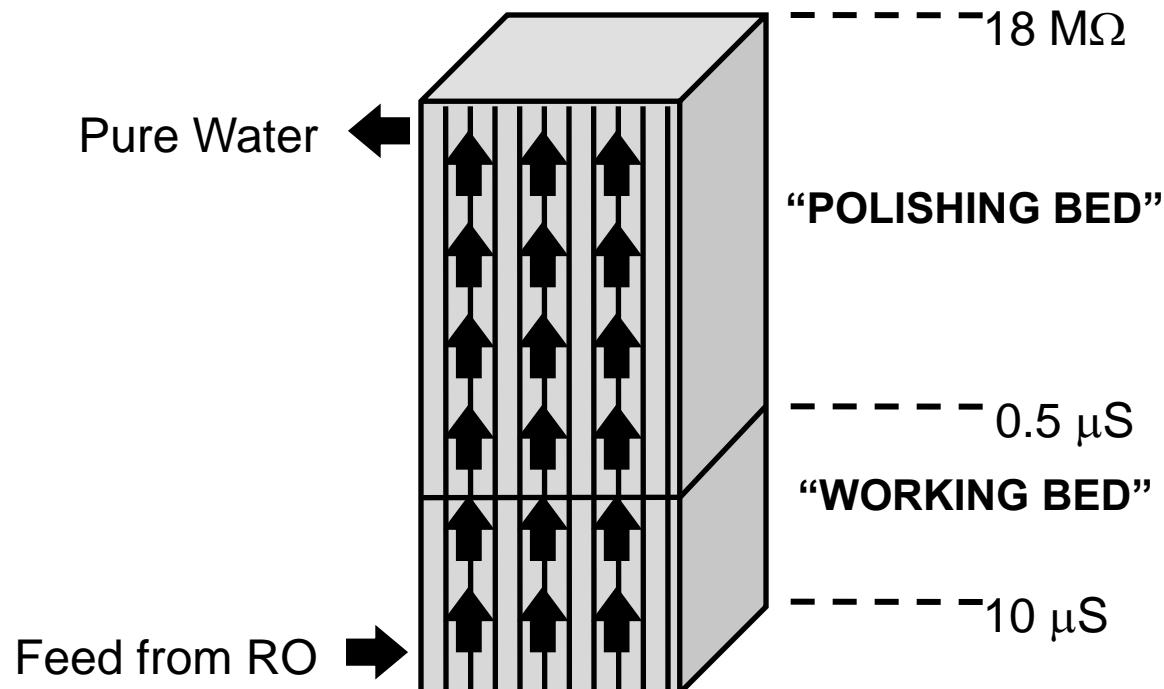


Combined Cycle High Pressure Boilers

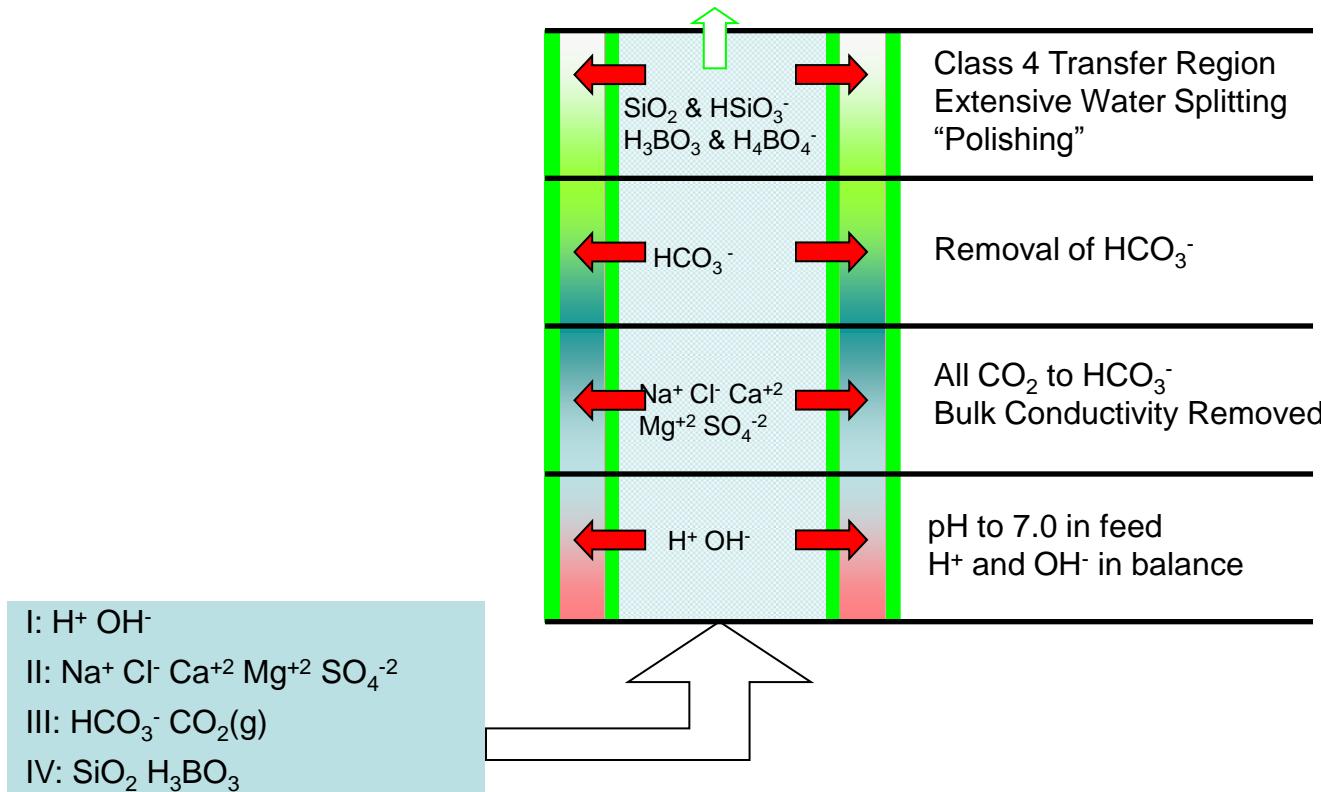
$\text{SiO}_2 < 5 \text{ ppb}$



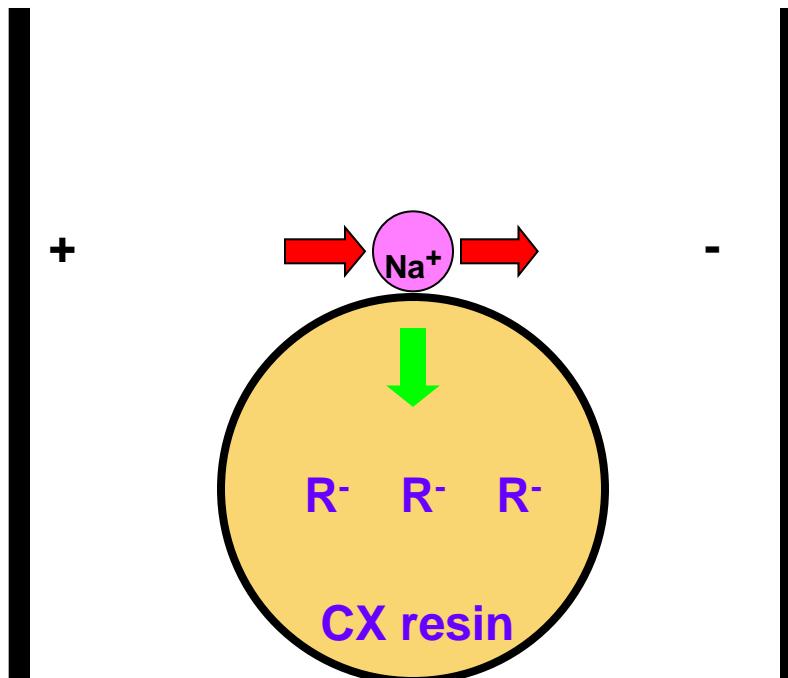
Old EDI Model: Working Bed-Polishing Bed



Electropure's New Specific Ion Model

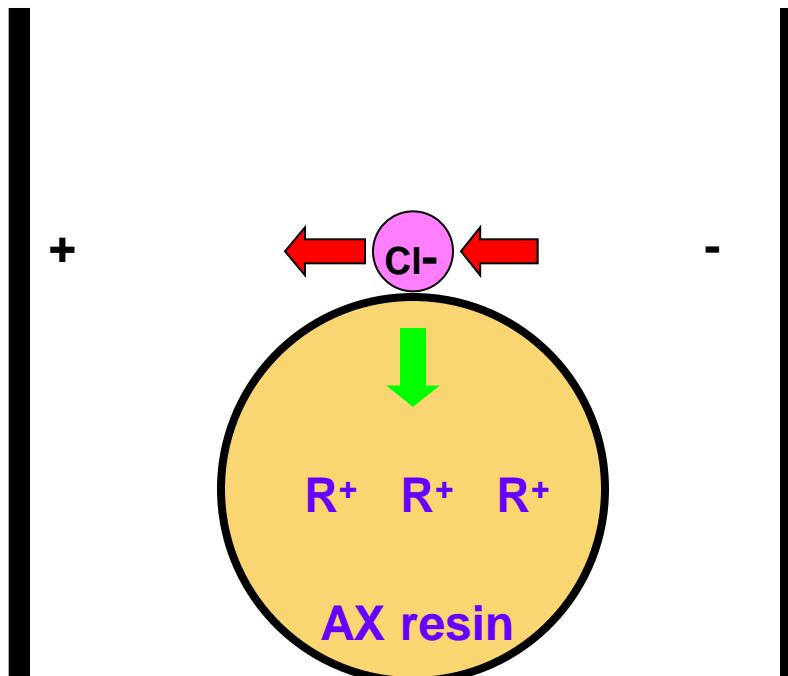


Forces on Cations in EDI



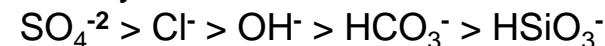
- Force 1:
 - Electrical Attraction to resin
 - K, Selectivity Coefficient
 - Force 2:
 - Electrical attraction to electrodes
 - E, Charge/Mass
-
- K, Selectivity Coefficient
 - $\text{Ca}^{+2} > \text{Mg}^{+2} > \text{K}^+ > \text{Na}^+ > \text{H}^+$
 - E, Electrical Force/Mass
 - $\text{H}^+ > \text{Mg}^{+2} > \text{Ca}^{+2} > \text{Na}^+ > \text{K}^+$

Forces on Anions in EDI

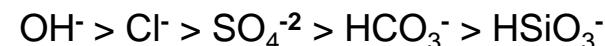


- Force 1:
 - Electrical Attraction to resin
 - K, Selectivity Coefficient
- Force 2: ul>- Electrical attraction to electrodes
- E, Charge/Mass

K, Selectivity Coefficient



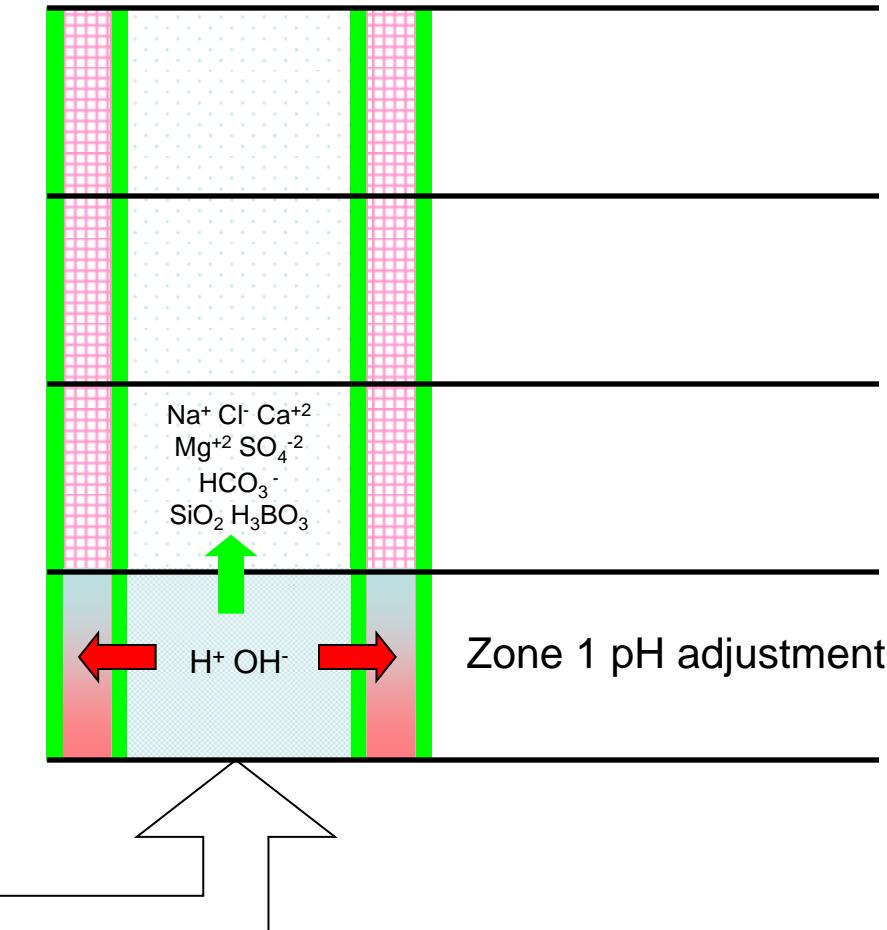
E, Electrical Force/Mass



Electropure's 4 Classes of Ions

Electropure™ Ion Class	Characteristics	Example Ions
Class 1	Low Selectivity High Mobility	H^+ OH^-
Class 2 “Conductivity”	High Selectivity Medium Mobility	Ca^{+2} Mg^{+2} Na^+ Cl^- SO_4^{-2}
Class 3 “Bicarbonate”	Low Selectivity Low Mobility Moderate Charge, Polar at pH 7	HCO_3^- pK = 6.3
Class 4 “Weakly Ionized Ions”	Very Low Selectivity Very Low Mobility Low charge at pH 7	HSiO_3^- pK = 9.8 H_4BO_4^- pK = 9.3

Class1: H⁺ and OH⁻



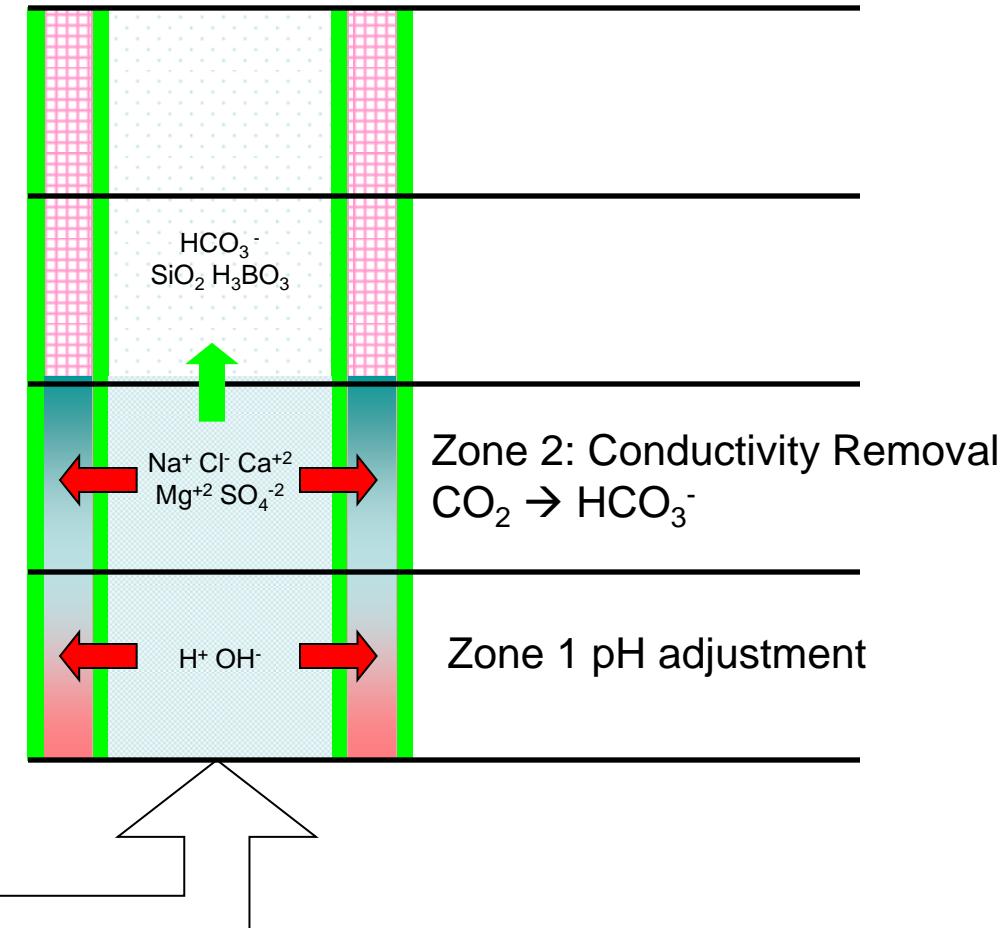
1: H⁺ OH⁻

2: Na⁺ Cl⁻ Ca⁺² Mg⁺² SO₄⁻²

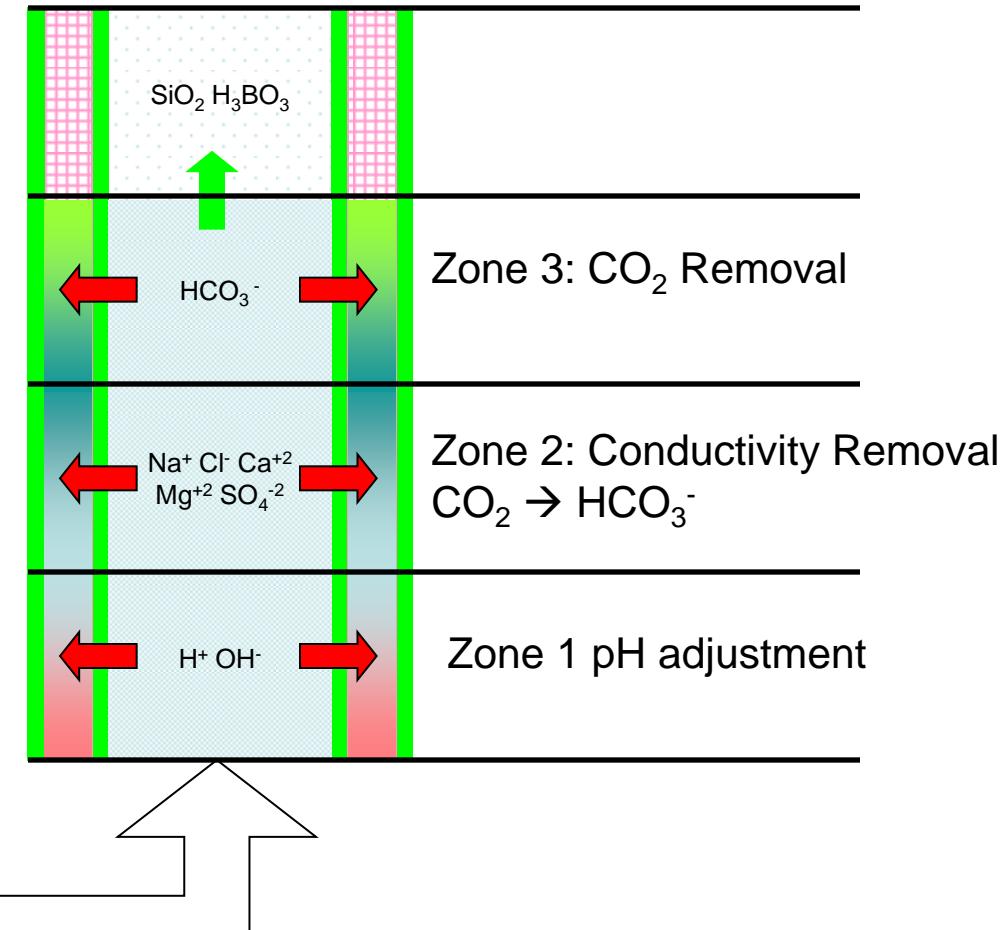
3: HCO₃⁻ CO₂(g)

4: SiO₂ H₃BO₃

Class 2: Easy Ions



Class 3: Bicarbonate Ion
 HCO_3^-



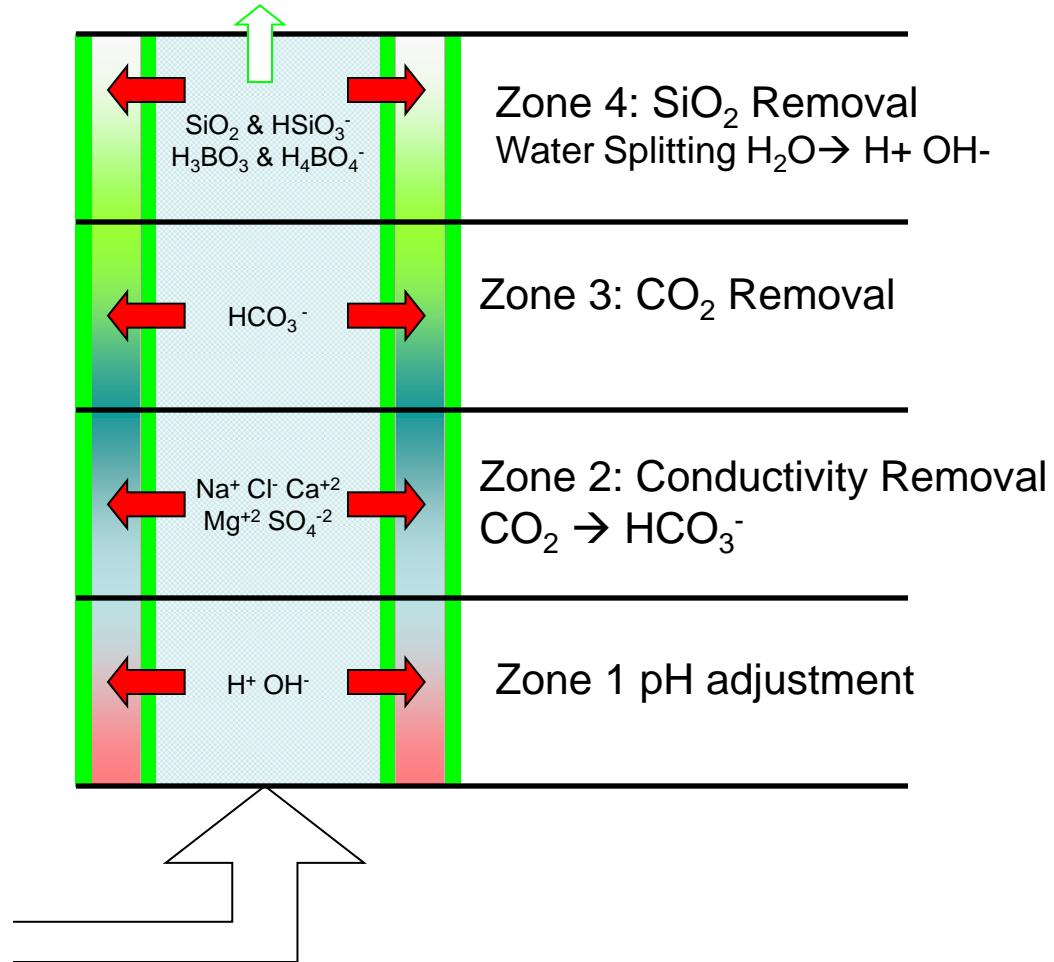
Class 4: Difficult Ions (SiO_2)

1: $\text{H}^+ \text{OH}^-$

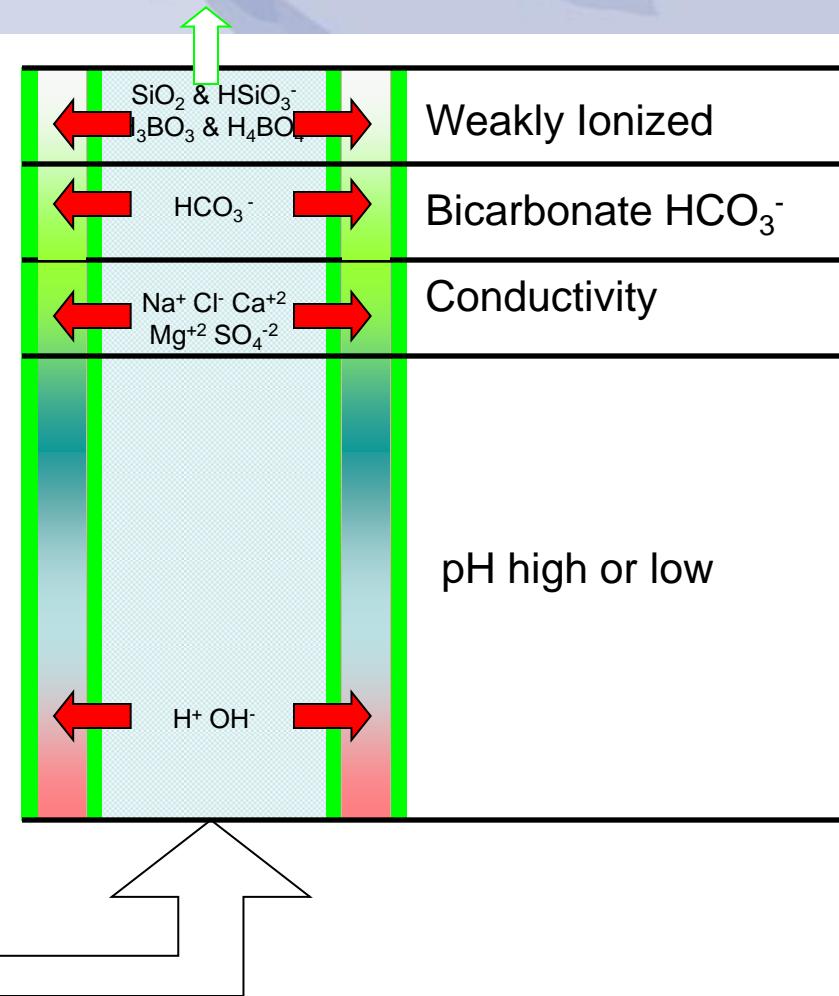
2: $\text{Na}^+ \text{Cl}^- \text{Ca}^{+2} \text{Mg}^{+2} \text{SO}_4^{-2}$

3: $\text{HCO}_3^- \text{CO}_2(\text{g})$

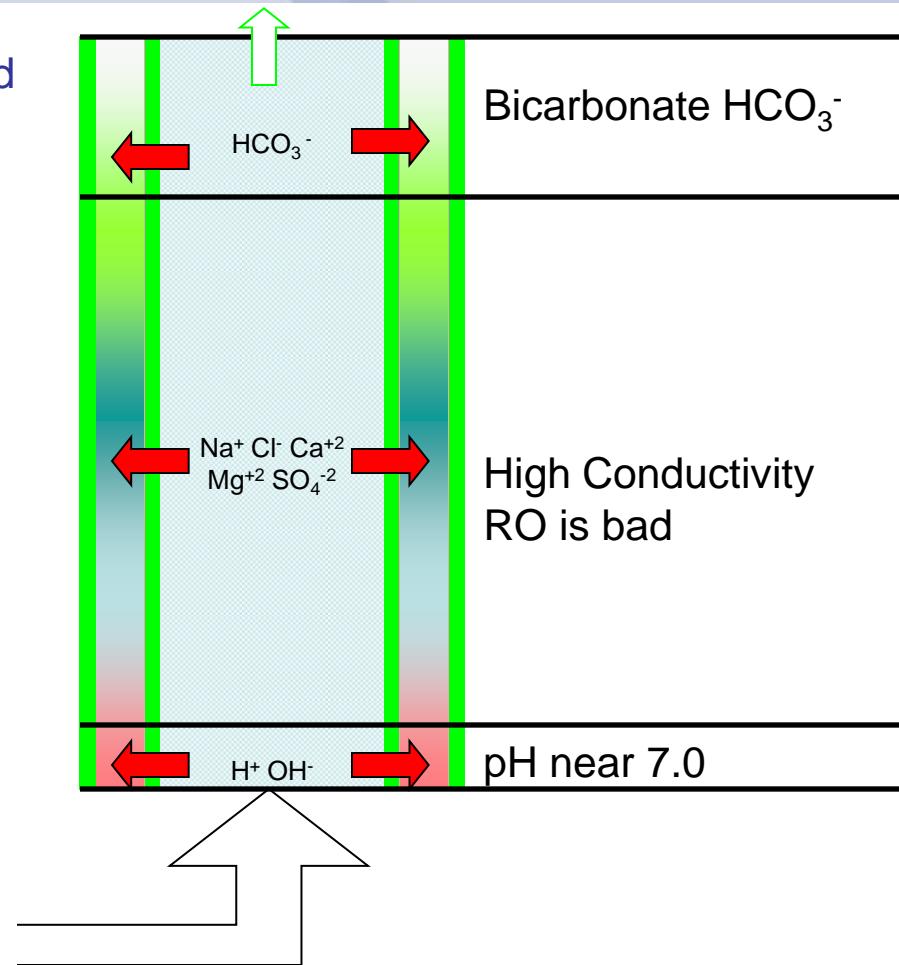
4: $\text{SiO}_2 \text{ H}_3\text{BO}_3$



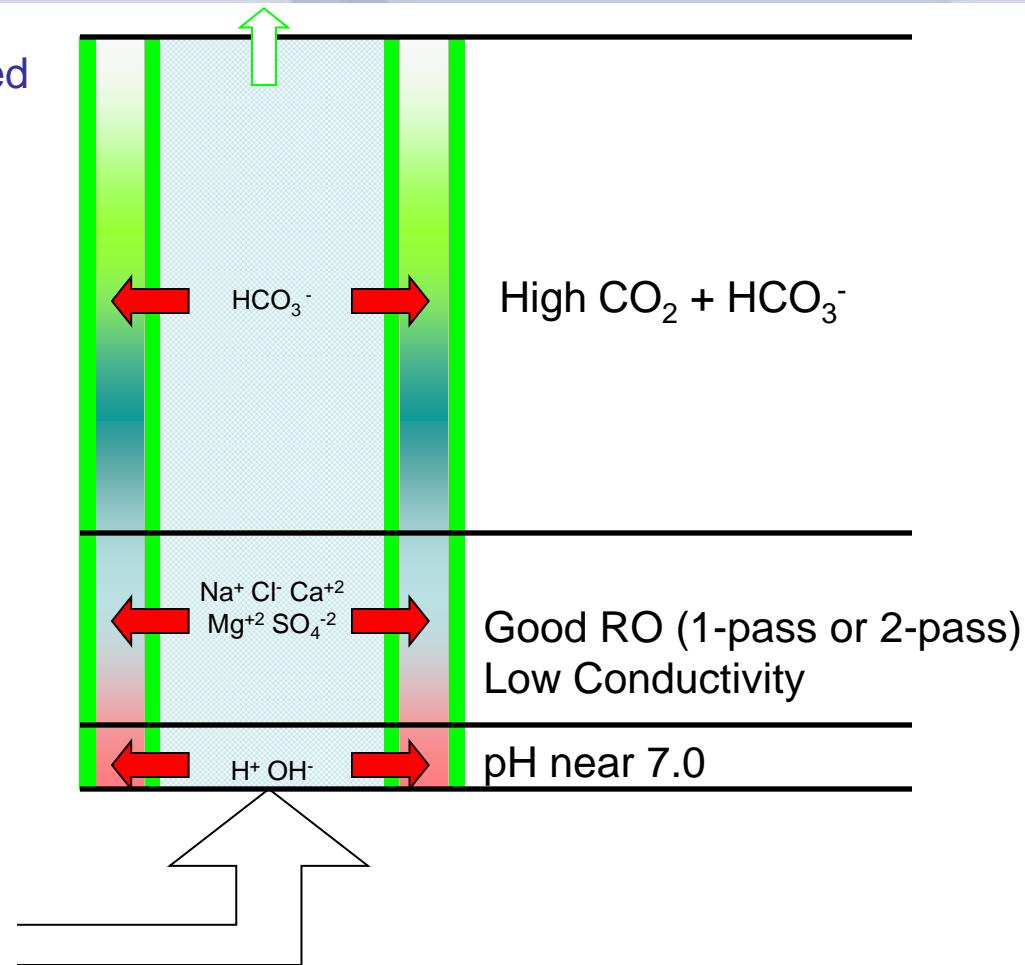
Case of high or low pH in EDI feed



Case: High conductivity in EDI feed

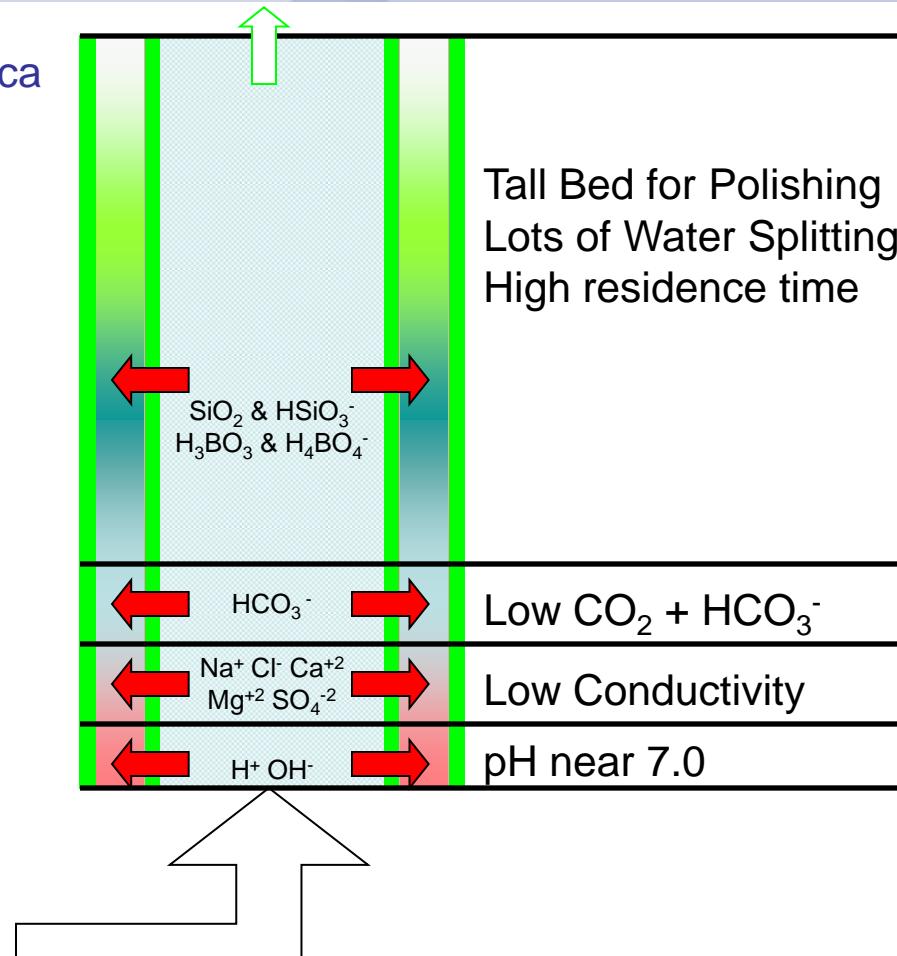


Case: High $\text{CO}_2 + \text{HCO}_3^-$ in EDI feed



EDI Optimized for Removal of Silica

1. pH in Control (6.5 to 7.5)
2. High Rejection RO
3. CO₂ Removal System (GTM)
4. Voltage Is Not Too Low

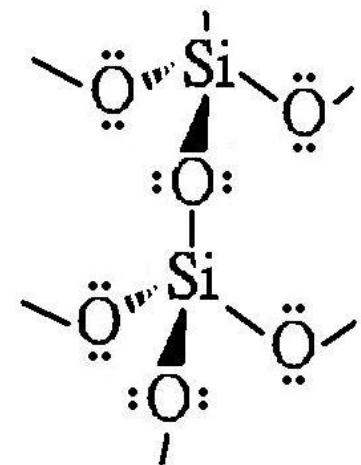
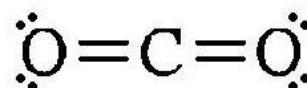


EDI “How Does It Work” Summary

- Silica < 5 ppb
- Working Bed-Polishing Bed EDI Model
- Electropure Specific Ion EDI Model
- Electropure's 4 Classes of ions
- Optimization Rules for SiO_2
 - pH of Feed (RO permeate) near 7
 - High rejection RO System
 - Removal of CO_2
 - Voltage is High-Good Water Splitting

How does EDI remove CO₂ and SiO₂?

- EDI removes charged ions
- CO₂ and SiO₂ are not charged
- How to optimize EDI Systems to remove CO₂ and SiO₂



CO₂ Chemistry



CO₂ Chemistry and pH

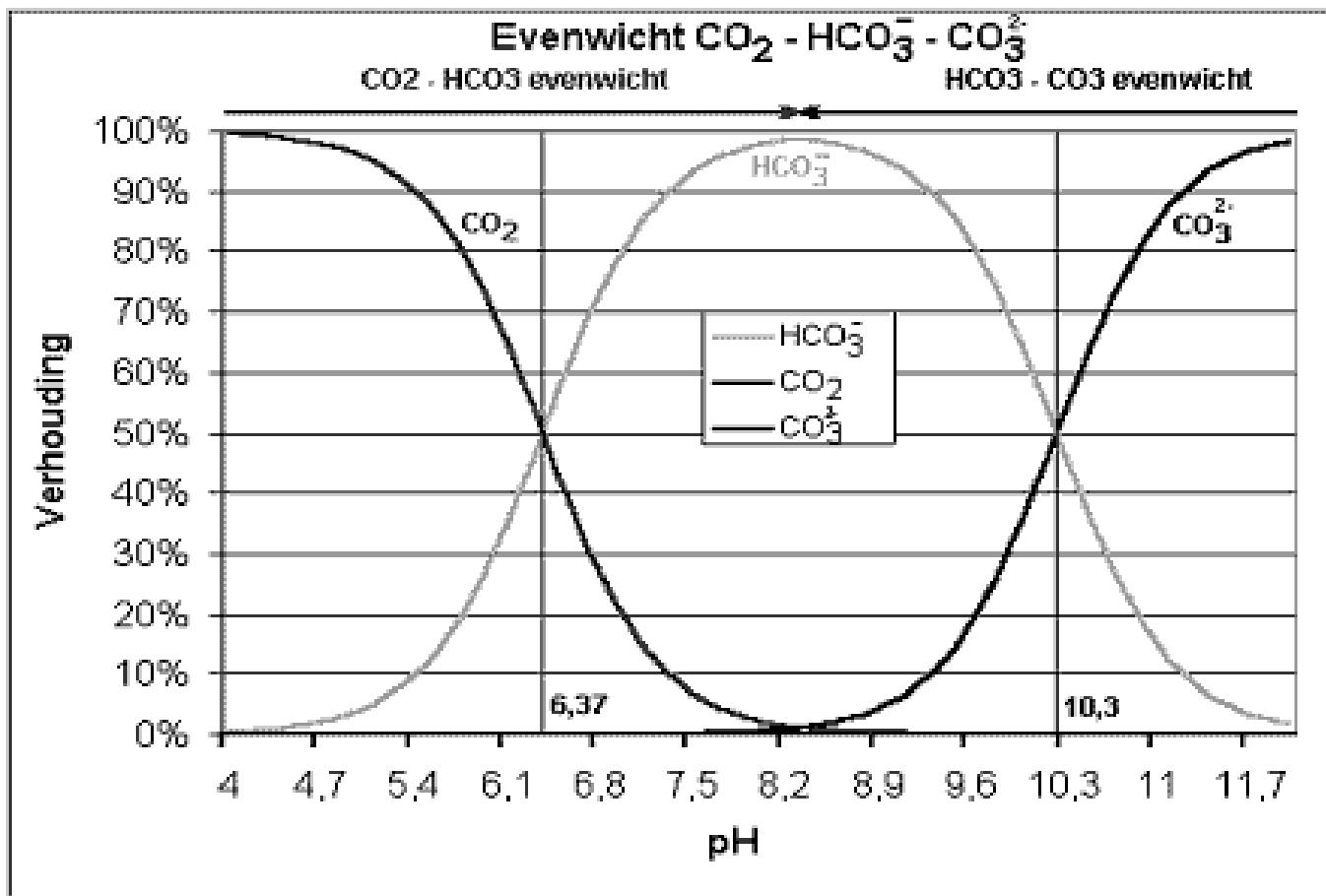


pH = 6.4

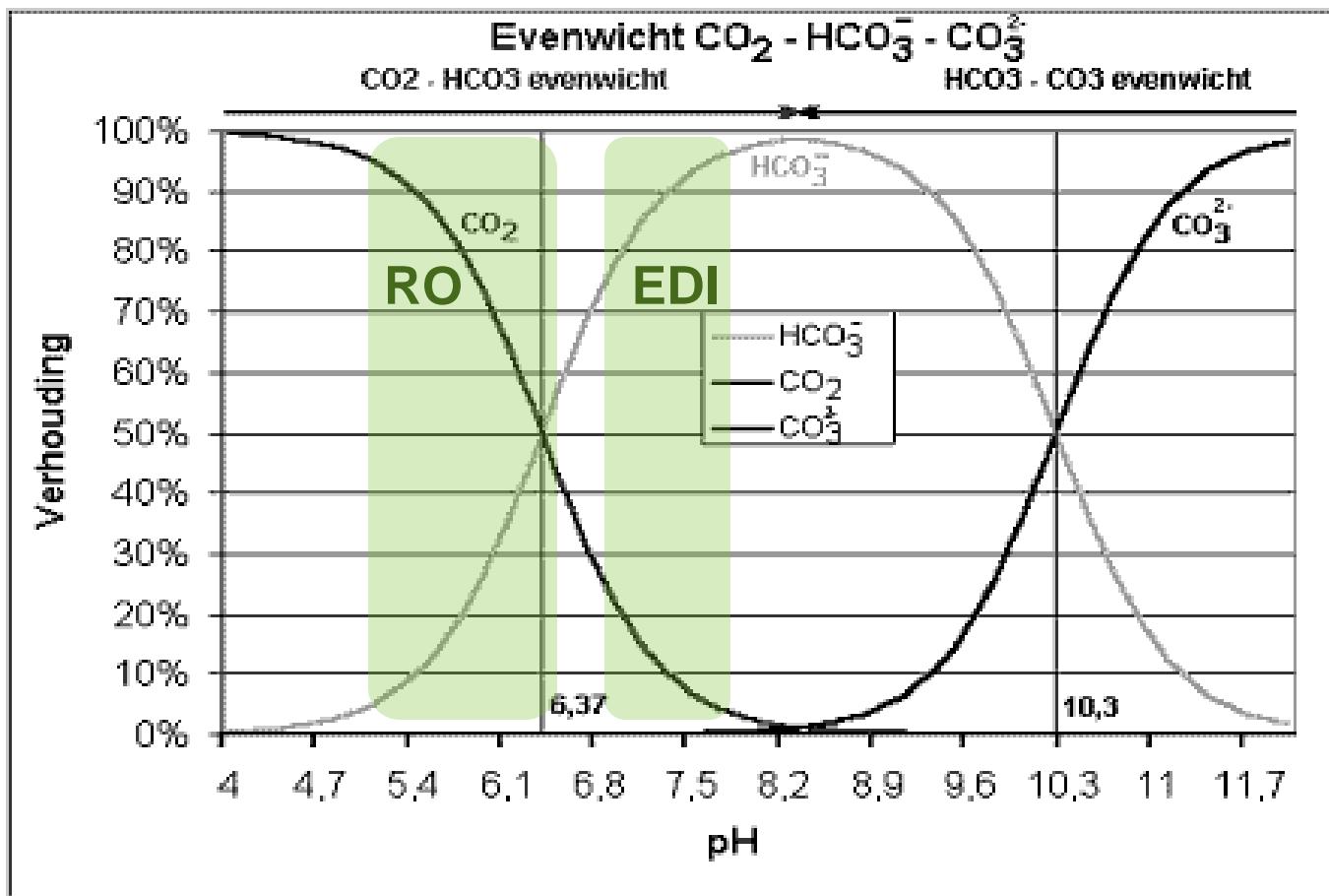


pH = 10.3

CO₂ Chemistry and pH

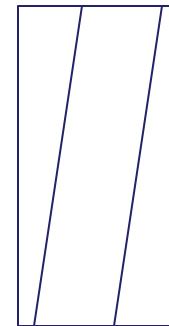


CO₂ Chemistry and pH

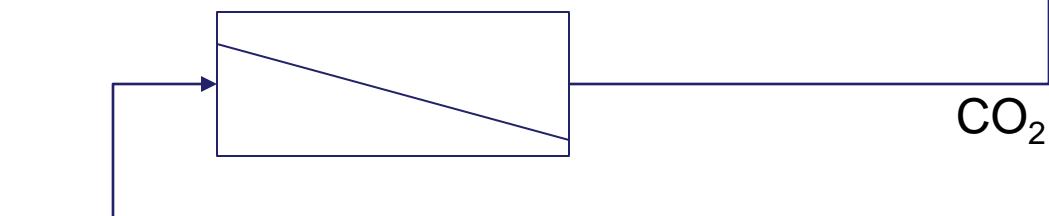


CO₂ in RO-EDI Systems

EDI: pH=7.0
CO₂+HCO₃⁻



Normal 1-pass RO:
pH=5.8-6.4
CO₂



SiO_2 Chemistry and pH



Silica is charged only above pH 9.8

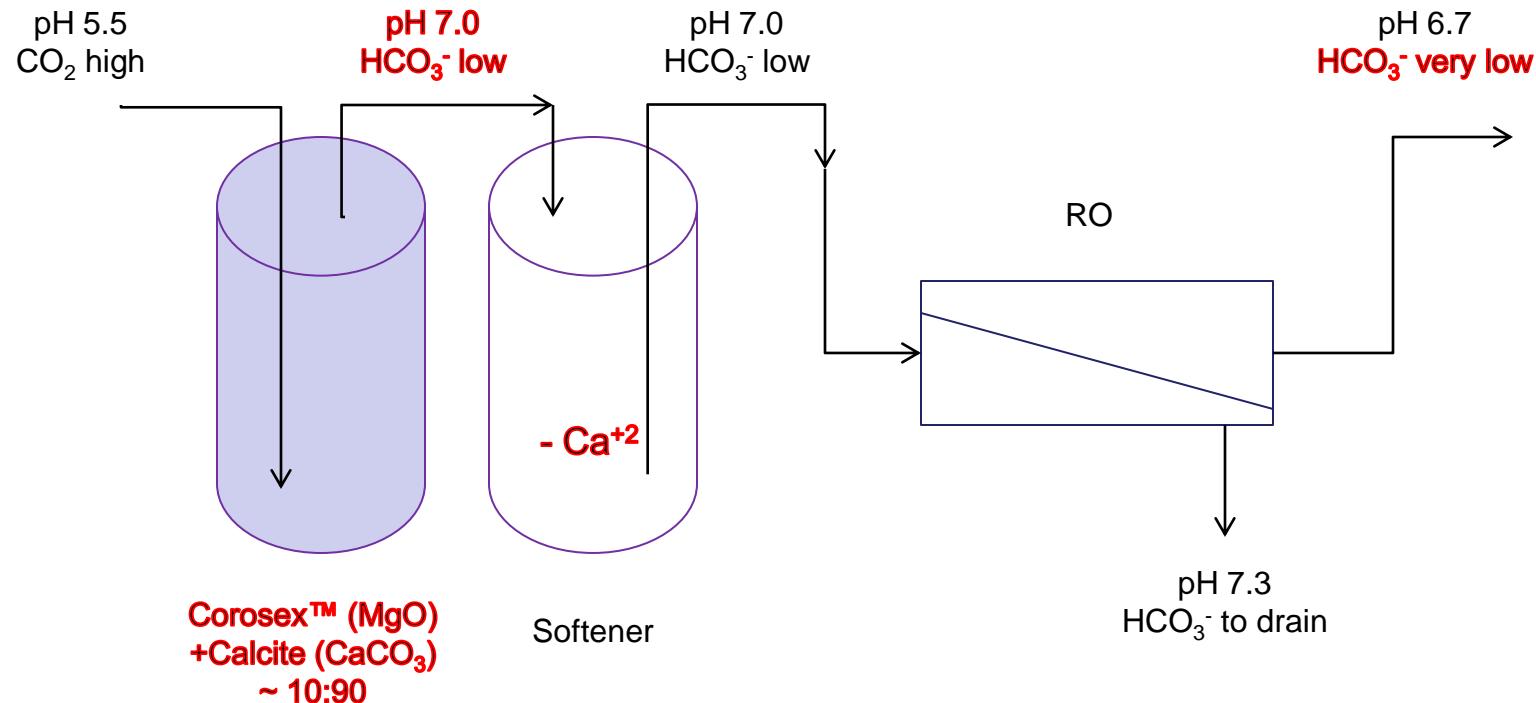
CO₂ and SiO₂ Conclusions

- RO: at pH < 6.4 CO₂ is difficult to reject
- RO: at pH < 9.8 SiO₂ is difficult to reject
- EDI: at pH = 7.0 HCO₃⁻ is weak
- EDI: at pH = 7.0 H₄SiO₄ is weak
- GTM: at pH < 6.0 GTM is very good for CO₂

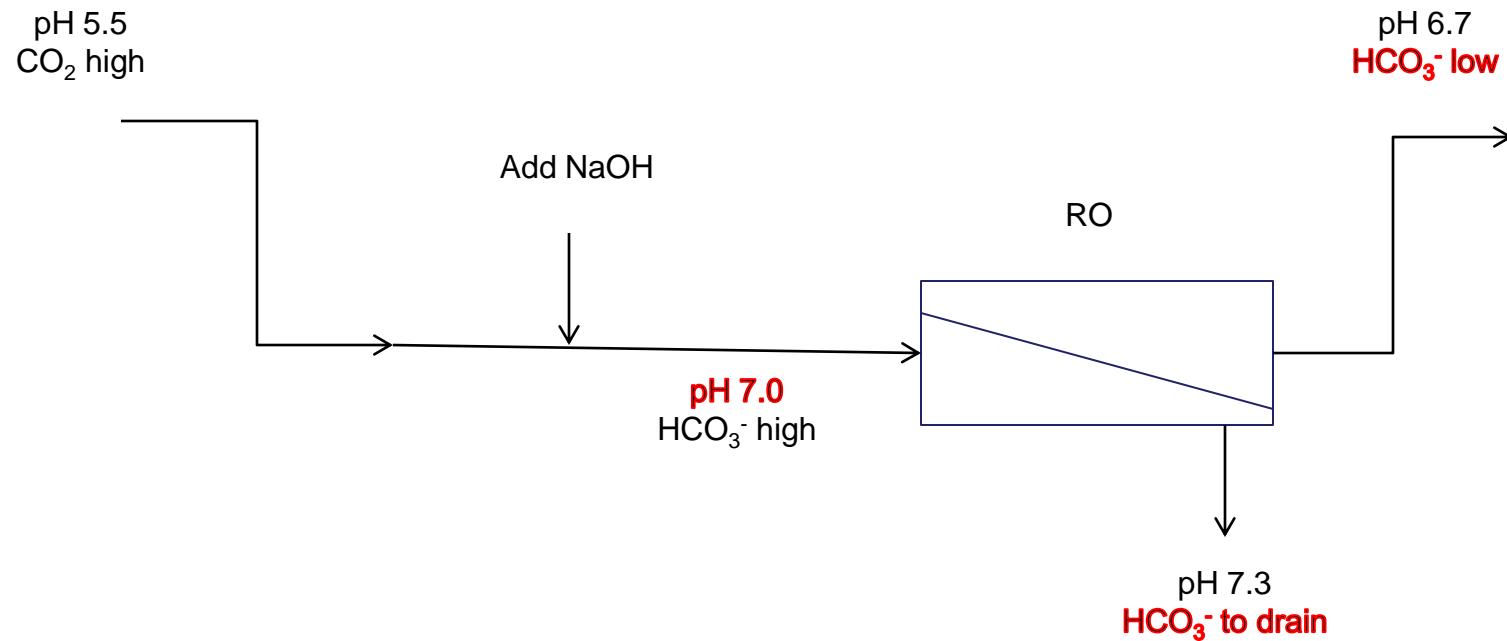
RO and CO₂

1. Use Corosex to remove CO₂ before the RO
2. pH in 1-pass RO above 6.8
3. Raise pH in 2-pass RO to above 8.3

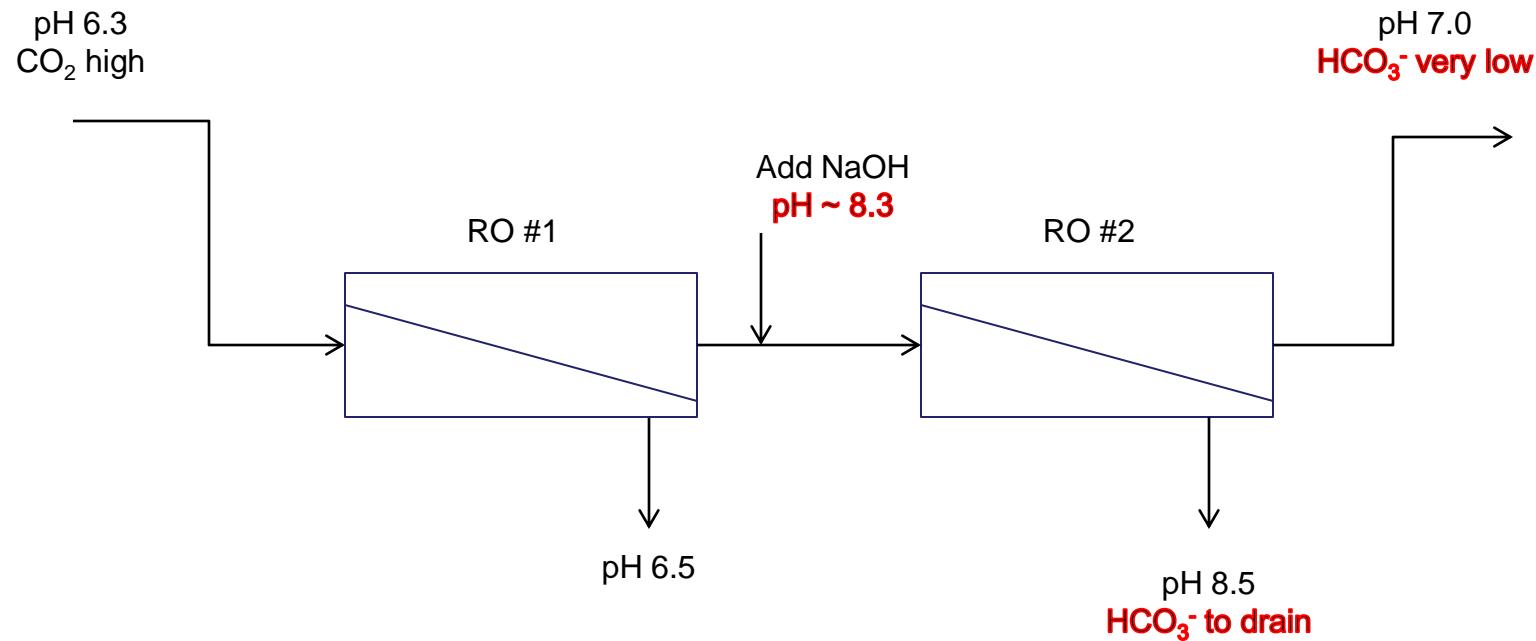
RO Option #1 (Corosex™)



RO Option #2 ($\text{pH} > 6.8$)



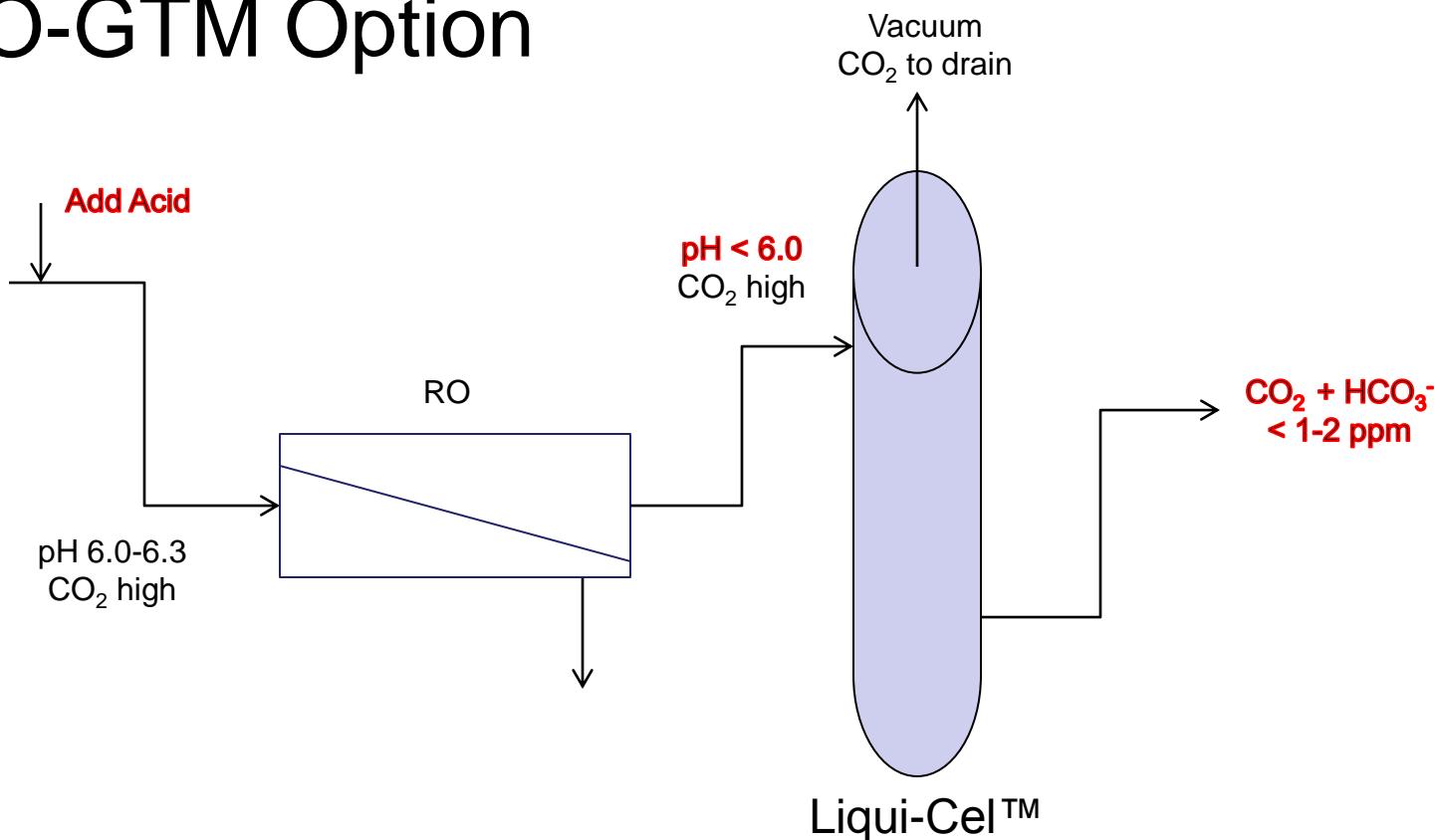
RO Option #3 (2-pass RO high pH)



GTM (Gas Transfer Membrane) and CO₂

- Use GTM (Liqui-Cel™) to remove CO₂ after the RO
- pH must be right for GTM
 - GTM removes CO₂ (gas) not HCO₃⁻
 - pH should be < 6.0

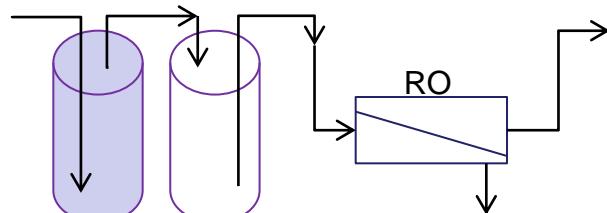
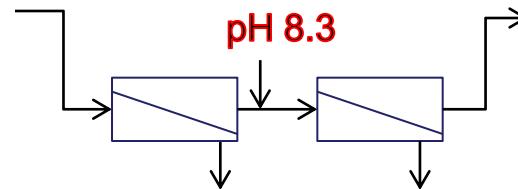
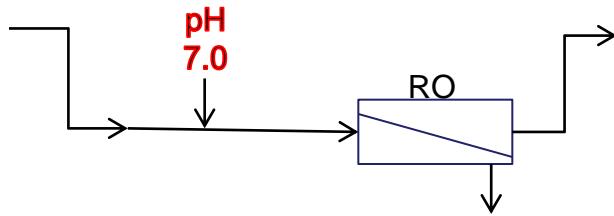
RO-GTM Option



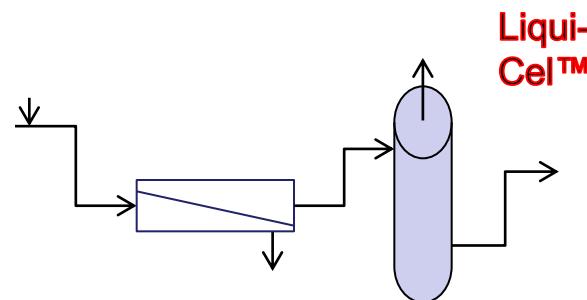
EDI Pretreatment Options

- Corosex™ removal of CO₂
- RO removal of CO₂ pH > 6.6
- 2-pass RO pH > 8.3
- RO-GTM pH < 6.0

EDI Pretreatment Options



Corosex™
+Calcite



Conclusion for CO₂

- pH is important
 - pH < 6.4 (for GTM) CO₂
 - pH > 6.4 (for RO) HCO₃⁻
- Remove CO₂ before EDI
- Remove CO₂ in EDI (pH = 7.0)

Conclusion for SiO_2

- pH is important
 - H_3SiO_4^- above pH = 9.8
- SiO_2 competes with HCO_3^- and Cl^-
 $\text{SiO}_2 \text{ HCO}_3^- \text{ Cl}^-$
 - HCO_3^- and Cl^- are stronger
- Use EDI pretreatment
 - CO_2 and conductivity removal
- EDI will remove up to 99% of SiO_2
 - 0.200 ppm → 2 ppb SiO_2